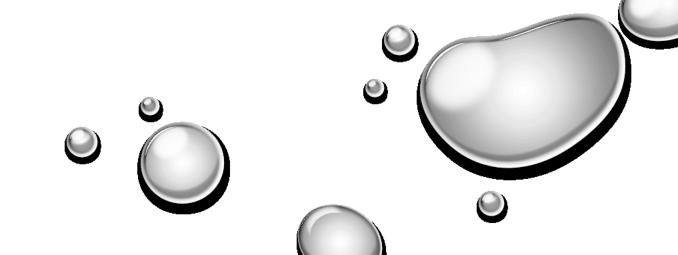


PRACTICAL CONSIDERATIONS

DIFFERENCES BETWEEN LABORATORY AND LARGER SCALE PROCESSES



DIFFERENCES BETWEEN ACADEMIC AND PROCESS CHEMISTRIES

Academic – Discovers, reveals, disputes, confirms, brings new knowledge.

Small amount of material.

Process – Selects, optimizes, seeks for efficiency, defines control points, considers efficiency and environment (also safety).

Role of chemical engineers.

Relatively large amount of material.

Laboratory (medicinal) chemistry (mg – g) has to be **diverse** and **flexible**; chromatography is very common; Can be done by a synthetic chemist only;

Process (up-scaled) pathway (kg — 1000 kg) must provide reliable results, the procedure is expected to be robust, repeatable, simple, economic, focuses on safety (both operators and patients); chromatography is to be avoided; Must be done in mutual cooperation of a synthetic chemist (thinks in steps) and a chemical engineer (thinks in unit operations)





What is scale-up?

Transferring a lab-scale chemical process to pilot or commercial equipment with:

- same yield
- same selectivity
- same quality

Scale-up is NOT a simple linear increase in geometric dimensions





What is scale-up?

MORE

- understanding of critical parameters
- how to control them
- ability to predict performance at any scale







Laird, T. – How to Minimise Scale Up Difficulties

- 1. Appropriate conditions
- 2. Correct dosing time
- 3. Hazards
- 4. Mass transfer issues
- 5. Solvent extractions
- 6. Optimising using statistical methods
- Laird, T. Chemical Industry Digest, p. 51, July 2010





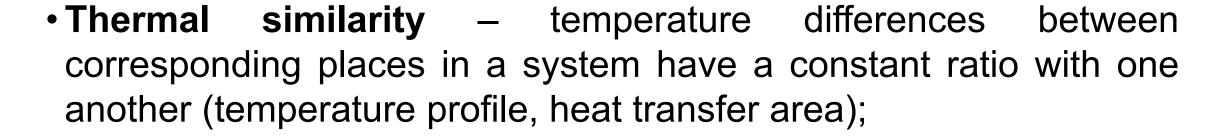


The best way to minimize the scaleup problems is by important data gathering and detailed process understanding.

Ideally, dimensions in geometry, velocities of the components, forces on the system, temperatures and concentrations should be kept constant between different scales

- Surface area per volume ratio (serious consequences for heat removal and heat input during process scale-up);
- **Kinematic similarity** they exists when two systems have the same shape and the ratios of the velocities between corresponding places are also equal; Fluid dynamics the Reynolds number (*Re*)
 - it increases during scale-up at a constant stirrer speed as the diameter of the stirrer increases;
- Hydrodynamic similarity they exists when the ratios of forces between corresponding places are also equal in both systems;





• Chemical similarity – concentration differences between corresponding places in two systems have a constant ratio to one another (ratio between the chemical conversion rate, rate of molecular diffusion).

Maintaining geometrical similarities for various scales is not practical in batch processing as the jacket heat-exchange area per unit reduces significantly with a scale

	Reactor Size [L]	Surface Area [m²]	Surface Area / Volume [m²/L]	Factor
Lab Scale	0.5	0.02	0.04	28.6
Lab Scale	10	0.20	0.02	14.3
Pilot Plant Scale	380	2.32	0.0061	4.4
Large Production	38 000	53.0	0.0014	1











- gives a measure of the degree of turbulence or the ratio of inertial force to viscous force (the higher Reynolds number the higher turbulence of the system)

 $R_e = ND^2 \rho/\mu$ (mostly for homogeneous systems)

R_e ... Reynolds number

N ... rotational speed (revolutions per second)

D ... diameter of the stirrer (m)

 μ/ρ ... kinematic viscosity (m²/s)

Maintaining total similarity of all possible scale-up parameters on different scales cannot be established and, in fact, is almost impossible;

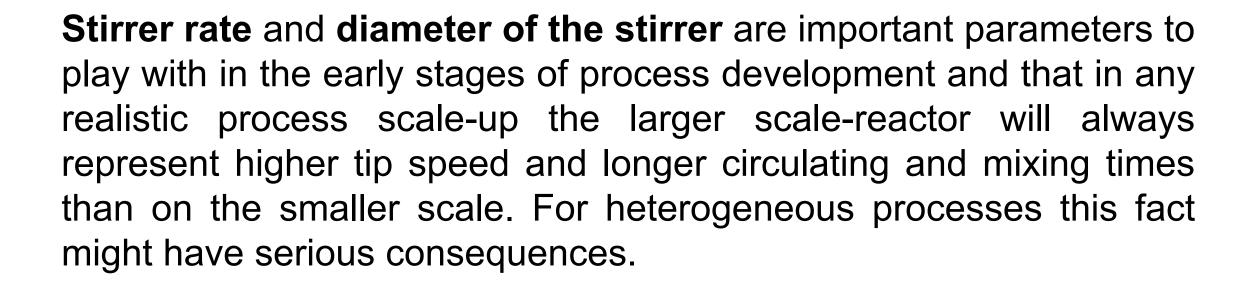
A reliable batch process scale-up cannot be simulated in generally applicable mathematical models without a clear understanding of all process and reaction mechanisms;

Regime analysis – significance/trade-off of particular similarities – can be done in an early stage of process development;

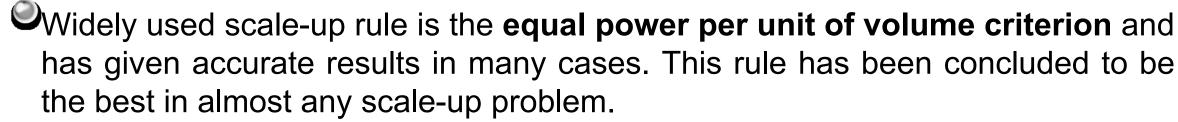
Regime analysis can be done in an early stage of the process development:

- If heat effects are relative small, then the thermal similarity will be easily maintained;
- If reaction rate is slow compared to the mixing time, a turbulent regime is not that relevant anymore;
- For very rapid reactions any limitation in diffusion might be the ratecontrolling step and the chemical reaction is a subject to a hydrodynamic regime and the energy input should get priority;
- if in a heterogeneous reaction the particle size and, therefore, the dissolution rate is an important process parameter, the chemical regime might dictate a stirrer rate on large scale where all particles are free from bottom of the reactor;









For non-laminar flow (high Reynolds number), with constant geometry and the same stirrer type

$$P/V = P_0 \times \rho \times N^3 \times D^2 = constant$$

P₀ ... power number of the stirrer

ρ ... density

N ... stirrer speed

D ... diameter of the stirrer











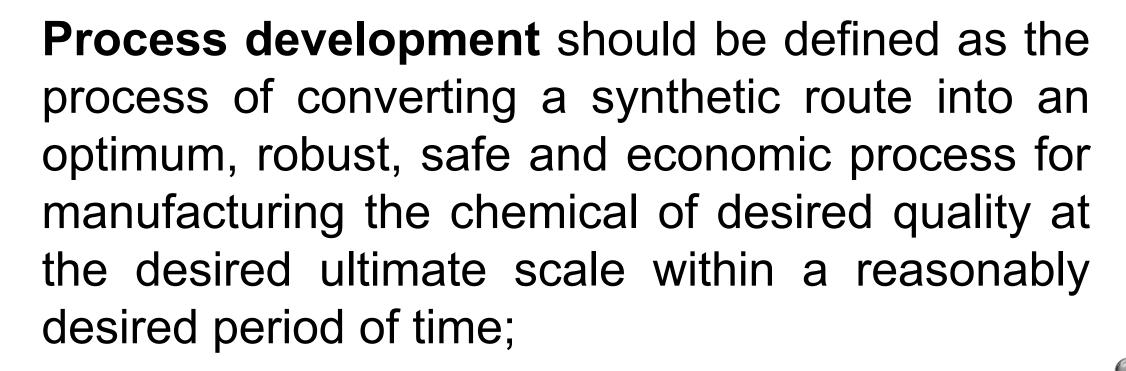
Parameter	Power	P/V	Q/V	Tip Speed	Reynolds number
Equal P	1.0	10 ⁻³	0.0215	0.215	2.15
Equal P/V	10 ³	1.0	0.215	2.15	21.5
Equal N	10 ⁵	10 ²	1.0	10	10 ²
Equal Tip Speed	10 ²	0.1	0.1	1.0	10
Equal Reynolds numner	0.1	10-4	10 ⁻²	0.1	1.0

Q/V ... the liquid pumping capacity of the stirrer per volume

Why is scale-up so difficult?

- There are no standard approaches for doing quantitative process scale-up;
- Textbooks on scale-up are limited;
- Scale-up practice largely depends upon individual experience;
- There is a shortage of people with the right experience;
- The success of process scale-up depends to a great extent on the communication and transfer of information between the chemists and the chemical engineers;
- There are no systematic ways for a chemical engineer to ask a chemist what information is required for process scale-up and *vice versa*;
- Companies and chemical engineering community are not learning from the success and failures that are occurring on a daily basis throughout the industry;
- There is a gap between how chemical engineers and chemists want the process to run in the plant and how the operators actually run it, due to lack of training or involvement.







- SAFETY
- TEMPERATURE CONTROL
- TEMPERATURE RANGE
- MOBILE (TRANSFERABLE) STREAMS
- INCREASE EFFECTIVITY (MINIMIZE SOLVENTS, INCREASE CONCENTRATION WHERE POSSIBLE)
- STABILITY OF COMPONENTS DURING REACTION AND HOLD ONS
- SIMULATE LARGE SCALE CONDITIONS IN LABORATORY (prolonged additions, heat accumulation, stability of reactants and products, etc.)
- GET INFORMATION ABOUT PROPERTIES (solubilities) pH tolerance, ...)

- DETERMINE CONTROL POINTS (in process controls)
- KEEP IT SIMPLE
- ANTICIPATE FATE OF VOLATILE REAGENTS
- DEVELOP EFFICIENT AND STRAIGHTFORWARD WORK UP PROCEDURE
- CONSIDER INERT ATMOSPHERE TO AVOID THE PRESENCE OF MOISTURE AND OXYGEN
- ASSUME SCRUBBING FOR ANNOYING OR TOXIC OFF-GASES
- SUGGEST RESISTANT MATERIAL





CHARGING



- Charging of liquids (by weight or by volume) use the same approach in the laboratory – density of liquids will change slightly with temperature;
- Recommended accuracy (tolerance) volumes <u>+</u> 5%, weights <u>+</u> 2%;
- Different transfer times considering a laboratory scale and the production (large) scale;

SOLVENT CONSIDERATIONS

watch out hydrocarbon solvents with even number of carbons (toxicity, electrostatic buildup);

- Classification of solvents **ICH Harmonised Guideline Q3C** Impurities: Guideline for Residual Solvents
 - Class 1 solvents to be avoided (known human carcinogens, strongly suspected human carcinogens, and/or environmental hazards, e.g. carbon tetrachloride (concentration limit 4 ppm), 1,2-dichloroethane (5 ppm), 1,1,1-trichloroethane (1500 ppm), benzene (2 ppm))
 - Class 2 solvents to be limited (non-genotoxic animal carcinogens, agents of irreversible toxicity, e.g. acetonitrile (410 ppm), chlorobenzene (360 ppm), chloroform (60 ppm), *N*,*N*-dimethylformamide (880 ppm), hexane (290 ppm), methanol (3000 ppm), *N*-methylpyrrolidone (530 ppm), toluene (890 ppm))
 - Class 3 solvents with low toxic potential (permissible daily exposure 50 mg or more per day, e.g. acetic acid, acetone, ethyl acetate, heptane, 2-propanol, triethylamine)

Solvents for which no adequate toxicological data was found – a manufacturer is asked to supply justification for residual levels of these solvents (e.g. diisopropyl ether, petroleum ether, trifluoroacetic acid)

IN PROCESS CONTROLS (IPCs)

Off-line analysis In-line analysis On-line analysis

WORK UP

Efficiency – e.g. crystallization directly from the reaction mixture;

labor cost is very important;

Extractions are generally preferred over filtration to remove impurities; Column chromatography is rare and very expensive;

- Includes operations after the reaction was declared complete;
- Such operations include quenching the reaction both to remove impurities and facilitate product isolation and to allow **safe** handling of process streams, even after product isolation.
- Quenching reactive species
- pH adjustment
- Filtration
- Precipitation
- Extractions
- Concentration (including azeotropic distillation)
- (Chromatography)





Typical time and money saving technique

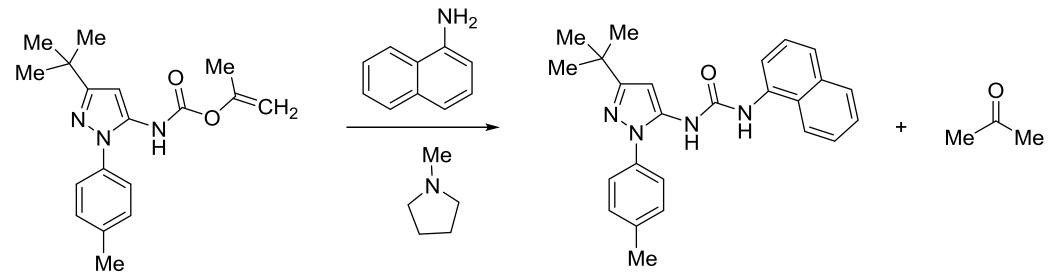
TELESCOPING

The reaction proceeds further without full isolation of an intermediate, with advantage even without any quench;

Pushing a reaction to completion – removal of side products







Gallou, F. et al J. Org. Chem. 70, 6960 (2005)



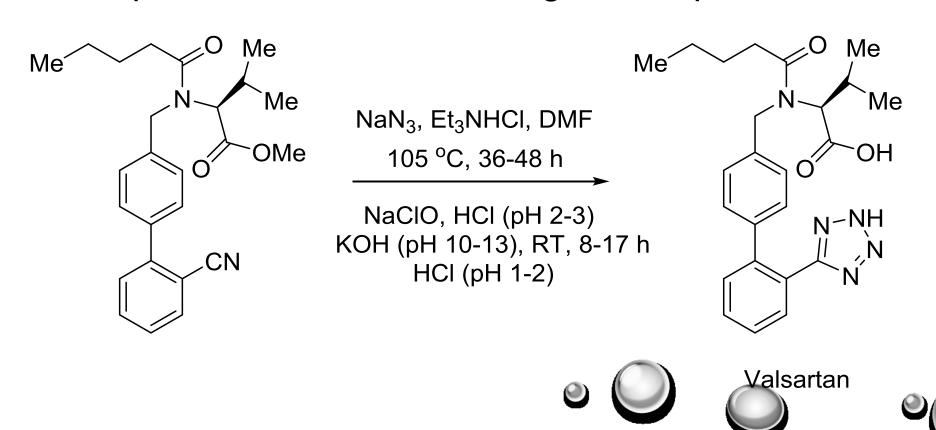






QUENCHING REACTIONS

Safe decomposition of excessive reagents stops a reaction



QUENCHING REACTIONS

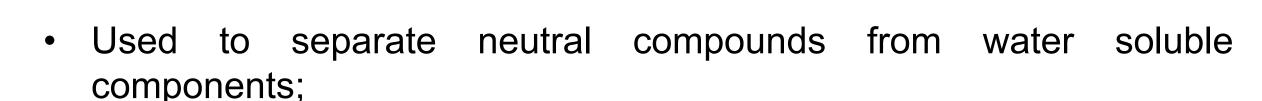
$$2 \text{ NaN}_3 + 2 \text{ HNO}_2 \longrightarrow 3 \text{ N}_2 + 2 \text{ NO} + 2 \text{ NaOH}$$

VERY CAREFUL

Recent issue with the formation of nitrosamines (e.g. limit in Valsartan (320 mg dose) will be 0.03 ppm in 2021

Careful with halogenated solvents (e.g. dichloromethane) in the presence of azides (diazidomethane !!)





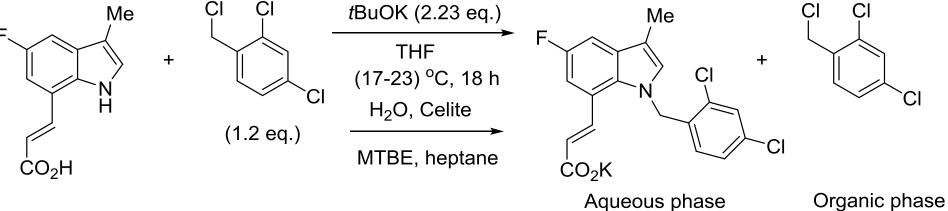
- Solid Phase Extraction (SPE) separate compounds of significant different polarity;
- Solubility or miscibility of organic solvents with water;
- Separation of layers
- pH value adjustment extra opportunities;
- Ionic strength;
- Solubility at higher temperatures;



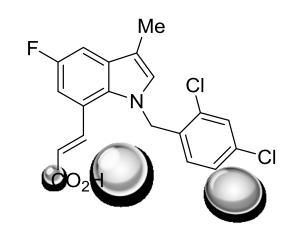








Zegar, S. *et al Org. Process Res. Dev.* 11, 747 (**2007**)



HCI to pH 1

MTBE, heptane

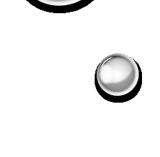


EXTRACTIONS

Convenient Aqueous Solutions for Extractions

Solvent	pH of 0.1 N solution	Relative Solubility in Organic Solvents	Comments
HCI	1.1	High	Corrosive, volatile
H ₂ SO ₄	1.2	Low	
AcOH	2.9	High	Weak acid
Na ₂ HPO ₄	8.5	Low	
NaHCO ₃	8.4	Low	
NH ₃	11.1	Moderate	Volatile
Na ₂ CO ₃	11.6	Low	
Na ₃ PO ₄	12.0	Low	
		(9)	





Polish Filtration – an operation to remove trace amounts of insoluble impurities before other operations – passing a process stream through in-line filters with different porosity;

Very important for crystallizations, avoiding emulsions;

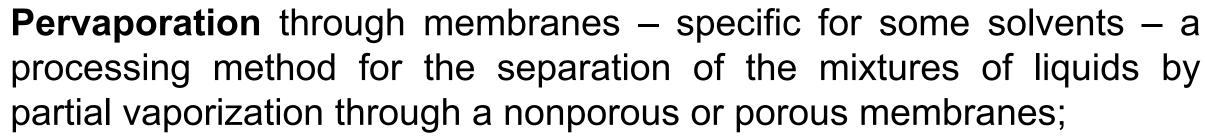
Ultrafiltration – protein separation through membranes;











Separation of components is based on a difference on a transport rate of individual components through the membrane;

Pervaporation is effective for solutions containing traces or minor amounts of the component to be removed;

Hydrophilic membranes for dehydration of alcohols containing small amount of water, hydrophobic membranes for removal of traces of organic compounds from aqueous solutions;



Hydrophilic membranes – commercially most successful membranes are formed from polyvinyl alcohol or polyimides;

Hydrophobic membranes – based on polydimethylsiloxane

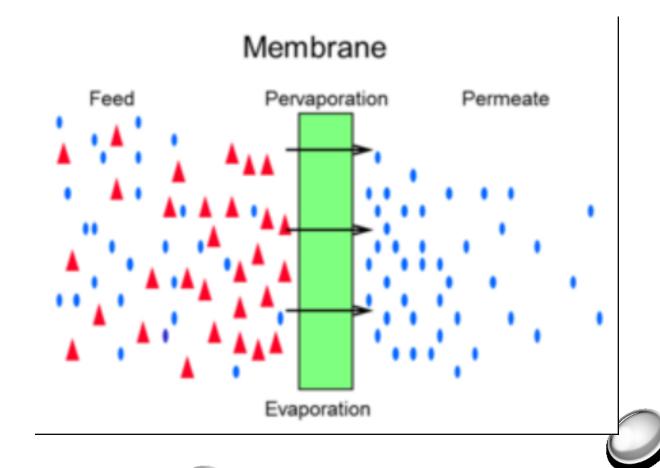
PRINCIPAL

The pressure difference on sides of a membrane (usually atmospheric vs. vacuum), **permeate** goes through a membrane, **retentate** does not go through and thus it is separated.











Best to avoid, technically difficult and expensive on large-scale, but still used in special cases (preparative chromatography);

Solid Phase Extraction

Simulated Moving Bed Chromatography

https://www.youtube.com/watch?v=Harx2khTuEc







EFFICIENT PROCESS DEVELOPMENT

- Anticipate and avoid problems
- Do experiments at minimum and maximum ranges to confirm robustness/sensitivity in cases where a particular parameter is significant
- Identify critical impurities within the whole process and their fate
- Get maximum allowed level of critical impurities
- How to proceed if the specification criteria in IPCs are not met?
- Pay attention to details, observe unusual changes
- Avoid systematic errors
- Take into account future process validation









PROCESS VALIDATION

- The cumulative effort to demonstrate reliable processing and product quality;
- The fruition of the labor of process chemists and engineers, the ultimate tests of how well one understands the process;
- Before 1970s little attention has been paid to efficient process development;
- 1987 FDA Guideline on General Principles of Process Validation (validation is defined as
 establishing documented evidence which provides a high degree of assurance that a
 specific process will consistently produce a product meeting its predetermined
 specifications and quality attributes);
- 2008 FDA process validation is the collection and evaluation of data, from the process design stage throughout production, which establishes scientific evidence that a process is capable of consistently delivering quality products; the quality is built up into the product through process understanding and cannot be tested in batches – quality by design (QbD)





