## **Precursor Methods**

**Goals – decrease diffusion paths, shorten reaction times and temperatures** 

Intimate mixing of components in solution, precipitation, filtration, washing, drying, calcination

**●**<sup>\*</sup> High degree of homogenization

**●**<sup>\*</sup> Large contact area

**\*** Reduction of diffusion distances

**●**<sup>\*</sup> Faster reaction rates

**•**\* Lower reaction temperatures

**●**<sup>\*</sup> Metastable phases, smaller grain size, larger surface area

**Coprecipitation applicable to nitrates, acetates, oxalates, hydroxides, alkoxides, beta-diketonates** 

<b>Requires:</b>	similar salt solubilities
	similar precipitation rates
	no supersaturation
Washing:	water, organic solvents
Drying:	evaporation
	azeotropic distillation
	freeze-drying

Disadvantage: difficult to prepare high purity, accurate stoichiometric phases if solubilities do not match

#### **Spinels**

oxalates:  $Zn(CO_2)_2/Fe_2[(CO_2)_2]_3/H_2O 1 : 1 mixing, H_2O evaporation, salts coprecipitation Solid-solution mixing on atomic scale, filter, calcine in air$ 

 $Zn(CO_2)_2 + Fe_2[(CO_2)_2]_3 \rightarrow ZnFe_2O_4 + 4CO + 4CO_2$ 

Al<sub>2</sub>O<sub>3</sub> Bayer Process

**BaTiO<sub>3</sub>** 

BaCl<sub>2</sub> + TiOCl<sub>2</sub> + 2 H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> + 4 H<sub>2</sub>O + Ln dopants BaTiO(C<sub>2</sub>O<sub>4</sub>)<sub>2</sub>.4H<sub>2</sub>O + 4 HCl filtration, washing, drying, calcination @ 730 °C

Spinel

 $Al(NO_3)_3 + Mg(NO_3)_2 + H_2O$  freeze-drying gives amorphous mixture, calcination @ 800 °C !!! low T

 $Mg(NO_3)_2 + 2 Al(NO_3)_3 \longrightarrow MgAl_2O_4 + 6 NO_x + (10-3x)O_2$ random

Ruby Ion exchange  $Al(NO_3)_3 + Cr(NO_3)_3 \longrightarrow Al(OH)_3 + Cr(OH)_3$  sol

freeze drying gives solid (Al/Cr)(OH)<sub>3</sub> @ LN<sub>2</sub> temperature, 5 Pa anealing @ 950 °C for 2.5 h gives solid solution Al<sub>2-x</sub>Cr<sub>x</sub>O<sub>3</sub>

Zirconia

 $ZrSiO_4(zircon) + NaOH \longrightarrow Na_2ZrO_3 + Na_2SiO_3 \longrightarrow$ 

 $\operatorname{ZrOCl}_2 \xrightarrow{\operatorname{OH}^2, \operatorname{YCl}_3} \operatorname{Zr}(\operatorname{OH})_4 / \operatorname{Y}(\operatorname{OH})_3 \xrightarrow{\operatorname{azeot. dist.}} \operatorname{nano-Y/ZrO}_2$ 

**High-T**<sub>c</sub> **Superconductors** 

 $La^{3+} + Ba^{2+} + Cu^{2+} + H_2C_2O_4 \longrightarrow ppt \xrightarrow{1373 \text{ K}} La_{1.85}Ba_{0.15}CuO_4$ 

Magnetic garnets, tunable magnetic materials

 $Y(NO_3)_3 + Gd(NO_3)_3 + FeCl_3 + NaOH \rightarrow Y_xGd_{3-x}Fe_5O_{12}$ 

Firing @ 900 °C, 18-24 hrs, pellets, regrinding, repelletizing, repeated firings, removes REFeO<sub>3</sub> perovskite impurity Isomorphous replacement of  $Y^{3+}$  for  $Gd^{3+}$  on dodecahedral sites, solid solution, similar rare earth ionic radii complete family accessible, 0 < x < 3,  $2Fe^{3+}$  O<sub>h</sub> sites,  $3Fe^{3+}$  T<sub>d</sub> sites,  $3RE^{3+}$  dodecahedral sites

## **Pechini and Citrate Gel Method**

Aqueous	solution	of metal	l ions
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**Chelate formation with citric acid** 

Polyesterification with polyfunctional alcohol on heating

Further heating leads to resin, transparent glassy gel calcination provides oxide powder

Control of stoichiometry by initial reagent ratio

**Complex compositions, mixture of metal ions** 

Good homogeneity, mixing at the molecular level

Low firing temperatures

#### **Pechini and Citrate Gel Method**

BaTiO<sub>3</sub> by conventional powder method at 1200 °C

 $Ba^{2+} + Ti(O^{i}Pr)_{4} + citric acid at 650 °C$ 

 $Sc_2O_3 + 6 \text{ HCOOH} \longrightarrow 2Sc(\text{HCOO})_3 + 3 \text{ H}_2\text{O}$  $MnCO_3 + 2 \text{ HCOOH} \longrightarrow Mn(\text{HCOO})_2 + CO_2 + \text{H}_2\text{O}$ 

added to citric acid, water removal, calcination @ 690 °C gives ScMnO<sub>3</sub> without citric acid only mixture of Sc<sub>2</sub>O<sub>3</sub> and Mn<sub>2</sub>O<sub>3</sub> is formed

## **Double Salt Precursors**

Double salts of known and controlled stoichiometry such as:  $Ni_3Fe_6(CH_3COO)_{17}O_3(OH).12Py$ 

Burn off organics 200-300 °C, then 1000 °C in air for 2-3 days Product highly crystalline phase pure  $NiFe_2O_4$  spinel Good way to make chromite spinels, important tunable magnetic materials

Juggling the electronic-magnetic properties of the  $\rm O_h$  and  $\rm T_d$  ions in the spinel lattice

<b>Chromite spinel</b>	Precursor	Ignition T, °C
MgCr <sub>2</sub> O <sub>4</sub>	(NH <sub>4</sub> ) <sub>2</sub> Mg(CrO <sub>4</sub> ) <sub>2</sub> .6H <sub>2</sub> O	1100-1200
NiCr <sub>2</sub> O <sub>4</sub>	(NH <sub>4</sub> ) <sub>2</sub> Ni(CrO <sub>4</sub> ) <sub>2</sub> .6H <sub>2</sub> O	1100
MnCr <sub>2</sub> O <sub>4</sub>	MnCr <sub>2</sub> O <sub>7</sub> .4C <sub>5</sub> H <sub>5</sub> N	1100
CoCr <sub>2</sub> O <sub>4</sub>	CoCr <sub>2</sub> O <sub>7</sub> .4C <sub>5</sub> H <sub>5</sub> N	1200
CuCr <sub>2</sub> O <sub>4</sub>	$(NH_4)_2Cu(CrO_4)_2.2NH_3$	700-800
ZnCr <sub>2</sub> O <sub>4</sub>	(NH <sub>4</sub> ) <sub>2</sub> Zn(CrO <sub>4</sub> ) <sub>2</sub> . 2NH <sub>3</sub>	1400
FeCr <sub>2</sub> O <sub>4</sub>	$(NH_4)_2Fe(CrO_4)_2$	1150

#### **Single Source Precursor**

Compounds containing desired elements in a proper stoichiometric ratio

Easy chemical pathway for ligand removal



**Vegard law behavior:** 

Any property P of a solid-solution member is the atom fraction weighted average of the end-members

The composition of the A<sub>1-x</sub>B<sub>x</sub> alloy can be calculated from Vegard's law

The lattice parameter of a solid solution alloy will be given by a linear dependence of lattice parameter on composition:

 $a(A_{1-x}B_x) = x a(B) + (1-x) a(A)$ 

 $c(CdSe_{1-x}S_x) = x c(CdS) + (1-x) c(CdSe)$ 



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 $P(Y_{x}Ce_{!-x}RhIn_{5}) = x P(Y_{x}Ce_{!-x}RhIn_{5}) + (1-x) P(Y_{x}Ce_{!-x}RhIn_{5})$ 

Any property P of a solid-solution member is the atom fraction weighted average of the end-members

Tetragonal lattice constant a as a function of Y concentration x for the  $Ce_{1-x}Y_{x}RhIn_{5}$  system



A linear relationship exists between the concentration of the substitute element and the size of the lattice parameters

The direction of the linear relationship, increasing or decreasing, depends upon the system being analyzed

As the concentration of Y is increased, lattice constant *a* decreases, implying the cell is contracting along the *a* axis

**Vegard law behavior:** 

$$P(Y_{x}Gd_{3-x}Fe_{5}O_{12}) = x/3 P(Y_{3}Fe_{5}O_{12}) + (3-x)/3 P(Gd_{3}Fe_{5}O_{12})$$

Any property P of a solid-solution member is the atom fraction weighted average of the end-members

Tunable magnetic properties by tuning the x value in the binary garnet  $Y_xGd_{3-x}Fe_5O_{12}$ 

- 3 T<sub>d</sub> Fe<sup>3+</sup> sites, 5 UPEs
- 2 O<sub>h</sub> Fe<sup>3+</sup> sites, 5UPEs

Ferrimagnetically coupled material, oppositely aligned electron spins on the  $T_d$  and  $O_h$  Fe<sup>3+</sup> magnetic sublattices

Counting spins  $Y_3Fe_5O_{12}$  ferrimagnetic at low T:  $3 \times 5 - 2 \times 5 = 5UPEs$ Counting spins  $Gd_3Fe_5O_{12}$  ferrimagnetic at low T:  $3 \times 7 - 3 \times 5 + 2 \times 5 = 16$  UPEs

 $Y_xGd_{3-x}Fe_5O_{12}$  creates a tunable magnetic garnet that is strongly temperature and composition dependent,

applications in permanent magnets, magnetic recording media, magnetic bubble memories and so forth, similar concepts apply to magnetic spinels





Molten salts (inert or reactive), oxides, metals MNO<sub>3</sub>, MOH, (M = alkali metal) FLINAK: LiF-NaF-KF  $M_2Q_x$  (M = alkali metal, Q = S, Se, Te)

molten salts ionic, low mp, eutectics, completely ionized act as solvents or reactants, T = 250-550 °C enhanced diffusion, reduced reaction temperatures in comparison with powder method products finely divided solids, high surface area (SA) slow cooling to grow crystals separation of water insoluble product from a water soluble flux incorporation of the molten salt ions in product prevented by using salts with ions of much different sizes than the ones in the product (PbZrO<sub>3</sub> in a B<sub>2</sub>O<sub>3</sub> flux)

Lux-Flood formalism oxide = strong base acid = oxide acceptor  $A + OB \longrightarrow AO + B$ base = oxide donor

700 K  $Zr(SO_4)_2 + eut. (Li/K)NO_3 \longrightarrow ZrO_2$ 540 K  $Zr(SO_4)_2 + eut. (Li/K)NO_2 \longrightarrow ZrO_2$  $ZrOCl_2 + eut. (Na/K)NO_3 \xrightarrow{520 \text{ K}} ZrO_2 \text{ amorph.} \longrightarrow t- ZrO_2$ 720 K  $ZrOCl_2 + YCl_3 + eut. (Na/K)NO_3 \longrightarrow ZrO_2$ 

 $BaCO_3 + SrCO_3 + TiO_2 + eut.$  (Na/K)OH



 $NH_4H_2PO_4 + (Na/K)NO_3 + M(NO_3)_2 \longrightarrow (Na/K)MPO_4$ 

4 SrCO<sub>3</sub> + Al<sub>2</sub>O<sub>3</sub> + Ta<sub>2</sub>O<sub>5</sub> \_\_\_\_\_ Sr<sub>2</sub>AlTaO<sub>6</sub> 900 °C in SrCl<sub>2</sub> flux 1400 °C required for a direct reaction

 $K_2Te_x + Cu \longrightarrow K_2Cu_5Te_5$   $K_2Te_x$  reactive flux, 350 °C

**Electrolysis in molten salts** 

**Reduction of TiO<sub>2</sub> pellets to Ti sponge in a CaCl<sub>2</sub> melt at 950 °C** 

O<sup>2-</sup> dissolves in CaCl<sub>2</sub>, diffuses to the graphite anode

insulating  $TiO_2 \rightarrow TiO_{2-x}$  conductive

graphite anode anodic oxidation  $2 O^{2-} \rightarrow O_2 + 4 e^{-}$ 

cathode TiO<sub>2</sub> pellet cathodic reduction

 $Ti^{4+} + 4e^{-} \rightarrow Ti$ 

**Organic cations (containing N, P)** 

Inorganic anions: Cl<sup>-</sup>, AlCl<sub>4</sub><sup>-</sup>, Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup>, Al<sub>3</sub>Cl<sub>10</sub><sup>-</sup>, PF<sub>6</sub><sup>-</sup>, SnCl<sub>3</sub><sup>-</sup>, BCl<sub>3</sub><sup>-</sup>, BF<sub>4</sub><sup>-</sup>, NO<sub>3</sub><sup>-</sup>, OSO<sub>2</sub>CF<sub>3</sub><sup>-</sup> (triflate), CH<sub>3</sub>C<sub>6</sub>H<sub>4</sub>SO<sub>3</sub><sup>-</sup>, N(SO<sub>2</sub>CF<sub>3</sub>)<sub>2</sub><sup>-</sup>, PO<sub>4</sub><sup>-3-</sup>



- Oldest known (1914) :  $EtNH_3^+NO_3^-$  mp 12 °C
- →Liquids at room temperature or low mp
- →Thermal operating range from -40 °C to 400 °C
- → Higly polar, noncoordinating, completely ionized
- →Nonvolatile no detectable vapor pressure
- →Nonflamable, nonexplosive, nonoxidizing, high thermal stability
- →Electrochemical window > 4V (not oxidized or reduced)
- →Immiscible with organic solvents
- →Hydrophobic IL immiscible with water





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#### **Synthesis of Ionic Liquids**

 $NR_3 + RCl \rightarrow [NR_4]^+ Cl^-$ 

Aluminates  $[NR_4]^+ Cl^- + AlCl_3 \rightarrow [NR_4]^+ [AlCl_4]^-$ 

Metal halide elimination  $[NR_4]^+ Cl^- + MA \rightarrow MCl + [NR_4]^+ A^-$ 

Reaction with an acid  $[NR_4]^+ Cl^- + HA \rightarrow HCl + [NR_4]^+ A^-$ 

Ion exchange [NR₄]<sup>+</sup> Cl<sup>-</sup> + Ion exchanger A → [NR₄]<sup>+</sup> A<sup>-</sup>

## Halogenoaluminate(III) Ionic Liquids

The most widely studied class of IL

High sensitivity to moisture – handling under vacuum or inert atmosphere in glass/teflon

 $RCl + AlCl_3 \leftrightarrows R^+ [AlCl_4]^ 2 [AlCl_4]^- \leftrightarrows [Al_2Cl_7]^- + Cl^-$  autosolvolysis  $K_{eq} = 10^{-16}$  to  $10^{-17}$  at 40 °C

  $2 [Al_2Cl_7]^- \leftrightarrows [Al_3Cl_{10}]^- + [AlCl_4]^-$  

 Acidic: excess of  $AlCl_3$  as  $[Al_2Cl_7]^ x(AlCl_3) > 0.5$  

 Basic: excess of  $Cl^ x(AlCl_3) < 0.5$  

 Neutral:  $[AlCl_4]^ x(AlCl_3) = 0.5$ 

## **Equilibria in Halogenoaluminate(III) IL**



#### Halogenoaluminate(III) Ionic Liquids

2  $[AlCl_4]^- \leftrightarrows [Al_2Cl_7]^- + Cl^-$  autosolvolysis  $K_{eq} = 10^{-16}$  to  $10^{-17}$  at 40 °C Acidic IL with an excess of AlCl<sub>3</sub>

 $HCl + [Al_2Cl_7]^- \leftrightarrows H^+ + 2 [AlCl_4]^-$ 

**Proton extremely poorly solvated = high reactivity** 

Superacid [EMIM]Cl/AlCl<sub>3</sub>/HCl  $H_0 = -19$  (HSO<sub>3</sub>F:  $H_0 = -15$ )

Latent acidity

 $MCl + [Al_2Cl_7]^- \leftrightarrows M^+ + 2 [AlCl_4]^-$  buffered IL

 $\mathbf{B} + \mathbf{M}^+ + [\mathbf{AlCl}_4]^- \leftrightarrows \mathbf{MCl} + \mathbf{B} - \mathbf{AlCl}_3$ 

## **Superacidity**



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## Superacidic [EMIM]Cl/AlCl<sub>3</sub>/HCl



I = not protonated II = slightly protonated III and IV = 10-20 % V = 75-90% VI-VIII = nearly completely IX and X = completely

log K<sub>b</sub> in HF

#### **Completely inorganic ionic liquids**

Compound	mp (K)	Compound	mp (K)
Na <sub>13</sub> [La(TiW <sub>11</sub> O <sub>39</sub> ) <sub>2</sub> ]	253.0	Na <sub>13</sub> [Tm(TiW <sub>11</sub> O <sub>39</sub> ) <sub>2</sub> ]	260.2
Na <sub>13</sub> [Ce(TiW <sub>11</sub> O <sub>39</sub> ) <sub>2</sub> ]	263.0	Na <sub>13</sub> [Yb(TiW <sub>11</sub> O <sub>39</sub> ) <sub>2</sub> ]	267.2
Na <sub>13</sub> [Pr(TiW <sub>11</sub> O <sub>39</sub> ) <sub>2</sub> ]	253.0	Na <sub>5</sub> [CrTiW <sub>11</sub> O <sub>39</sub> ]	261.5
Na <sub>13</sub> [Sm(TiW <sub>11</sub> O <sub>39</sub> ) <sub>2</sub> ]	256.0	Na <sub>5</sub> [MnTiW <sub>11</sub> O <sub>39</sub> ]	253.0
Na <sub>13</sub> [Gd(TiW <sub>11</sub> O <sub>39</sub> ) <sub>2</sub> ]	265.1	Na <sub>5</sub> [FeTiW <sub>11</sub> O <sub>39</sub> ]	257.6
Na <sub>13</sub> [Dy(TiW <sub>11</sub> O <sub>39</sub> ) <sub>2</sub> ]	265.2	Na <sub>6</sub> [ZnTiW <sub>11</sub> O <sub>39</sub> ]	257.4
Na <sub>13</sub> [Er(TiW <sub>11</sub> O <sub>39</sub> ) <sub>2</sub> ]	261.0		

## **Melting Point of Ionic Liquids**

Melting point is influenced by:

Cation – low symmetry, weak imtermolecular interactions, good distribution of charge Anion – increasing size leads to lower mp Composition – Phase diagram



# **Melting Point of Ionic Liquids**

Me <sup>-N</sup> , X <sup>-</sup>			
R	х	mp/°C	
Me Et n-Bu Et Et Et Et Et Et Et n-Bu	Cl Cl NO <sub>3</sub> AlCl <sub>4</sub> BF <sub>4</sub> CF <sub>3</sub> SO <sub>3</sub> (CF <sub>3</sub> SO <sub>3</sub> ) <sub>2</sub> N CF <sub>3</sub> CO <sub>2</sub> CF <sub>3</sub> SO <sub>3</sub>	125 87 65 38 7 6 -9 -3 -14 16	

## **Density of Ionic Liquids**

The density of IL decreases as the bulkiness of the organic cation increases:



### **Viscosity of Ionic Liquids**

The viscosity of IL depends on:

van der Waals interactions

**H-bonding** 

Anion [A]-	$\eta  [ m cP]$
$CF_3SO_3^-$ $n-C_4F_9SO_3^-$ $CF_3COO^-$ $n-C_3F_7COO^-$ $(CF_3SO_2)_2N^-$	90 373 73 182 52

## **Solubility in/of Ionic Liquids**

```
Variation of the alkyl group
Increasing nonpolar character of the cation increases solubility of
nonpolar solutes.
```

Water solubility depends on the anion water-soluble [BMIM] Br, CF<sub>3</sub>COO, CF<sub>3</sub>SO<sub>3</sub> Water-immiscilble [BMIM] PF<sub>6</sub> (CF<sub>3</sub>SO<sub>2</sub>)<sub>2</sub>N

IL miscible with organic solvent IF their dielectric constant is above a certain limit given by the cation/anion combination

```
Polarity by E_{(T)}(30) scale
```

[EtNH<sub>3</sub>][NO<sub>3</sub>] 0.95 between CF<sub>3</sub>CH<sub>2</sub>OH and water

[BMIM] PF<sub>6</sub> as methanol

#### **Solubility in/of Ionic Liquids**



## **Applications of Ionic Liquids**

Electrodeposition of metals and alloys (also nanoscopic) Al, CoAl<sub>x</sub>, CuAl<sub>x</sub>, FeAl<sub>x</sub>, AlTi<sub>x</sub>

Semiconductors Si, Ge, GaAs, InSb, CdTe

Electrodeposition of a Bi-Sr-Ca-Cu alloy (precursor to SC oxides)

Melt of MeEtImCl at 120 °C

BiCl<sub>3</sub>, SrCl<sub>2</sub>, CaCl<sub>2</sub>, CuCl<sub>2</sub> dissolve well

 $\begin{array}{cccc} Constituent & BiCl_3 & SrCl_2 & CaCl_2 & CuCl_2 \\ Concentration & 0.068 & 0.50 & 0.18 & 0.050 \\ (mol \ kg^{-1} \ MeEtImCl) & & & & & \\ \end{array}$ 

Substrate Al -1.72 V vs the Ag/Ag<sup>+</sup> reference electrode

#### **Applications of Ionic Liquids**

**Biphasic solvent systems** 

**Preparation of aerogels** 

 $2 \text{ HCOOH} + \text{Si}(\text{OMe})_4 \longrightarrow \text{ag-SiO}_2 + 2 \text{ MeOH} + 2 \text{ HCOOMe}$ 

Natural gas sweetening (H<sub>2</sub>S, CO<sub>2</sub> removal)

**Electrolytes in batteries or solar cells** 

Dissolving spent nuclear fuel  $(U^{4+} \text{ oxidized to } U^{6+})$ 

Extraction

**Enyzme activity** 

## **Applications of Ionic Liquids**

Olefin polymerization Ethene + TiCl<sub>4</sub> + AlEtCl<sub>2</sub> in acidic IL Ethene + Cp<sub>2</sub>TiCl<sub>2</sub> + Al<sub>2</sub>Me<sub>3</sub>Cl<sub>3</sub> in acidic IL

 $Cp_{2}TiCl_{2} + [cation]^{+}[Al_{2}Cl_{7}]^{-} \leftrightarrows [Cp_{2}TiCl]^{+} + [cation]^{+} + 2 [AlCl_{4}]^{-}$ 

Olefin hydrogenation Cyclohexene + H<sub>2</sub> + [RhCl(PPh<sub>3</sub>)<sub>3</sub>] (Wilkinson's catalyst)