

LOSCHMIDT  
LABORATORIES



# Enzyme Kinetics

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# OUTLINE

- ENZYME KINETICS
- STEADY-STATE vs. TRANSIENT KINETICS
- MATHEMATICS AND SOFTWARES
- RAPID MIXING TECHNIQUES
- KINETIC MECHANISMS
- KINETICS IN PROTEIN ENGINEERING

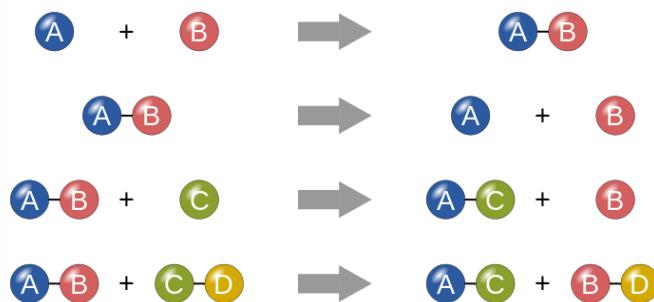
# ENZYME KINETICS

- ❑ **KINETICS** - study of motion and its causes

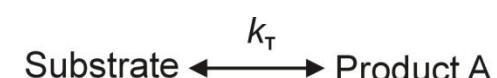
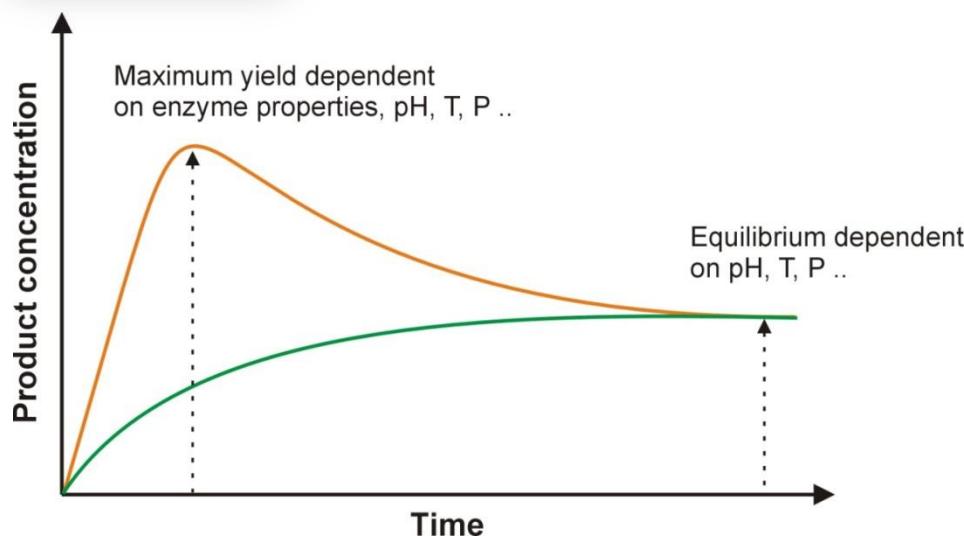


# ENZYME KINETICS

- **KINETICS** - study of motion and its causes
- **(BIO)CHEMICAL KINETICS** - rate of reactions/interactions

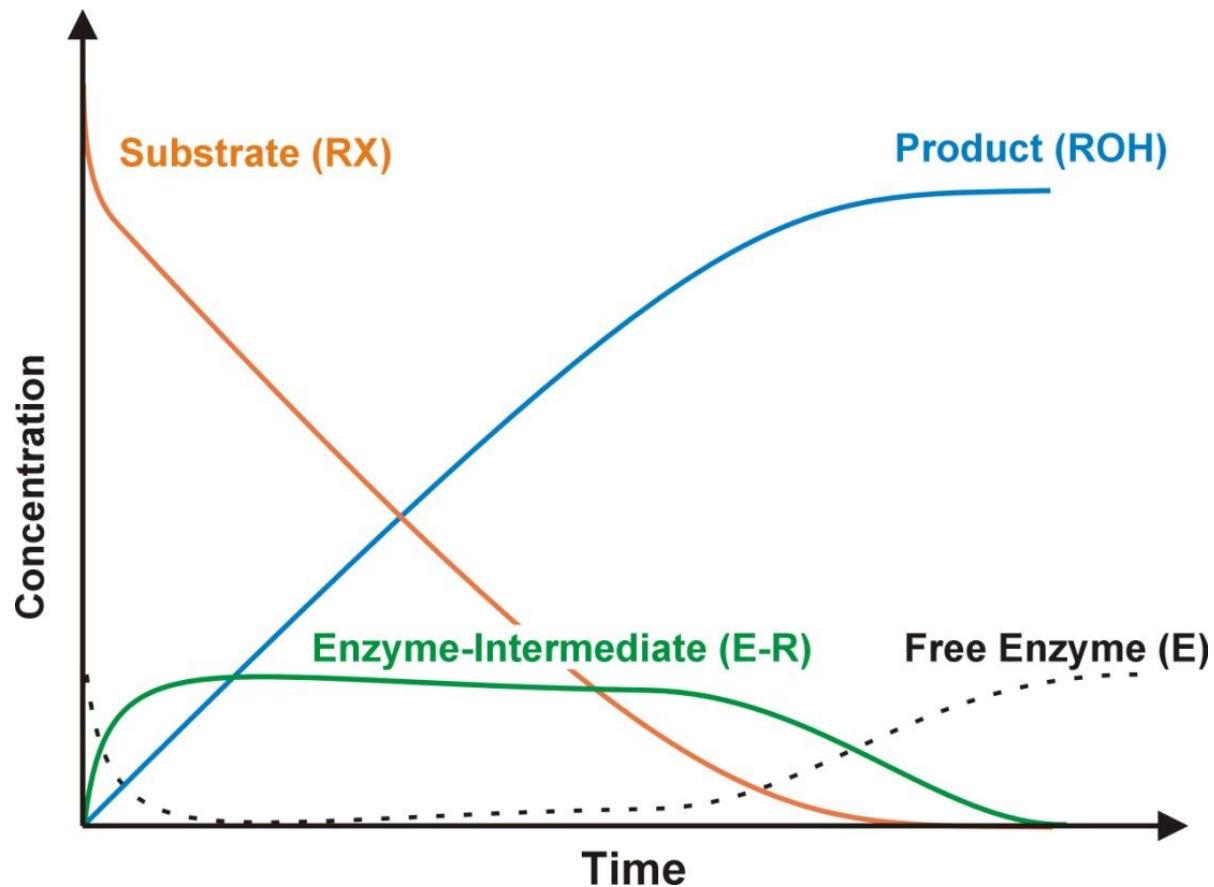


- chemical kinetics
- enzyme kinetics
- binding kinetics
- (un)folding kinetics
- pharmacokinetics



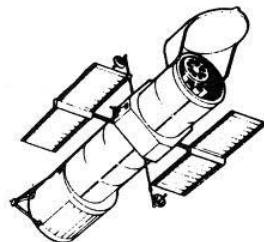
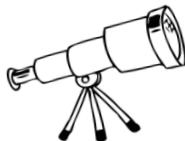
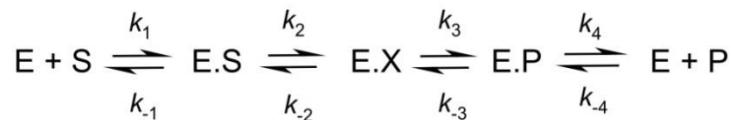
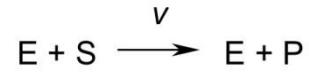
Hydrolytic product

# ENZYME REACTION



# STEADY-STATE vs. TRANSIENT

- ACTIVITY ANALYSIS
- STEADY-STATE KINETICS
- TRANSIENT KINETICS

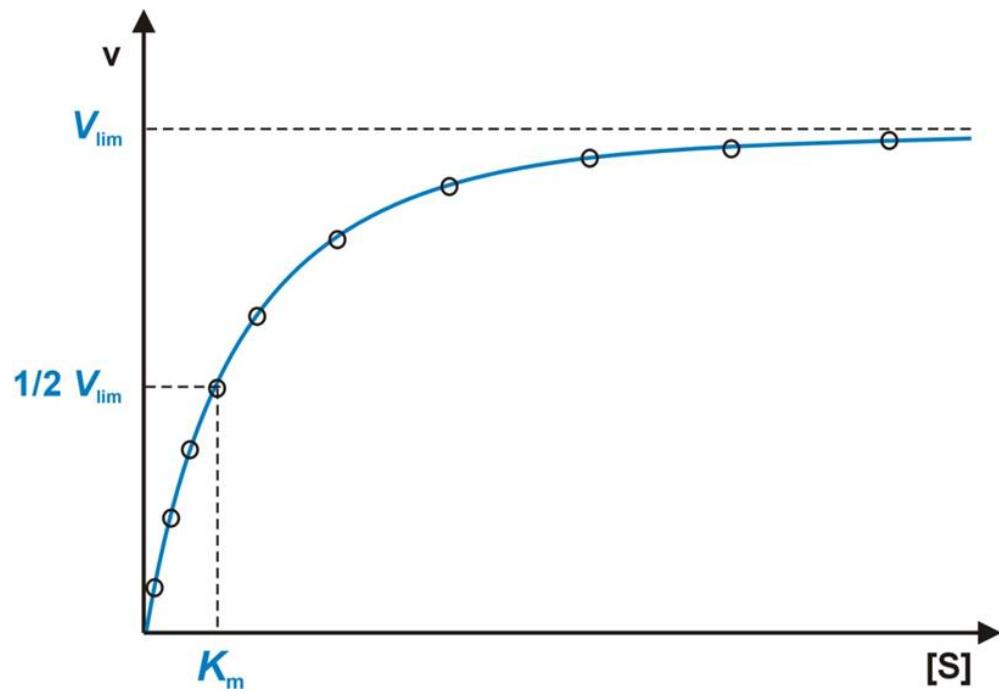
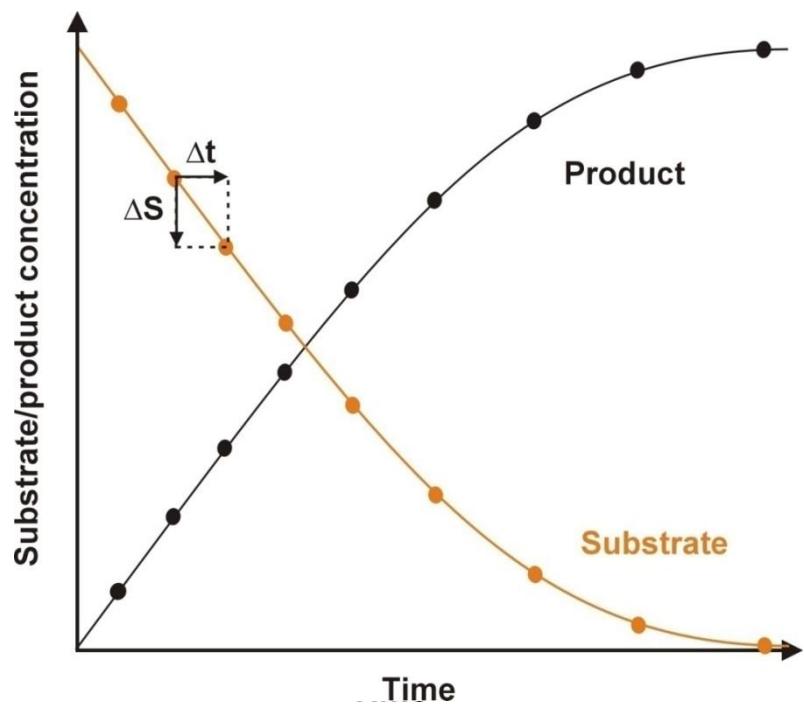


$$K_m = \frac{k_{-1}.(k_{-2}.(k_{-3} + k_4) + k_3.k_4) + k_2.k_3.k_4}{k_1.((k_2 + k_{-2}).(k_{-3} + k_4) + k_2.k_3 + k_3.k_4)}$$

$$k_{cat} = \frac{k_2.k_3.k_4}{(k_2 + k_{-2}).(k_{-3} + k_4) + k_2.k_3 + k_3.k_4}$$

# STEADY-STATE KINETICS

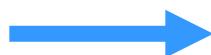
- ACTIVITY ANALYSIS
- MICHAELIS-MENTEN KINETICS



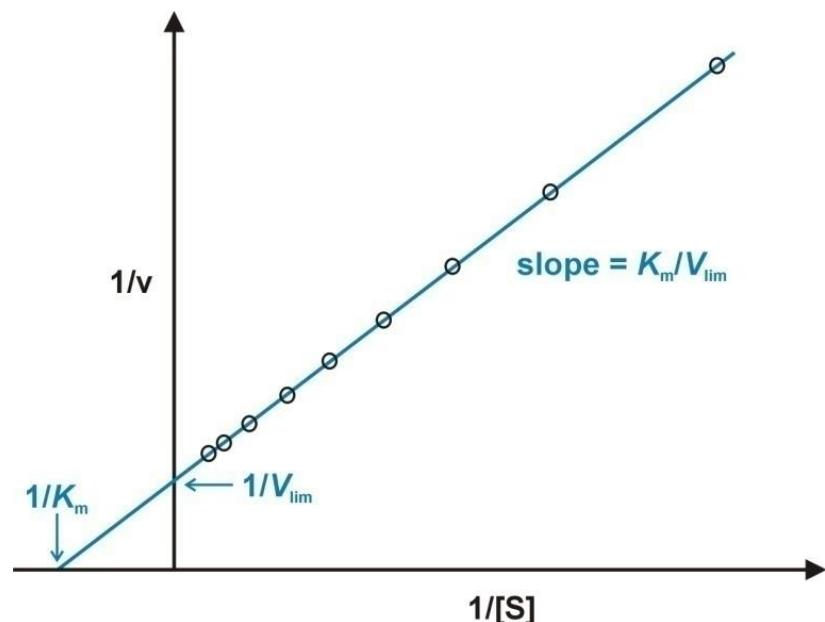
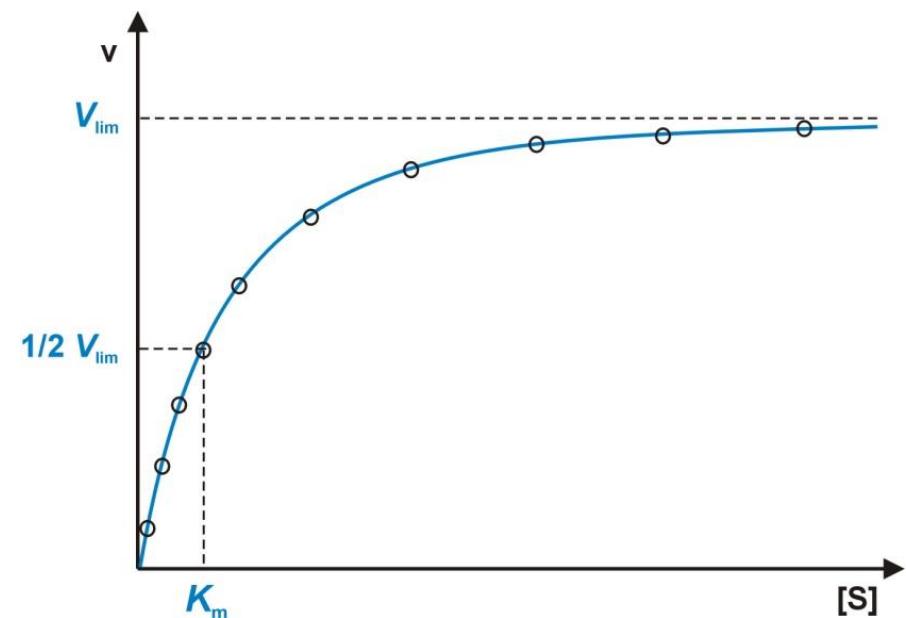
# STEADY-STATE KINETICS

## □ linearization

$$v = \frac{k_{\text{cat}} \cdot [S]}{K_m + [S]}$$



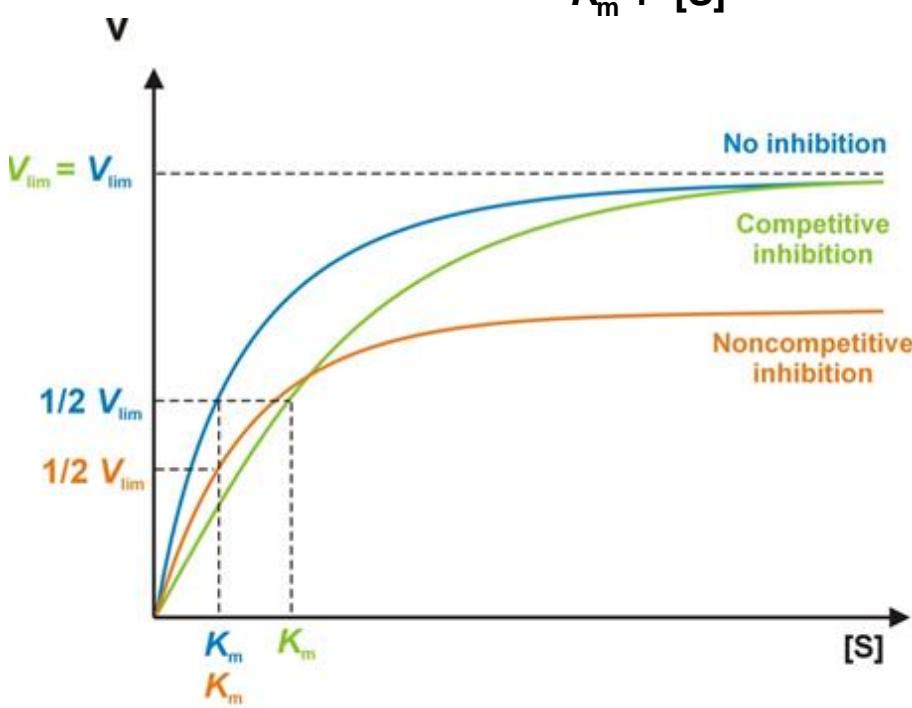
$$\frac{1}{v} = \frac{1}{V_{\text{lim}}} + \frac{K_m}{V_{\text{lim}}} \cdot \frac{1}{[S]}$$



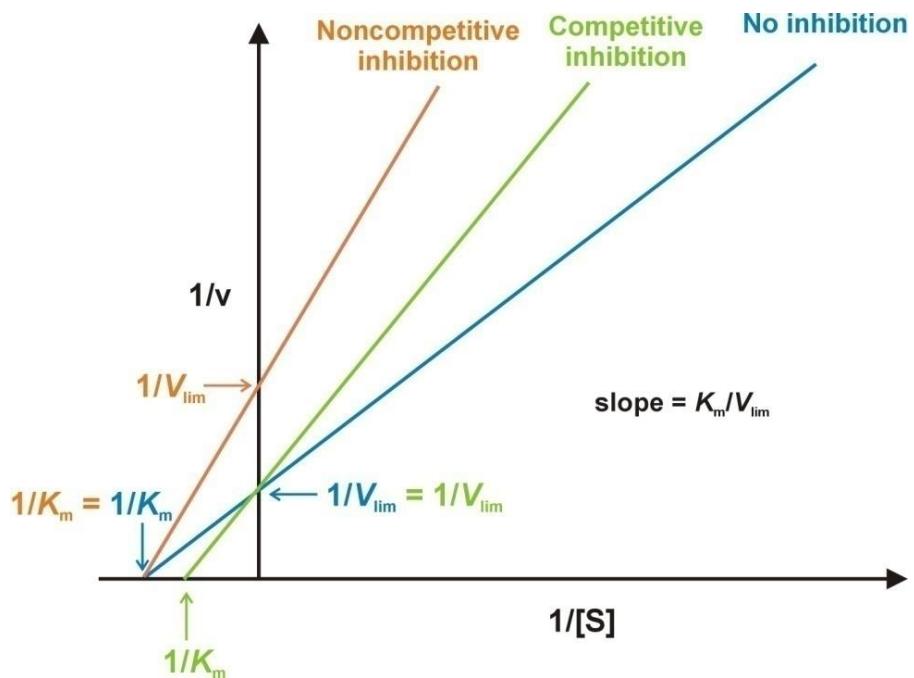
# STEADY-STATE KINETICS

## □ linearization

$$v = \frac{k_{\text{cat}} \cdot [S]}{K_m + [S]}$$



$$\frac{1}{v} = \frac{1}{V_{\text{lim}}} + \frac{K_m}{V_{\text{lim}}} \cdot \frac{1}{[S]}$$



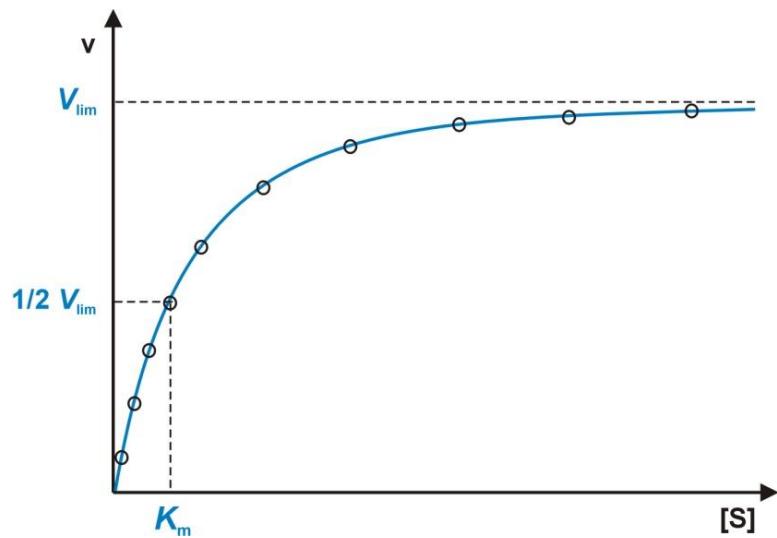
# STEADY-STATE KINETICS



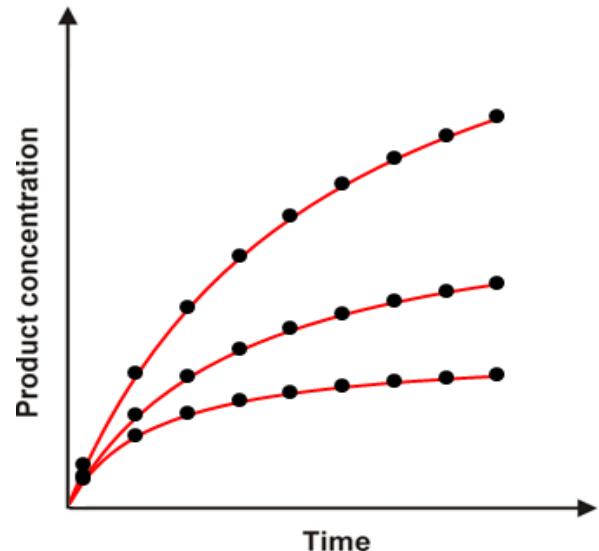
- linearization
- nonlinear regression (e.g., SigmaPlot, Origin, EnzFitter)
- numerical simulation (e.g., Gepasy, DynaFit, Kintek Explorer)



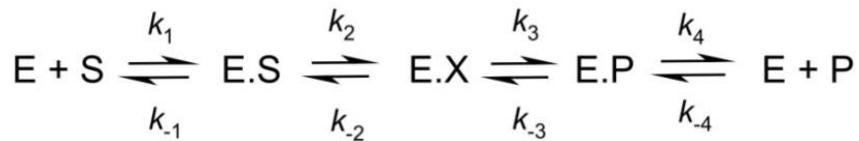
$$v = \frac{k_{\text{cat}} \cdot [S]}{K_m + [S]}$$



$$\begin{aligned}\frac{d[S]}{dt} &= -k_1 \cdot [E] \cdot [S] + k_{-1} \cdot [ES] \\ \frac{d[ES]}{dt} &= k_1 \cdot [E] \cdot [S] - k_{-1} \cdot [ES] \\ \frac{d[P]}{dt} &= k_2 \cdot [ES]\end{aligned}$$



# STEADY-STATE KINETICS



$$K_m = \frac{k_{-1}.(k_{-2}.(k_{-3} + k_4) + k_3.k_4) + k_2.k_3.k_4}{k_1.((k_2 + k_{-2}).(k_{-3} + k_4) + k_2.k_3 + k_3.k_4)}$$

$$k_{cat} = \frac{k_2.k_3.k_4}{(k_2 + k_{-2}).(k_{-3} + k_4) + k_2.k_3 + k_3.k_4}$$

## □ Michaelis-Menten constant, $K_m$ (mol.l<sup>-1</sup>)

- apparent equilibrium constant
- determined by true binding constant and rates of catalytic steps

## □ Turnover number, $k_{cat}$ (s<sup>-1</sup>)

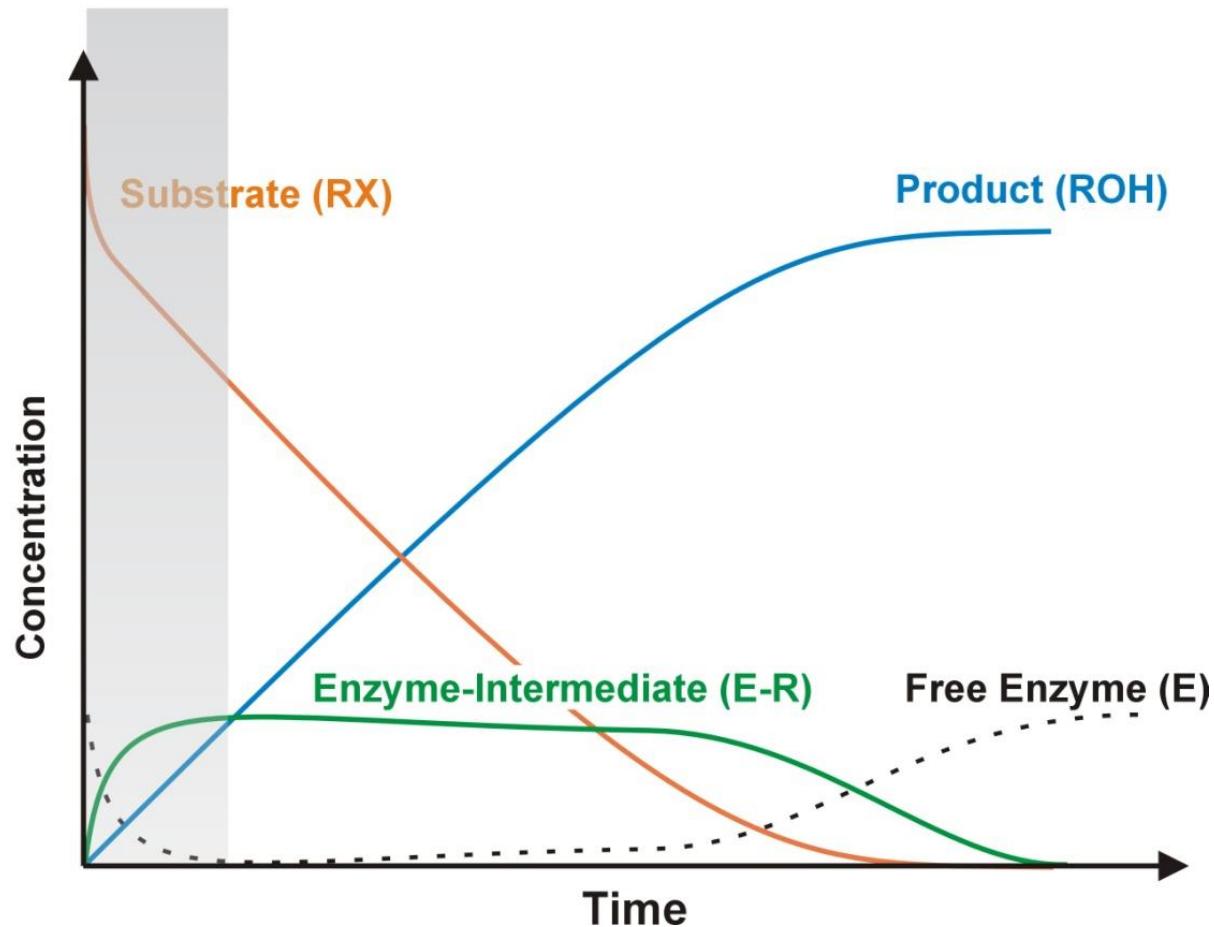
- number of molecules converted per second by one enzyme molecule under saturation
- influenced only by rates of catalytic steps (limiting step)

## □ Specificity constant, $k_{cat}/K_m$ (mol.l<sup>-1</sup>.s<sup>-1</sup>)

- apparent second order rate constant

# TRANSIENT KINETICS

## TRANSITION STATE



# RAPID MIXING TECHNIQUES



**STOPED-FLOW**

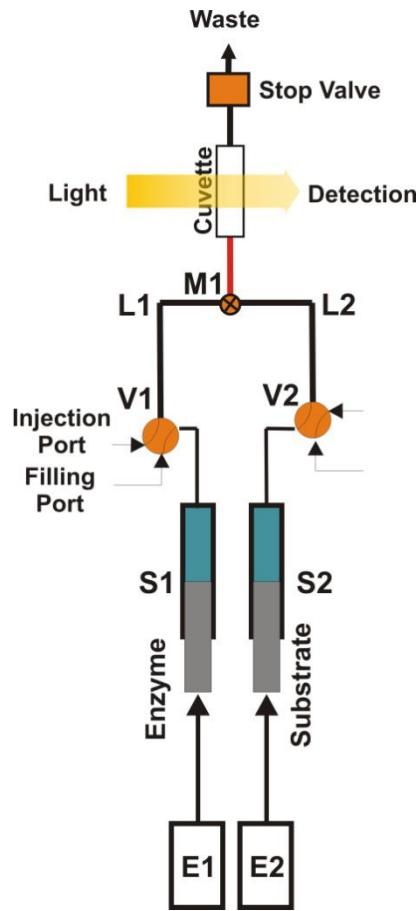


**RAPID QUENCH-FLOW**

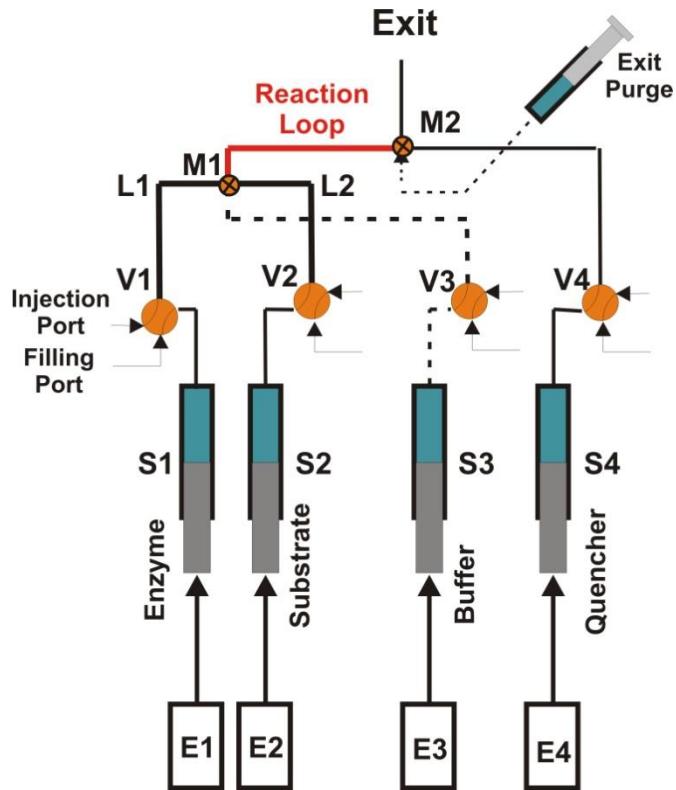


# RAPID MIXING TECHNIQUES

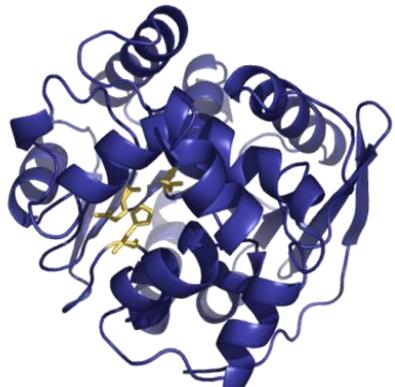
## STOPPED-FLOW



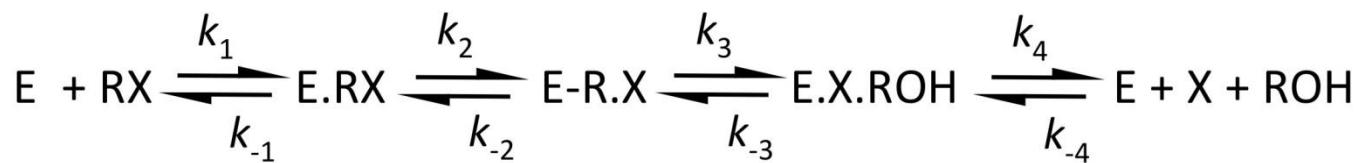
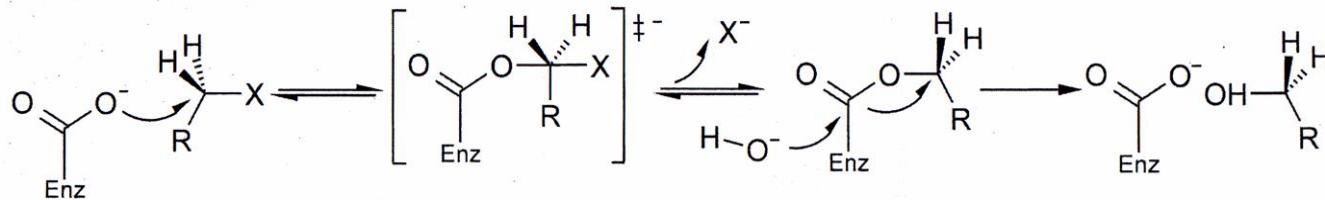
## RAPID QUENCH-FLOW



# KINETIC MECHANISMS

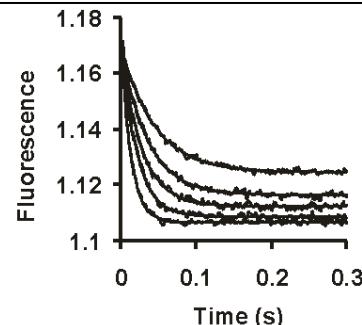


- **dehalogenase (EC 3.8.1.5)**
- **globular proteins**
- **monomeric/oligomeric**
- **no cofactor requirement**
- **cleavage carbon-halogen bond**

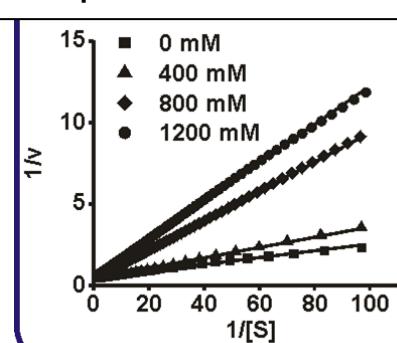
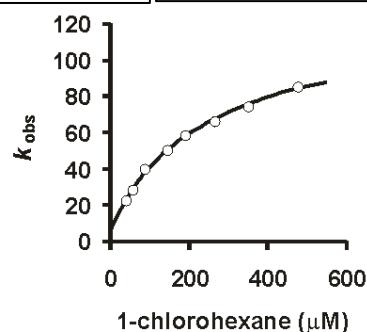


# KINETIC MECHANISMS

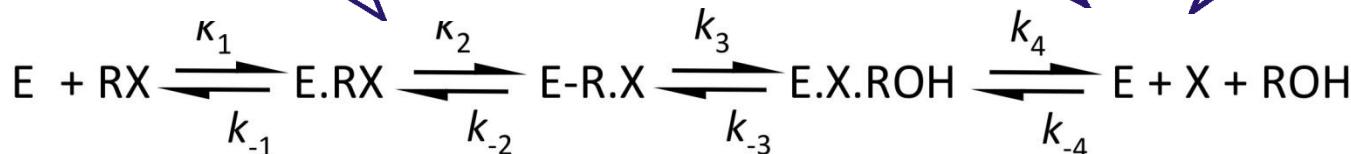
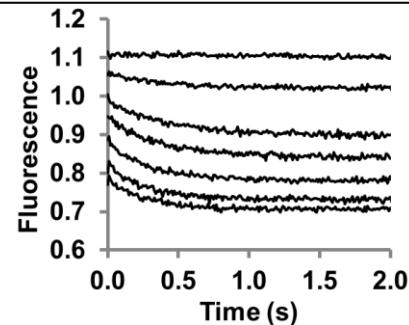
$$k_{\text{obs}} = \frac{k_2 \cdot [S]}{[S] + K_s} + k_2 + k_3$$



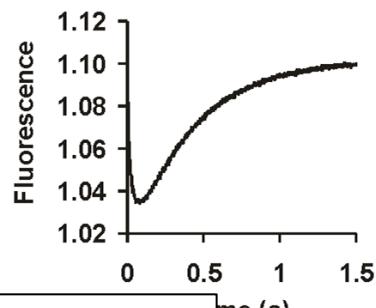
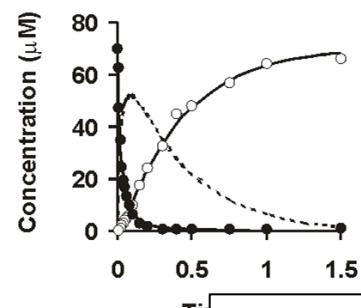
$$v = \frac{[S] \cdot k_{\text{cat}}}{K_m \cdot (1 + [P]/K_{p1}) + [S] \cdot (1 + [P]/K_{p2})}$$



$$k_{\text{obs}} = \frac{[P] \cdot k_{4b}}{K_{4a} + [P]} + k_{-4b}$$

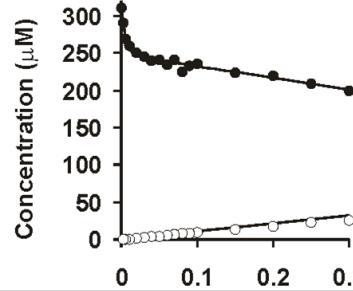


## SINGLE TURNOVER KINETICS



$$A = A_1 \cdot e^{-k_1 \cdot t} + A_2 \cdot e^{-k_2 \cdot t}$$

## REACTION BURST



$$A = A_0 \cdot e^{-k \cdot t} + k_2 \cdot t$$

# KINETIC MECHANISMS

	Substrat	$K_s$ ( $\mu\text{M}$ )	$k_2$ ( $\text{s}^{-1}$ )	$k_{-2}$ ( $\text{s}^{-1}$ )	$k_3$ ( $\text{s}^{-1}$ )	$k_4$ ( $\text{s}^{-1}$ )	$K_m$ ( $\mu\text{M}$ )	$k_{\text{cat}}$ ( $\text{s}^{-1}$ )
LinB	1-chlorohexane	240	117	0.4	3.2	-	16	2.6
	bromocyclohexane	> 450	> 200	1.1	2.5	-	23	1.8
	chlorocyclohexane	> 500	> 40	12.5	0.075	-	221	0.1
DhIA	1,2-dibromoethane <sup>1</sup>	> 27	> 130	-	10	4	10	3
	1,2-dichloroethane <sup>1</sup>	2 200	50	-	14	8	530	3.3
DhaA	1,3-dibromopropane <sup>2</sup>	60 - 300	300	-	14.8	3.9	5	2.7

distinct rate-limiting steps  
for relative enzymes

# PROTEIN ENGINEERING

## RATIONAL DESIGN

### 1. Computer aided design



### 2. Site-directed mutagenesis



Individual mutated gene

### 3. Transformation

### 4. Protein expression

### 5. Protein purification

### 6. *not applied*



Constructed mutant enzyme

## DIRECTED EVOLUTION

### 1. *not applied*

### 2. Random mutagenesis



Library of mutated genes  
(>10,000 clones)

### 3. Transformation

### 4. Protein expression

### 5. *not applied*

### 6. Screening and selection

- stability
- selectivity
- affinity
- activity



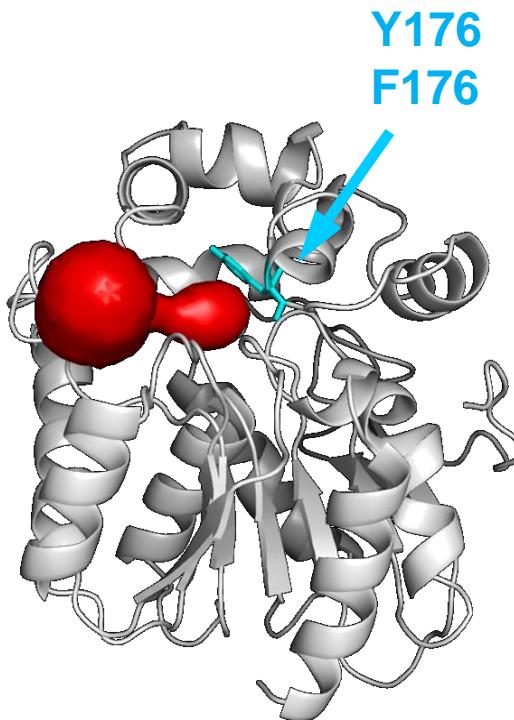
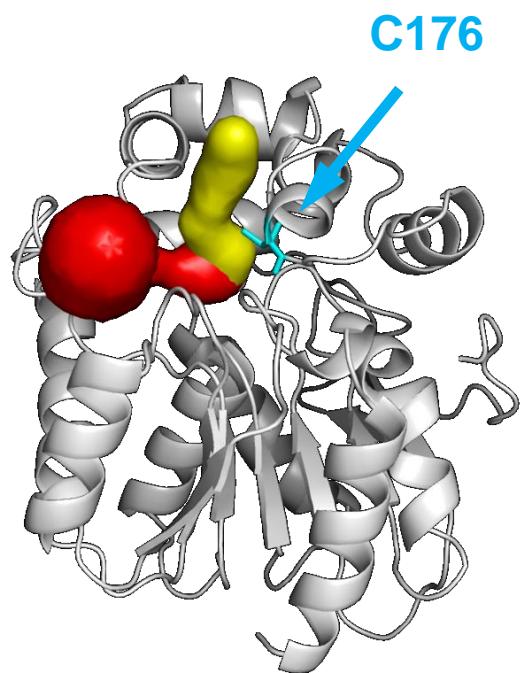
Selected mutant enzymes

IMPROVED  
ENZYME

### 7. Biochemical testing

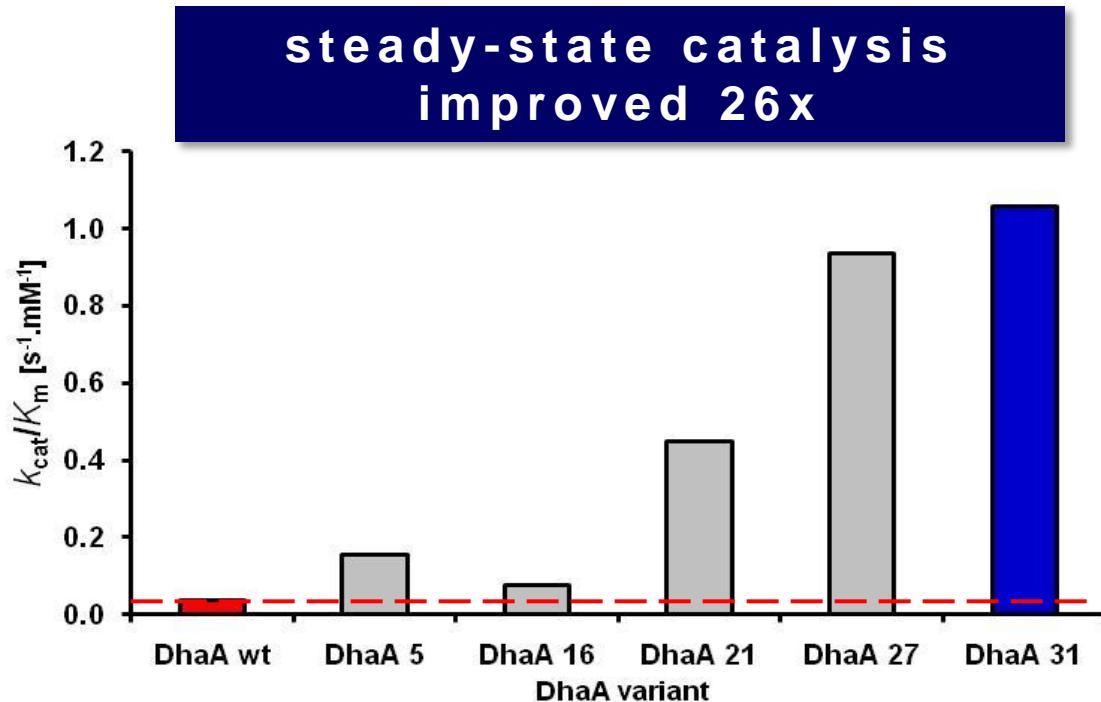
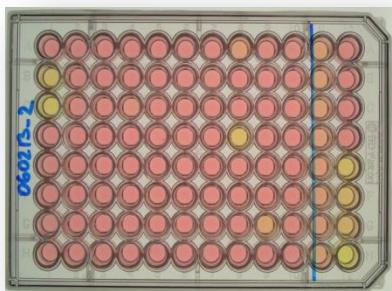
# PROTEIN ENGINEERING

- conversion of 1,2,3-trichloropropane
  - by dehalogenase from *Rhodococcus* sp.
- importance of access pathways



# PROTEIN ENGINEERING

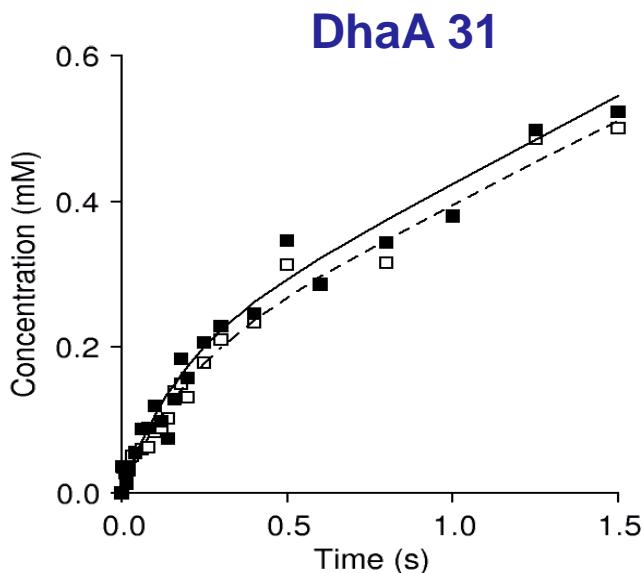
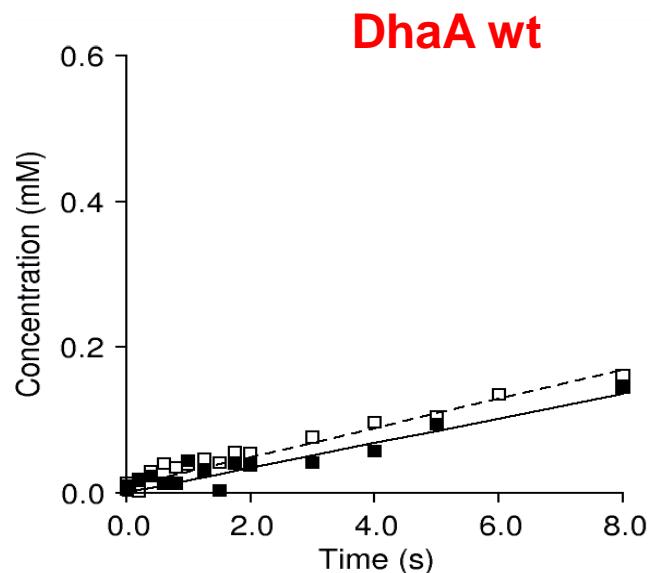
- library of 5,300 clones
- steady-state kinetics



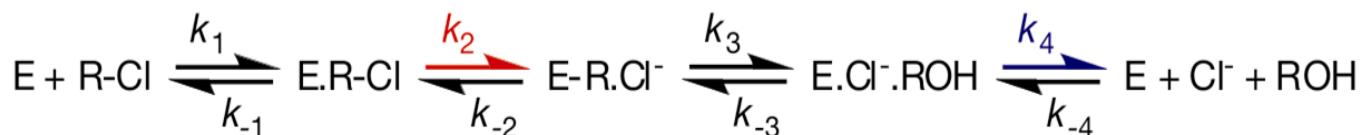
	$K_m$ (mM)	$k_{\text{cat}}$ ( $\text{s}^{-1}$ )	$k_{\text{cat}}/K_m$
DhaA wt	$0.98 \pm 0.17$	$0.035 \pm 0.002$	0.04
DhaA 31	$1.19 \pm 0.15$	$1.26 \pm 0.05$	1.06

# PROTEIN ENGINEERING

## □ transient kinetics



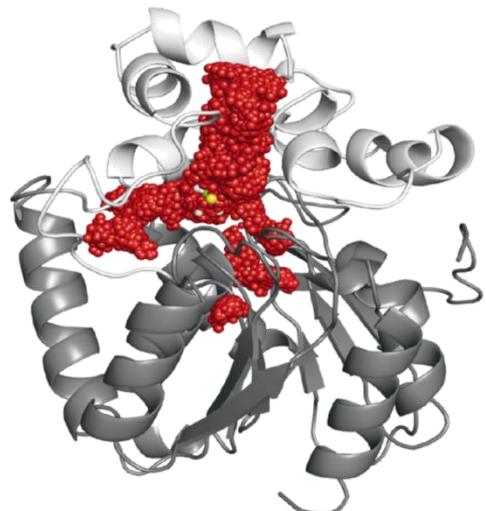
### Chemical reaction



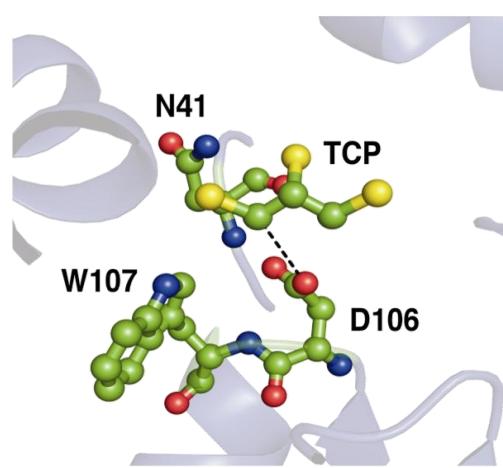
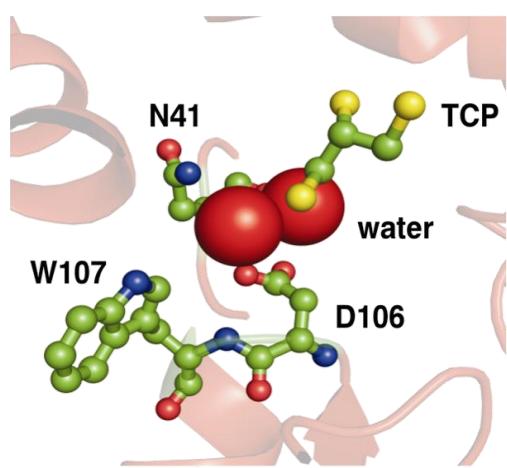
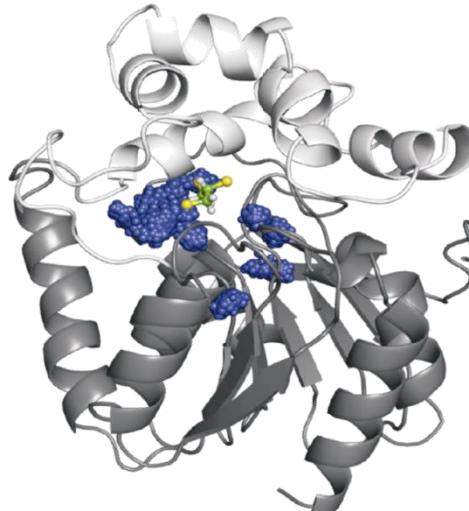
### Product release

# PROTEIN ENGINEERING

DhaA wt

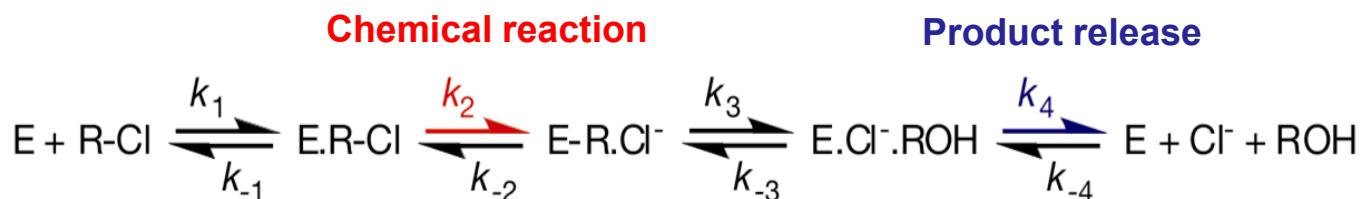
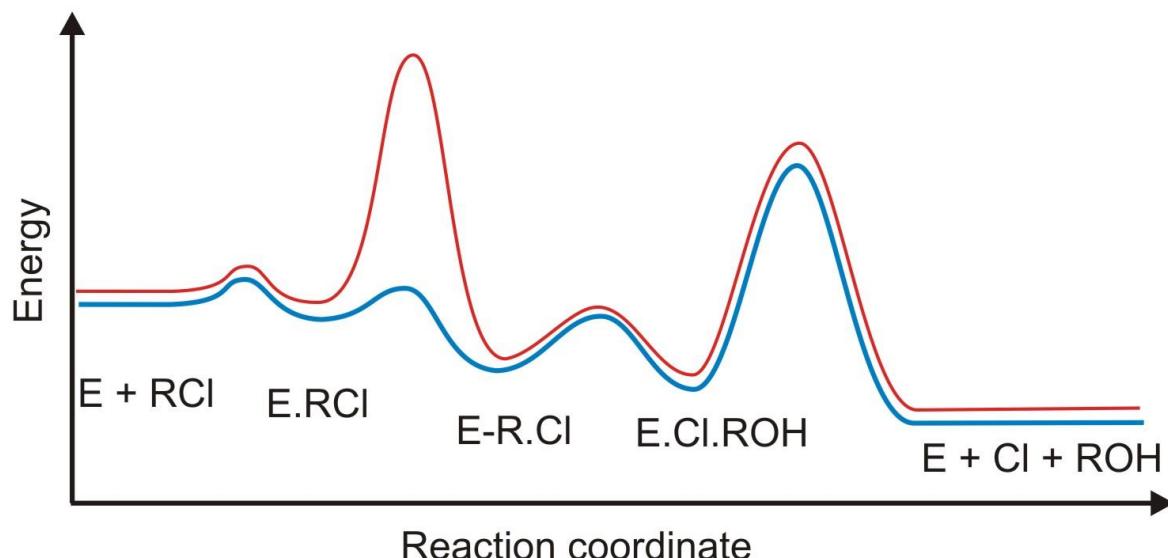


DhaA 31



# PROTEIN ENGINEERING

## ❑ transient kinetics



chemical step improved 450x