"HEAT-AND-BEAT" or "SHAKE-AND-BAKE" Solid state reactions

At least one of the reactants and one of the products are solid

Reactions in a lattice of atoms

Atomic mobility

High temperatures

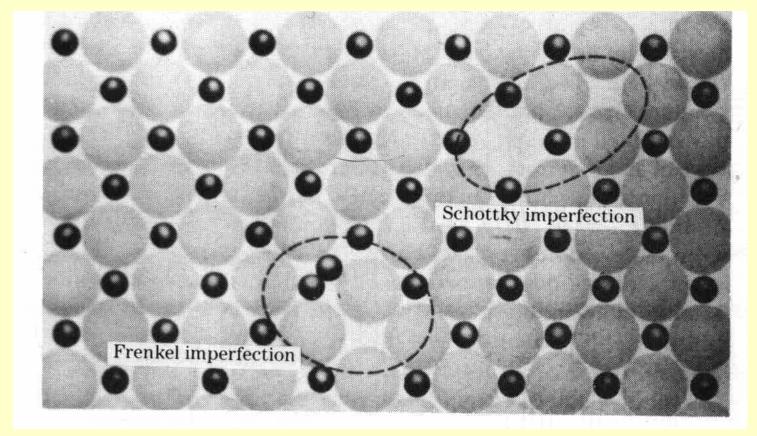
No mobility without defects – perfect crystal = no chemistry

Reactions on the interphase between phases

Microstructure

Diffusion controls the reaction rate

Point Defects



Schottky-imperfection: vacancy, missing ions moved to the surface

Frenkel-imperfection: vacancy, missing ions on interstitial positions

Reaction Types

Solid - solid synthesis - addition

$$A + B \rightarrow AB$$

$$MgO(s) + Al_2O_3(s) \rightarrow MgAl_2O_4(s)$$

$$MgO(s) + SiO_2(s) \rightarrow MgSiO_3(s) \text{ or } Mg_2SiO_4(s)$$

Solid - solid synthesis – exchange, metathesis $AB + C \rightarrow AC + B$

$$AB + C \rightarrow AC + B$$

$$CaCO_3(s) + SiO_2(s) \rightarrow CaSiO_3(s) + CO_2(g)$$

$$Ge(s) + 2 MoO_3(s) \rightarrow GeO_2(s) + 2 MoO_2(s)$$

Solid - solid synthesis – exchange and addition

$$PbSO_4 + ZrO_2 + K_2CO_3 \rightarrow K_2SO_4 + PbZrO_3 + CO_2$$

Solid - solid synthesis - dissociation

$$AB \rightarrow A + B$$

$$Ca_3SiO_5(s) \rightarrow Ca_2SiO_4(s) + CaO(s)$$

Reaction Types

Solid - solid synthesis - addition

$$A + B \rightarrow AB$$

$$MgO(s) + Al_2O_3(s) \rightarrow MgAl_2O_4(s)$$

$$MgO(s) + SiO_2(s) \rightarrow MgSiO_3(s) \text{ or } Mg_2SiO_4(s)$$

Solid - solid synthesis – exchange, metathesis

$$AB + C \rightarrow AC + B$$

$$CaCO_3(s) + SiO_2(s) \rightarrow CaSiO_3(s) + CO_2(g)$$

$$Ge(s) + 2 MoO_3(s) \rightarrow GeO_2(s) + 2 MoO_2(s)$$

Solid - solid synthesis - dissociation

$$AB \rightarrow A + B$$

$$Ca_3SiO_5(s) \rightarrow Ca_2SiO_4(s) + CaO(s)$$

Reaction Types

Solid – gas synthesis
$$A + B \rightarrow AB$$

$$2 \operatorname{Fe_3O_4(s)} + 1/2 \operatorname{O_2(g)} \rightarrow 3 \operatorname{Fe_2O_3(s)}$$

$$2 \operatorname{SiCl}_4(g) + 4 \operatorname{H}_2(g) + \operatorname{Mo}(s) \rightarrow \operatorname{MoSi}_2(s) + 8 \operatorname{HCl}(g)$$

High temperature corrosion of metals in air

Solid – gas dissociation
$$AB \rightarrow A + B$$

$$CaCO_3(s) \rightarrow CaO(s) + CO_2(g)$$

$$Al_4Si_4O_{10}(OH)_8(s) \rightarrow Al_4(Si_4O_{10})O_4(s) + 4 H_2O(g)$$

Kaolinite Metakaolinite

Other Examples

Oxides

BaCO₃ + TiO₂
$$\longrightarrow$$
 BaTiO₃ + BaTi₂O₅ + CO₂

873 K

UF₆ + H₂ + 2 H₂O \longrightarrow UO₂ (powder) + 6 HF

dust = radiological hazard, milling, sintering to UO₂ pellets

YBCO 123 Superconductor (1987)

$$Y_2O_3 + BaCO_3 + CuO \xrightarrow{1223 \text{ K}} \xrightarrow{473 \text{ K}} YBa_2Cu_3O_{7-x}$$

$$Tl_2O_3 + 2BaO + 3CaO + 4CuO \longrightarrow Tl_2Ba_2Ca_3Cu_4O_{12}$$

Other classes than oxides

Pnictides

$$Na_3E + ME + E \xrightarrow{1100 \text{ K}} Na_2M_3E_4 \qquad M = Eu, Sr, E = P, As$$

Metals

$$UF_4 + 2 Ca \longrightarrow U + 2 CaF_2$$
 Manhattan Project

Chlorides

$$3 \operatorname{CsCl} + 2 \operatorname{ScCl}_{3} \longrightarrow \operatorname{Cs}_{3} \operatorname{Sc}_{2} \operatorname{Cl}_{9}$$

$$6 \operatorname{NH}_{4} \operatorname{Cl} + \operatorname{Y}_{2} \operatorname{O}_{3} \longrightarrow 2 \operatorname{YCl}_{3} + 3 \operatorname{H}_{2} \operatorname{O} + 6 \operatorname{NH}_{3}$$

$$6 \operatorname{NH}_{4} \operatorname{Cl} + \operatorname{Y} \longrightarrow (\operatorname{NH}_{4})_{3} \operatorname{YCl}_{6} + 1.5 \operatorname{H}_{2} + 3 \operatorname{NH}_{3}$$

$$4 \operatorname{NH}_{4} \operatorname{Cl} + 3 \operatorname{NH}_{4} \operatorname{ReO}_{4} \longrightarrow 3 \operatorname{Re} + 12 \operatorname{H}_{2} \operatorname{O} + 3.5 \operatorname{N}_{2} + 4 \operatorname{HCl}$$

Aluminosilicates

$$NaAlO_2 + SiO_2 \longrightarrow NaAlSiO_4$$

Chalcogenides

Pb + Mo + S
$$\xrightarrow{1400 \text{ K}}$$
 PbMo₆S₈ Chevrel phases (M_xMo₆X₈, M = RE, Sn, Pb, Cu, X = S, Se, Te)

Powder Mixing Method

Precise weighing for exact stoichiometry

Mixing (components, dopants, additives)

Milling or grinding (ball mill, mortar)

Compaction (pelleting, organic binders)

Calcination @ high temperature (> 1000 °C)

Firing/grinding cycles

Planetary ball mill

Horizontal section Movement of the supporting disk Centrifugal force

Planetary ball mill

Rotation and counter-wise spining



Rotation speed: up to 400 rpm Milling jars: alumina, YSZ, tungsten carbide, agate



Atritor mill

Compaction - Pressing







Hydraulic Uniaxial Press

Maximum pressure: 120 MPa

Warm Isostatic Press

Max. pressure: 400 MPa Max. temperature: 80 °C

Volume: 2,51

Hot press

Max. temperature: 1250 °C

Max. pressure: 100 MPa
Max. diameter: 25 mm2

Calcination



Tube Furnace

in air and in controled atmosphere Maximum temperature: 1450 °C or 1600 °C Furnace-tube diameter: up to 75 mm



Vacuum Furnace

in vacuum or Ar, N₂, O₂ atmosphere Maximum temperature: 1200 °C

Chamber Dimensions: 150x200x250 mm³

Advantages simple equipment

low cost and easily accessible starting materials well studied

Disadvantages

```
impurities from grinding (Fe, Cr, ...) broad particle size distribution some phases unstable @ high T, decomposition formation of undesirable phases slow formation, diffusion, long reaction times large grain size poor chemical homogeneity: poor mixing of large crystallites (milling lower limit \sim 100 nm) volatility of some components (Na<sub>2</sub>O, PbO, ...) uptake of ambient gas (O<sub>2</sub> in superconductors)
```

Experimental Considerations

6^{*} Reagents

Drying, fine grain powders for maximum SA, surface activation (Mo + H_2), in situ decomposition (CO_3^{2-} , OH^- , O_2^{2-} , $C_2O_4^{2-}$) for intimate mixing, precursor reagents, homogenization, organic solvents, grinding, ball milling, ultrasonication

6^{**} Container Materials

Chemically inert crucibles, boats, ampoules (open, sealed, welded)
Noble metals: Au, Ag, Pt, Ni, Rh, Ir, Nb, Ta, Mo, W
Refractories: alumina, zirconia, silica, BN, graphite
Reactivities with containers at high temperatures needs to be carefully evaluated for each system, pelleting minimizes contact with container, sacrificial pellet

Properties of Common Container Materials

Material	Maximum Working Temp., K	Thermal Shock Resistance	Thermal Conductivity, W m ⁻¹ K ⁻¹	Coefficient of Linear Expansion x10 ⁶ , K ⁻¹	Other Properties
Pyrex	770	GOOD	1.13	3.2	Permeable to air at high T
CaF ₂	1420	FAIR	-	24	-
SiO_2	1530	VERY GOOD	1.38 - 2.67	0.4 - 0.6	Permeable to air at high T, devitrification above 1670 K
Si_3N_4	1770	FAIR	10 - 33	6.4	-
Pt	1950	VERY GOOD	73	9.11	Plastic at high T
BN	1970	VERY GOOD	5.02	0.2-3	Oxidizes in air above 970 K
Vitreous C	2070	GOOD	4.19 - 8.37	2-3.5	Oxidizes in air above 900 K
Al_2O_3	2170	FAIR	35 - 39	8	Reacts with metals above 1800 K
AlN	2270	FAIR	50 - 170	5.7	-
BeO	2570	GOOD	230	8.4	Reacts with metals above 1800 K
ZrO_2	2570	GOOD	1.97	4.5	-
Ir	2600	VERY GOOD	148	6.8	-
MgO	2870	FAIR	37.7	25	High vapor pressure
ThO_2	3070	FAIR	4.19	6	Reacts with C above 2290 K

♦* Heating Program Slow or fast heating, cooling, holding at a set point temperature

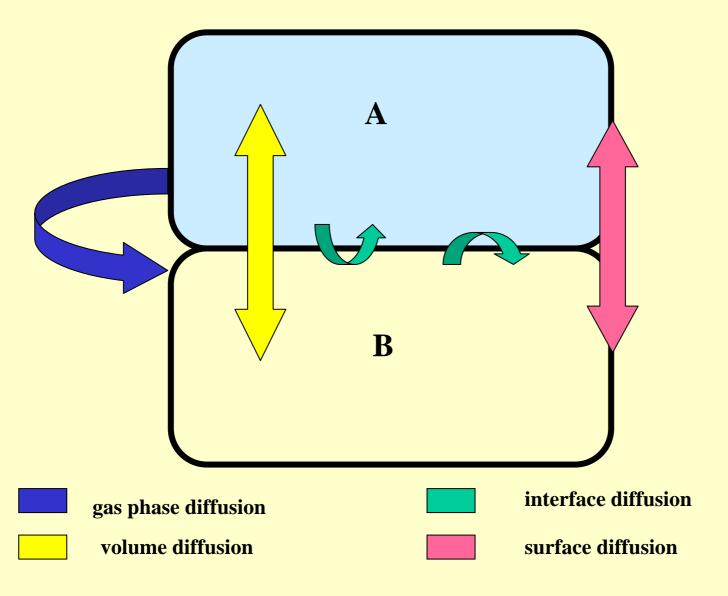
Tammann's rule: $T_r > 2/3 T_m$

Furnaces, RF, microwave, lasers, ion or electron beam

♠* Prior decomposition
Initial cycle at lower temperature to prevent spillage or volatilization, frequent cycles of heating, cooling, grinding, boost SA.
Overcoming sintering, grain growth, fresh surfaces. Pelleting, hot pressing, enhanced contact area increases rate and extent of reaction

◆* Controlled atmosphere (oxidizing, reducing, inert) or vacuum. Unstable oxidation states, preferential component volatilization if T too high, composition dependent atmosphere (O₂, NH₃, H₂S, ...)

Reaction Paths between Two Solids



Model reaction, well studied:

$$MgO + Al_2O_3 \rightarrow MgAl_2O_4$$
 Spinel
 $(ccp O^{2-}, Mg^{2+} 1/8 T_d, Al^{3+} 1/2 O_h)$

Single crystals of precursors, interfaces between reactant grains

On reaction, new reactant-product MgO/MgAl₂O₄ and Al₂O₃/MgAl₂O₄ interfaces are formed

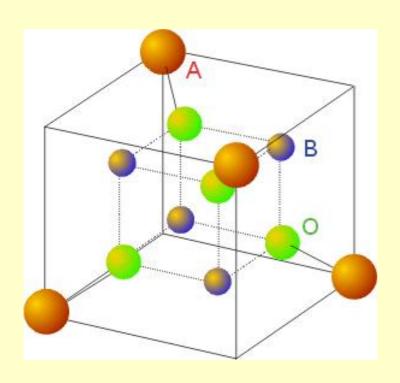
Free energy negative, favors reaction but extremely slow at normal temperatures (several days at 1500 °C)

Interfacial growth rates 3:1

Linear dependence of interface thickness x^2 versus t

Easily monitored rates with colored product at interface, T and t $NiO + Al_2O_3 \rightarrow NiAl_2O_4$ $MgO + Fe_2O_3 \rightarrow MgFe_2O_4$

The Spinel Structure: AB₂O₄



fcc array of O^{2-} ions, A occupies 1/8 of the tetrahedral and B 1/2 of the octahedral holes

 \rightarrow <u>normal spinel</u>: AB₂O₄

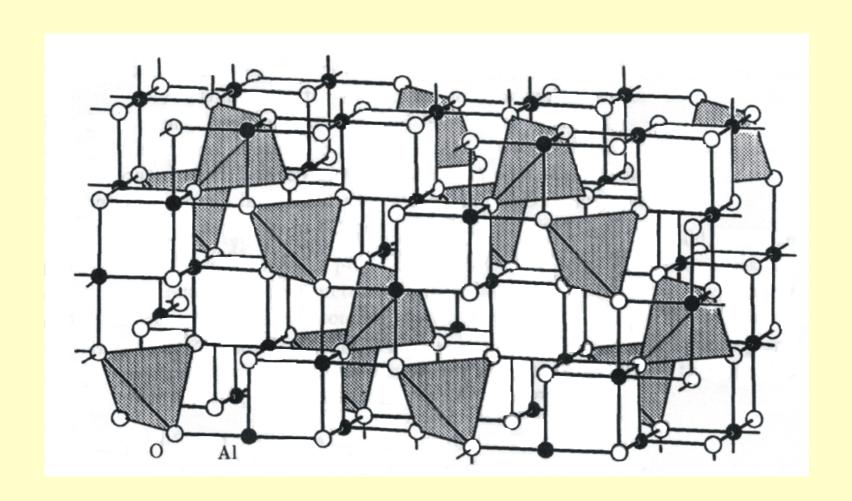
Co₃O₄, GeNi₂O₄, WNa₂O₄

 \rightarrow inverse spinel: B[AB]O₄

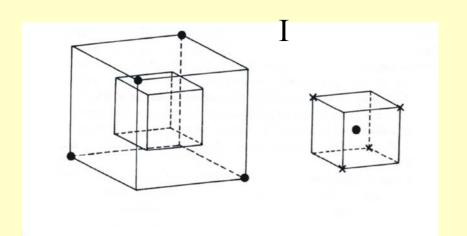
 Fe_3O_4 : $Fe^{3+}[Fe^{2+}Fe^{3+}]O_4$, $TiMg_2O_4$, $NiLi_2F_4$

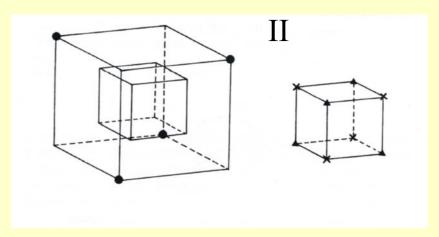
→ basis structure for several magnetic materials

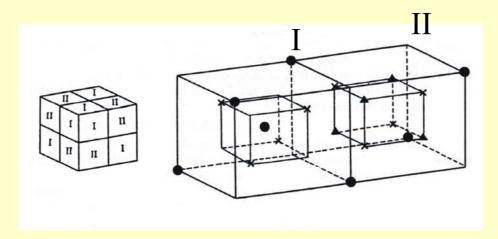
The spinel structure: MgAl₂O₄



The spinel structure: MgAl₂O₄







- $\bullet = Mg$
- $\mathbf{x} = \mathbf{O}$
- $\triangle = Al$

Why is nucleation, mass transport so difficult?

MgO ccp O^{2-} , Mg^{2+} in O_h sites Al_2O_3 hcp O^{2-} , Al^{3+} in 2/3 O_h sites $MgAl_2O_4$ ccp O^{2-} , Mg^{2+} 1/8 T_d , Al^{3+} 1/2 O_h

- **♦*** Structural differences between reactants and products, major structural reorganization in forming product spinel
- lacktriangle Making and breaking many strong bonds (mainly ionic), high temperature process as $D(Mg^{2+})$ and $D(Al^{3+})$ large for small highly charged cations
- **♦**** Long range counter-diffusion of Mg²⁺ and Al³⁺ cations across interface, usually RDS (= rate determining step), requires ionic conductivity, substitutional or interstitial hopping of cations from site to site to effect mass transport
- **♦*** Nucleation of product spinel at interface, ions diffuse across thickening interface, oxide ion reorganization at nucleation site
- **♦**** Decreasing rate as spinel product layer thickens

Parabolic rate law: dx/dt = k/x

$$x^2 = kt$$

Kinetics:

Linear x^2 vs. t plots observed ln k vs. 1/T experiments provide Arrhenius activation energy E_a for the solid-state reaction

Reaction mechanism requires charge balance to be maintained in the solid state interfacial reaction:

3Mg²⁺ diffuse in opposite way to 2Al³⁺

MgO/MgAl₂O₄ Interface:

$$2Al^{3+} - 3Mg^{2+} + 4MgO \rightarrow 1MgAl_2O_4$$

MgAl₂O₄/Al₂O₃ Interface:

$$3Mg^{2+} - 2Al^{3+} + 4Al_2O_3 \rightarrow 3MgAl_2O_4$$

Overall Reaction:

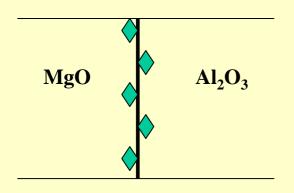
$$4MgO + 4Al_2O_3 \rightarrow 4MgAl_2O_4$$

the **Kirkendall** Effect: RHS/LHS growth rate of interface = 3/1

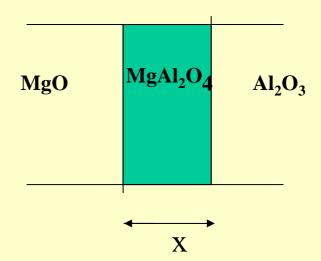
Model for a classical solid-solid reaction (below melting point!): Planar interface between two crystals

$$MgO + Al_2O_3 \rightarrow MgAl_2O_4$$
 (Spinel)

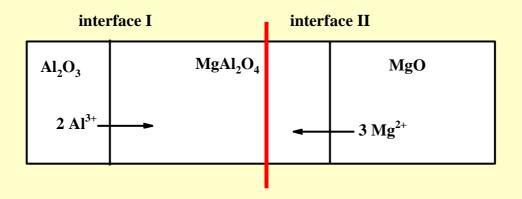
Phase 1: nucleation

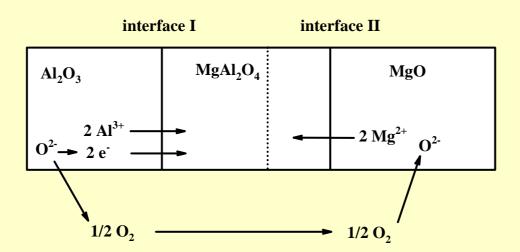


Phase 2: growth of nuclei



Reaction Mechanism





Thermodynamic and kinetic factors

General kinetic expression

$$g(\alpha) = \int k(T) dt$$
 $g(\alpha) = k(T) t$

$$\frac{d\alpha}{dt} = k(T)f(\alpha)$$

$$\frac{d\alpha}{dt} = k(T)f(\alpha)$$

$$\int \frac{d\alpha}{f(\alpha)} = g(\alpha) = \int k(T)dt$$

 α – the molar fraction of the reacted product at a time t k(T) – the rate constant of the process

Experimentally evaluate α at different t Fit data into a $g(\alpha) = k(T)$ t expression to obtain k(T) and the type of mechanism model

$$\alpha = \frac{P_t - P_0}{P_e - P_0}$$

$$P_t$$
 = the value of a property at time t
 P_0 = the value of a property at the beginning

 P_e = the value of a property at the end

$$\alpha = 0 - 1$$

e.g.
$$P_t = \text{mass loss}, x, \dots$$

$$\frac{d\alpha}{dt} = k(T)f(\alpha)$$

$$\int \frac{d\alpha}{f(\alpha)} = \int k(T)dt$$

$$g(\alpha) = \int k(T) dt$$

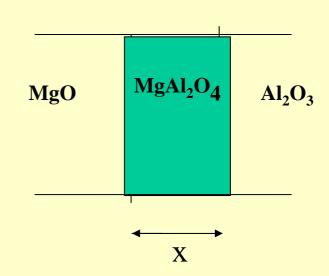
$$g(\alpha) = k(T) t$$

Decreasing reaction rate as spinel product layer (x) thickens

Here $\alpha = x$ Parabolic rate law:

$$dx/dt = k/x$$

$$x^2 = kt$$



Mechanism model

 $g(\alpha)$

 $(1-2/3\alpha) - (1-\alpha)^{2/3}$ $(1+\alpha)^{2/3} + (1-\alpha)^{2/3}$

Diffusion controlled

One-dimensional
$$\alpha^2$$
Two-dimensional $\alpha + (1-\alpha) \ln (1-\alpha)$
Three-dimensional, Jander $[1-(1-\alpha)^{1/3}]^{2/3}$
Three-dimensional, Ginstling $(1-2/3\alpha)-(1-\alpha)^{2/3}$
Three-dimensional, Carter $(1+\alpha)^{2/3}+(1-\alpha)^{2/3}$

Growth controlled

General	$[1-(1-\alpha)^{1-n}]$
First order, n = 1	$[-\ln{(1-\alpha)}]$

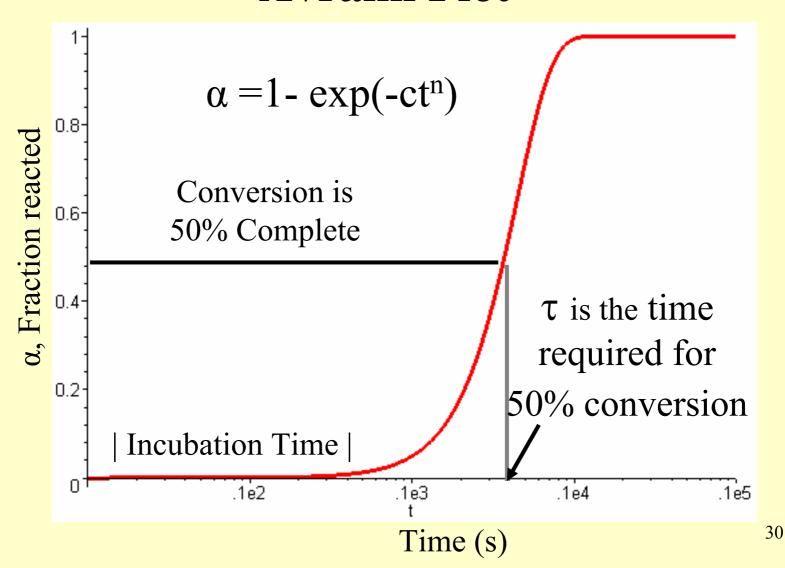
Nucleation controlled Power law

 $\alpha^{1/n}$

Nucleation-Growth controlled

Avrami	$\left[-\ln\left(1-\alpha\right)\right]^{1/2}$
Erofeev	$[-\ln{(1-\alpha)}]^{1/3}$
Planar boundary	$1-(1-\alpha)^{1/2}$
Spherical boundary	$1 - (1 - \alpha)^{1/3}$

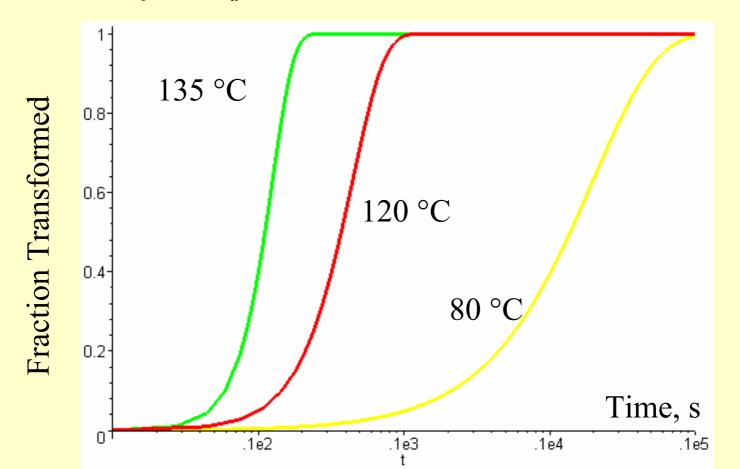
Avrami Plot



Perform the measurements in a range of temperatures \boldsymbol{T} use Arrhenius equation to evaluate the activation energy \boldsymbol{E}_a

$$k(T) = k_0 \exp(-E_a/RT)$$

Perform the measurements in a range of temperatures T use Arrhenius equation to evaluate the activation energy E_a $k(T)=k_0 \exp(-E_a/RT)$



FACTORS INFLUENCING REACTIONS OF SOLIDS

CONTACT AREA

- *****Surface area of reactants
- *****Particle size
- *****Pelleting, pressing, precursors

DIFFUSION RATE

- **★**Diffusion rates of atoms, ions, molecules in solids
- **★**Reaction temperature, pressure, atmosphere
- *****Diffusion length, particle size
- **★**Defect concentration, defect type
- *Reaction mechanism

NUCLEATION RATE

- **★**Nucleation of product phase within the reactant with similar crystal structure
- *****Epitactic and topotactic reactions
- **★**Surface structure and reactivity of different crystal planes/faces

KEY FACTORS IN SOLID STATE SYNTHESIS

CONTACT AREA and surface area (SA) of reacting solids control:

- → Rates of diffusion of ions through various phases, reactants and products
- → Rate of nucleation of the product phase

Reaction rate is greatly influenced by the SA of precursors as contact area depends roughly on SA of the particles

Surface Area (SA) of Precursors

spherical particles, radius r [nm], density ρ [g/cm³]

$$SA = A/m = \frac{4\pi r^2}{4/3\pi r^3 \cdot \rho}$$
 = 3000/r ρ [m²/g]

Consider 1 g of a material, density 1.0 g/cm³, cubic crystallites

number of cubes	edge length, cm	$SA, m^2/g$
1	1	6.10 ⁻⁴
10 ⁹	10 ⁻³	0.6
10 ¹⁸	10 ⁻⁶	600

Contact area

not in reaction rate expression for product layer thickness versus

time: dx/dt = k/x

But for a constant product volume

 $x \propto 1/A_{contact}$ and furthermore $A_{contact} \propto 1/d_{particle}$

Thus particle sizes and surface area inextricably connected and obviously $x \propto d$ and SA particle size affect the interfacial thickness

These relations suggest some strategies for rate enhancement in direct reactions:

- → Hot pressing densification of particles
 High pressure squeezing of reactive powders into pellets (700 atm)
 Pressed pellets still 20-40% porous. Hot pressing improves
 densification
- **→**Atomic mixing in composite precursor compounds
- **→** Coated particle mixed component reagents, corona/core precursors
- **→** Decreasing particle size, nanocrystalline precursors

Aimed to increase interfacial reaction area A and decrease interface thickness x, minimizes diffusion length scales

dx/dt = k/x = k'A = k''/d

DIFFUSION RATE

Fick's law J = -D(dc/dx)

J = flux of diffusing species, #/cm²s (dc/dx) = concentration gradient, #/cm⁴ D = diffusion coefficient, cm²/s, for good reaction rates > 10⁻¹²

D increases with temperature, rapidly as you approach the melting point

Tammann's rule: Extensive reaction will not occur until the temperature reaches at least 2/3 of the melting point of one or more of the reactants.

Factors influencing cation diffusion rates:

- **→**Charge, mass and temperature
- **→**Interstitial versus substitutional diffusion
- →Number and types of defects in reactant and product phases
 All types of defects enhance diffusion of ions
 (intrinsic or extrinsic, vacancies, interstitials, lines, planes, dislocations, grain boundaries)

Diffusion

Diffusion coefficients show an exponential temperature dependence (Arrhenius type):

 D_{∞} : D for $T \rightarrow \infty$,

Q: activation energy of diffusion

R: the gas constant

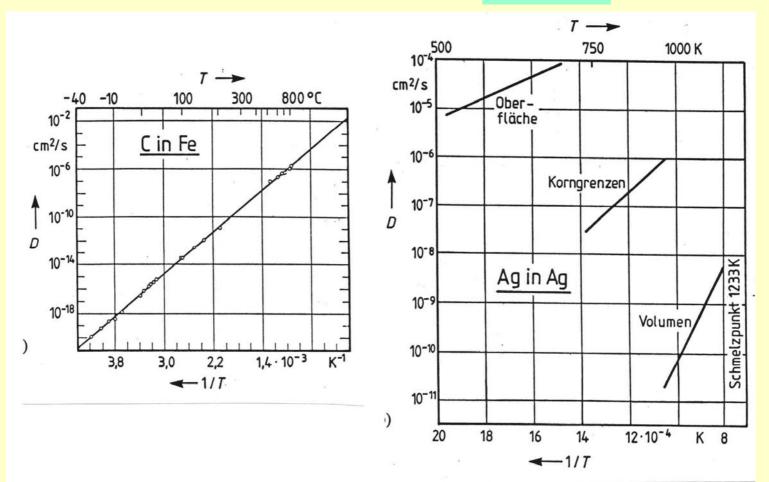
$$D = D_{\infty} \exp\left(-\frac{Q}{RT}\right)$$

The logarithmic representation of D verus 1/T is linear the slope corresponds to the activation energy Q and the intercept to D_{∞} .

Diffusion

C in Fe

Ag in Ag



NUCLEATION RATE

$$n = n_0 \exp\left(-\frac{\left(\Delta G_N + \Delta G_D\right)}{kT}\right)$$

Nucleation rate *n*

Nucleation rate =const. $x \exp\{-(\Delta G_N + \Delta G_D)/kT\}$

 ΔG_N = thermodynamic barrier to nucleation

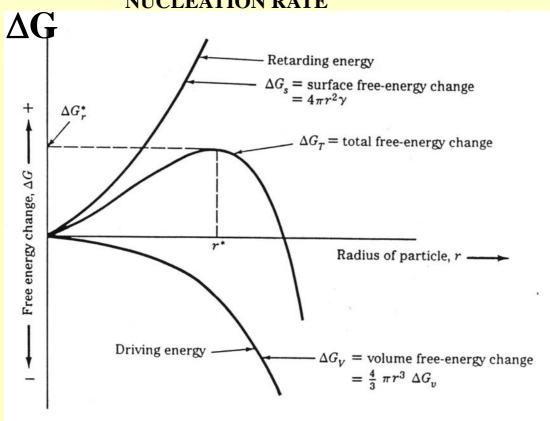
 ΔG_D = kinetic barrier to diffusion across the liquid/nucleus interface

$$\Delta G_{N} = \Delta G_{S} + 4/3\pi r^{3} \Delta G_{V}$$

 $\Delta G_{\rm S} = 4\pi r^2 \gamma$ surface free energy change positive $4/3\pi r^3 \Delta G_{\rm V}$ volume free energy change negative, 1 to s lowers energy

Nucleation rate n

NUCLEATION RATE



r: radius of spheric seed

r*: critical radius

(r>r* seed grows by itself)

 ΔG_N : total free energy change

 ΔG_s : <u>surface</u> free energy change

 ΔG_v : <u>volume</u> free energy change

$$\Delta G_{\rm N} = 4\pi r^2 \gamma + 4/3\pi r^3 \Delta G_{\rm V}$$

Solidification

$$\Delta G = 4/3 \pi r^3 \Delta G_v + 4 \pi r^2 \gamma$$

Volume free energy + surface energy

One solid phase changing to another

$$\Delta G = 4/3 \pi r^3 \Delta G_v + 4 \pi r^2 \gamma + 4/3 \pi r^3 \epsilon$$

- Volume energy + surface energy + strain energy
- the new solid does not take up the same volume as the old solid

Nucleation vs. Crystal Growth (solution or melt)

Undercooling – cooling below the melting point

relations between undercooling, nucleation rate and growth rate of the nuclei

large undercooling: <u>many</u> small nuclei

(spontaneous nucleation)

growth rate small - high viscosity, slow diffusion

small undercooling: <u>few</u> (evtl. small) nuclei

growth rate high – fast diffusion close to the m.p.

Nucleation vs. Crystal Growth

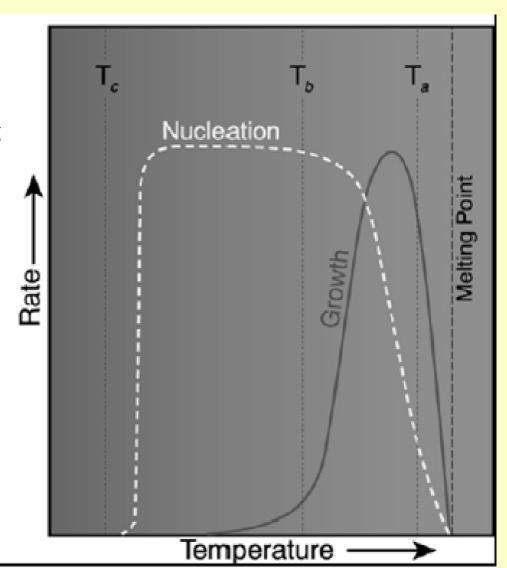
Rate of nucleation Rate of growth

T_a = small undercooling, slow cooling rate

Fast growth, slow nucleation = Few coarse crystals

T_b = larger undercooling, rapid cooling rate
Rapid nucleation, slow growth = many fine-grained crystals

T_c = very rapid cooling Nearly no nucleation = glass



NUCLEATION RATE

Nucleation requires structural similarity of reactants and products less reorganization energy = faster nucleation of product phase within reactants

MgO, Al₂O₃, MgAl₂O₄ example MgO (rock salt) and MgAl₂O₄ (spinel) similar ccp O²⁻ but distinct to hcp O²⁻ in Al₂O₃ phase

Spinel nuclei, matching of structure at MgO interface Oxide arrangement essentially continuous across MgO/MgAl₂O₄ interface

Bottom line: structural similarity of reactants and products promotes nucleation and growth of one phase within another Lattice of oxide anions, mobile Mg²⁺ and Al³⁺ cations

Topotactic and epitactic reactions
Orientation effects in the bulk and surface regions of solids
Implies structural relationships between reagent and product

Topotaxy occurs in bulk, 1-, 2- or 3-D Epitaxy occurs at interfaces, 2-D

Epitactic reactions

require 2-D structural similarity, lattice matching within 15% to tolerate oriented nucleation otherwise mismatch over large contact area, strained interface, missing atoms

Example: MgO/BaO, both rock salt lattices, cannot be lattice matched over large contact area

Lattice matched crystalline growth

Best with less than 0.1% lattice mismatch. Causes elastic strain at interface

Slight atom displacement from equilibrium position.

Strain energy reduced by misfit-dislocation

Creates dangling bonds, localized electronic states, carrier scattering by defects, luminescence quenching, killer traps, generally reduces efficacy of electronic and optical devices, can be visualized by HR-TEM imaging

Topotactic reactions

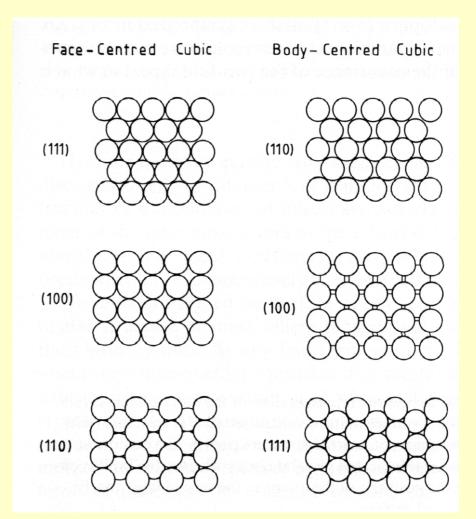
More specific, require interfacial and bulk crystalline structural similarity, lattice matching

Topotaxy: involves lock-and-key ideas of self-assembly, molecule recognition, host-guest inclusion, clearly requires available space or creates space in the process of adsorption, injection, intercalation etc.

Surface structure and reactivity

Nucleation depends on actual surface structure of reacting phases.

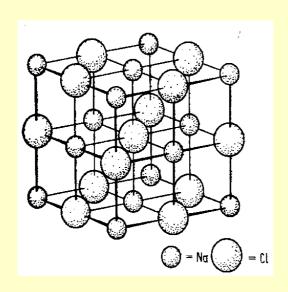
Different Miller index faces exposed, atom arrangements different, different surface structures, implies distinct surface reactivities.

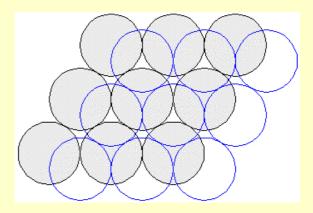


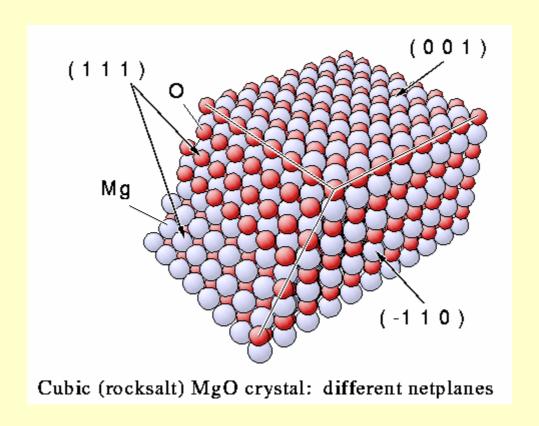
Example: MgO (rock salt)

{100} MgO alternating Mg²⁺, O²⁻ at corners of square grid

{111} MgO, Mg²⁺ or O²⁻ hexagonal arrangement







Different crystal habits possible, depends on rate of growth of different faces, octahedral, cubooctahedral, cubic possible and variants in between

CRYSTAL GROWTH

Most prominent surfaces, slower growth Growth rate of specific surfaces controls morphology Depends on area of a face, structure of exposed face, accessibility of a face, adsorption at surface sites, surface defects

Play major role in reactivity, nucleation, crystal growth, materials properties (electronic, optical, magnetic, charge-transport, mechanical, thermal, acoustical etc)

Azide Method

$$3 \text{ NaN}_3 + \text{NaNO}_2 \longrightarrow 2 \text{ Na}_2\text{O} + 5 \text{ N}_2$$

 $5 \text{ NaN}_3 + \text{NaNO}_3 \longrightarrow 3 \text{ Na}_2\text{O} + 8 \text{ N}_2$

9 NaN₃ + 3 NaNO₂ + 2 ZnO
$$\longrightarrow$$
 2 Na₆ZnO₄ + 15 N₂
8 NaN₃ + 4 NaNO₂ + Co₃O₄ \longrightarrow 3 Na₄CoO₄ + 14 N₂
2 NaN₃ + 4 CuO \longrightarrow 2 NaCu₂O₂ + 3 N₂

Self-Sustained High-Temperature Synthesis (SHS)

Mixing

Metal powders (Ti, Zr, Cr, Mo, W,) + other reactants

Pressing into pellets

Ignition by energy pulse (W wire)

S.S. reactor, under Ar

Exothermic reaction

Byproduct removal

SHS reactions:

- **6**^{**} heterogeneous
- exothermic, high temperatures, $T_f = 1500 3000$ °C
- **♦*** high thermal gradients
- **6**[₩] redox
- frontal mode, reaction wave velocity $u = 1 10 \text{ mm.s}^{-1}$
- **6**^{**} metastable phases

State of the substance in the reaction front:

$$solid \; (T_f < T_m, \, p < p_0) \;\; \text{,,solid flame"} \\ liquid, \, melt \; (T_f > T_m) \\ gaseous$$

Thermite reaction

$$\begin{array}{cccc} Zr + Fe_2O_3 & \longrightarrow & Zr_{1-x}Fe_xO_2 + Fe \\ Ti & + & C & \longrightarrow & TiC \\ Ti & + & B & \longrightarrow & TiB \end{array}$$

Self-Propagating Metathesis

Grinding of components in a glove box addition of NaCl, KCl or NH_4Cl as a heat sink, S.S. vessel, ignition by a resistively heated wire, reaction time 1 s, washing products with MeOH, water, drying

$$3 \operatorname{ZrCl_4} + 4 \operatorname{Na_3P} \longrightarrow 3 \operatorname{c-ZrP} + 12 \operatorname{NaCl} + \operatorname{P}$$

$$3 \text{ HfCl}_4 + 4 \text{ Li}_3 P \longrightarrow 3 \text{ c-HfP} + 12 \text{ LiCl} + P$$

c-ZrP and c-HfP hard and chemically inert materials, hexagonal to cubic transitions: ZrP 1425 °C, HfP 1600 °C

Self-Propagating Metathesis

Silicon production

$$Na_2SiF_6 + 4Na \longrightarrow 6NaF + Si$$

Hard materials production

$$TaCl_5 + Li_3N + NaN_3 + NH_4Cl \rightarrow c-TaN + LiCl + NaCl + N_2 + HCl$$

$$CrCl_3 + Li_3N + NH_4Cl \longrightarrow Cr + Cr_2N + c-CrN$$

$$CrI_3 + Li_3N \longrightarrow Cr_2N$$

$$CrI_3 + Li_3N + NH_4Cl \longrightarrow c-CrN$$

$$MoCl_5 + Li_3N \longrightarrow explosive$$

$$MoCl_5 + Ca_3N_2 + NH_4Cl \longrightarrow cubic \gamma - Mo_2N$$

Combustion Synthesis

Oxidizing reagents (metal nitrates) mixed with fuel (urea, glycine) by melting or in solution drying combustion ignited at 300-500 °C exothermic self-propagating non-explosive reaction (excess of fuel) reaction time 1 min, flame temperature 1000 °C product dry foam, crumbles to a fine powder.

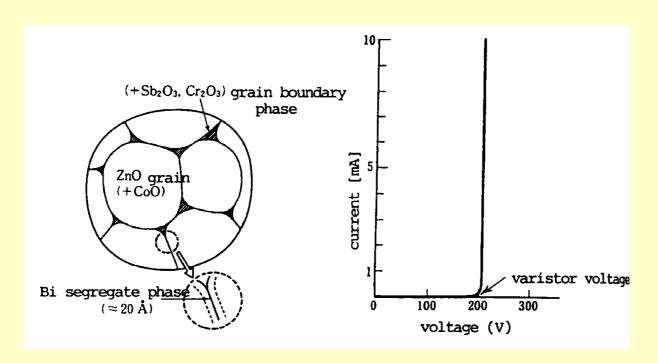
$$Zn(NO_3)_2.6H_2O + CO(NH_2)_2 \longrightarrow ZnO + N_2 + CO_2 + H_2O$$

Combustion Synthesis

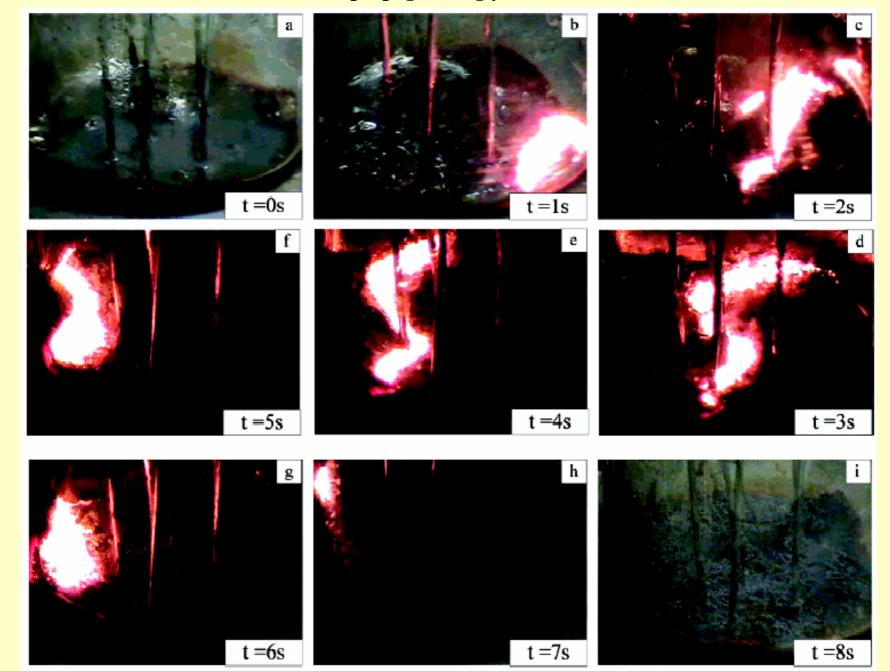
Examples

ZnO(90%) - Bi_2O_3 - Sb_2O_3

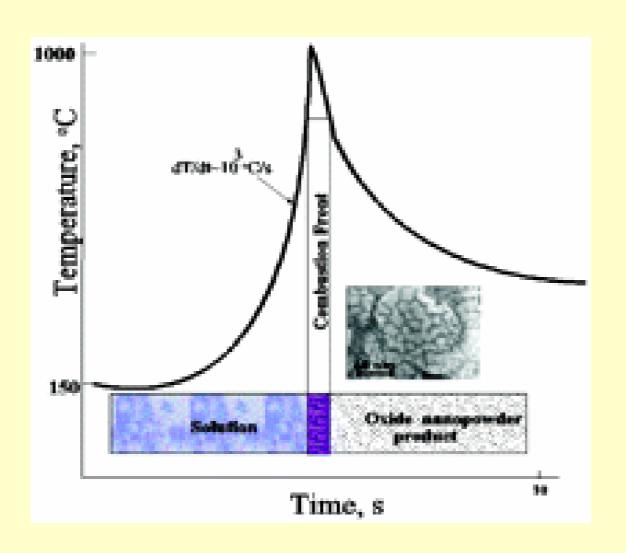
Non-Ohmic behavior $I = (U/C)^a$ C, a = constants, a = 50 Voltage stabilization, surge absorption



Reaction front propagation: glycine-iron nitrate



Self-Propagating Metathesis



Combustion Synthesis

Examples

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LiNO_3 + NH_4VO_3 + (NH_4)_2MoO_4 + glycine \rightarrow LiVMoO_6
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mixing 1:1:1 in aqueous solution, drying at 90 °C combustion at 250 °C calcination to LiVMoO $_6$ cathode material for Li-ion

Carbothermal Reduction

Acheson

$$SiO_2 + 3 C \xrightarrow{2000 \text{ K}} 2 CO + SiC \qquad \Delta H = 478 \text{ kJ}$$

 $3 SiO_2 + 6 C + 2 N_2 \longrightarrow 6 CO + Si_3N_4$

$$C + SiO_2 \longrightarrow SiO(g) + CO$$
 $SiO_2 + CO \longrightarrow SiO + CO_2$
 $C + CO_2 \longrightarrow 2 CO$
 $2 C + SiO \longrightarrow SiC + CO$

Carbothermal Reduction

Borides

$$TiO_{2} + B_{2}O_{3} + 5 C \xrightarrow{1300 \text{ K}} 5 CO + TiB_{2}$$

$$2 TiO_{2} + B_{4}C + 3 C \xrightarrow{2300 \text{ K}} 4 CO + 2 TiB_{2}$$

$$Al_{2}O_{3} + 12 B_{2}O_{3} + 39 C \xrightarrow{1820 \text{ K}} 2 AlB_{12} + 39 CO$$

Carbides

$$2 \text{ Al}_2\text{O}_3 + 9 \text{ C} \xrightarrow{2220 \text{ K}} \text{ Al}_4\text{C}_3 + 6 \text{ CO}$$

$$2 \text{ B}_2\text{O}_3 + 7 \text{ C} \xrightarrow{1820 \text{ K}} \text{ B}_4\text{C} + 6 \text{ CO}$$

$$W\text{O}_3 + 4 \text{ C} \xrightarrow{970 \text{ K}} \text{ WC} + 3 \text{ CO}$$

Nitrides

$$Al_2O_3 + N_2 + 3 C \xrightarrow{1970 \text{ K}} 2 \text{ AlN} + 3 CO$$

 $2 \text{ TiO}_2 + N_2 + 4 C \xrightarrow{1820 \text{ K}} 2 \text{ TiN} + 4 CO$

Fusion-Crystallization from Glass

Fusion-Crystallization from Glass

Mixing powders

Melting to glass: single phase, homogeneous (T, C), amorphous

Temperature limits: mp of reagents

volatility of reagents

Nucleation agent

Homogeneous nucleation, few crystal seeds

Slow transport of precursors to seed Lowest possible crystallization temperature

Crystallizing a glass above its glass transition Metastable phases accessible, often impossible to prepare by other methods

Fusion-Crystallization from Glass

Fusion-Crystallization from Glass

Production of window glass

Abrasive grains

$$Al_2O_3 + MgO \xrightarrow{2100 \text{ K}} \text{melt, solidify, crush, size}$$

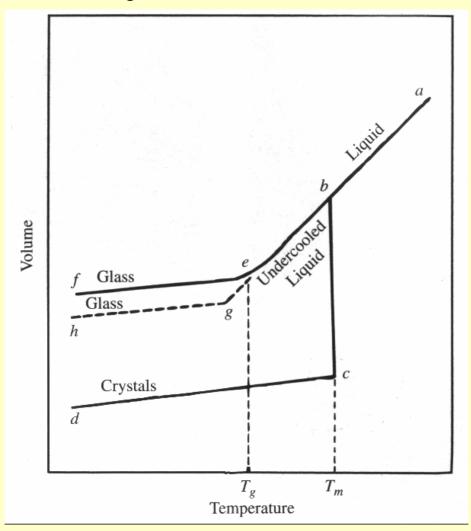
Crystallizing an inorganic glass, lithium disilicate

$$\text{Li}_2\text{O} + 2\text{SiO}_2 + \text{Al}_2\text{O}_3 \xrightarrow{1300 \text{ K, Pt crucible}} \text{Li}_2\text{Si}_2\text{O}_5$$

Li₂Si₂O₅ forms as a melt. Hold at 1100°C for 2-3 hrs. Homogeneous, rapid cooling, fast viscosity increase, quenches transparent glass

 $\text{Li}_2\text{Si}_2\text{O}_5$, glass 500-700°C, $\text{T}_g \sim 450$ °C from DSC $\rightarrow \text{Li}_2\text{Si}_2\text{O}_5$, crystals in 2-3 hrs., principle of crystallizing a glass above its glass transition

Fusion-Crystallization from Glass



DIRECT REACTION OF SOLIDS Fusion-Crystallization from Glass

Fusion-Crystallization from Glass

Glass Ceramics

polyxtalline materials made by controlled xtallization of glasses

Cooking utensils

 $\text{Li}_2\text{O/SiO}_2/\text{Al}_2\text{O}_3(>10\%)$ nucl. TiO_2 β -spodumene

Vacuum tube components

Li₂O/SiO₂/Al₂O₃(<10%) nucl. P₂O₅ Li-disilicate, quartz

Missile radomes

MgO/SiO₂/Al₂O₃ nucl. TiO₂ cordierite, cristobalite