Precursor Methods

Goals :
- **decrease diffusion paths**
- **shorten reaction times**
- **decrease reaction temperatures**

Intimate mixing of components in solution, precipitation, filtration, washing, drying, calcination

💣✳ **High degree of homogenization**
💣✳ **Large contact area**
💣✳ **Reduction of diffusion distances**
💣✳ **Faster reaction rates**
💣✳ **Lower reaction temperatures**
💣✳ **Metastable phases, smaller grain size, larger surface area**
💣✳ **Shaping to fibers, films, nanoparticles**

Coprecipitation Method

Coprecipitation applicable to nitrates, acetates, oxalates, hydroxides, alkoxides, beta-diketonates

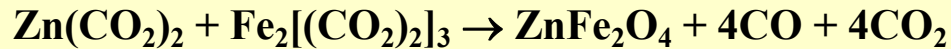|	
Requires:	**similar salt solubilities**
	similar precipitation rates
	no supersaturation
Washing:	**water, organic solvents**
Drying:	**evaporation**
	azeotropic distillation
	freeze-drying

Disadvantage: difficult to prepare high purity, accurate stoichiometric phases if solubilities do not match
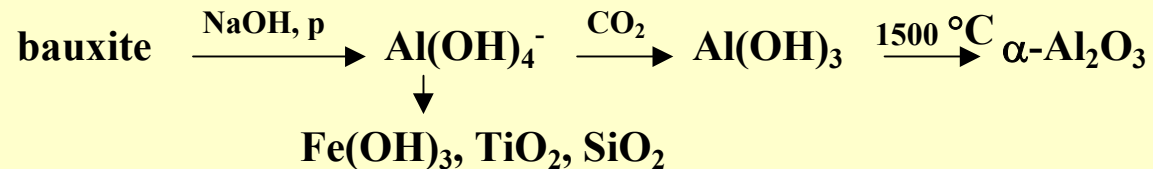
Coprecipitation Method

Spinels

oxalates: $Zn(CO_2)_2/Fe_2[(CO_2)_2]_3/H_2O$ **1 : 1 mixing, H_2O evaporation, salts coprecipitation**
Solid-solution mixing on atomic scale, filter, calcine in air

$$Zn(CO_2)_2 + Fe_2[(CO_2)_2]_3 \rightarrow ZnFe_2O_4 + 4CO + 4CO_2$$

Al_2O_3 Bayer Process

$$\text{bauxite} \xrightarrow{\text{NaOH, p}} Al(OH)_4^- \xrightarrow{CO_2} Al(OH)_3 \xrightarrow{1500\ °C} \alpha\text{-}Al_2O_3$$

$$\downarrow$$

$$Fe(OH)_3, TiO_2, SiO_2$$

$BaTiO_3$
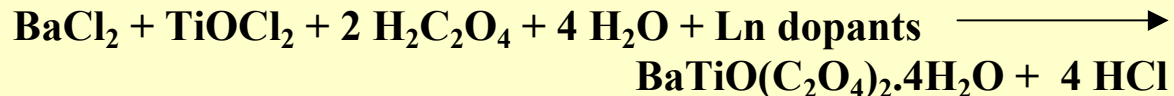
$BaCl_2 + TiOCl_2 + 2\ H_2C_2O_4 + 4\ H_2O + Ln$ dopants $\longrightarrow$
$BaTiO(C_2O_4)_2.4H_2O +\ 4\ HCl$
filtration, washing, drying, calcination @ 730 °C

Coprecipitation Method

Spinel

$Al(NO_3)_3 + Mg(NO_3)_2 + H_2O$ **freeze-drying gives amorphous mixture, calcination @ 800 °C !!! low T**

$$Mg(NO_3)_2 + 2\ Al(NO_3)_3 \longrightarrow MgAl_2O_4 + 6\ NO_x + (10\text{-}3x)O_2$$
$$\text{random}$$

Ruby
Ion exchange

$$Al(NO_3)_3 + Cr(NO_3)_3 \longrightarrow Al(OH)_3 + Cr(OH)_3\ \text{sol}$$
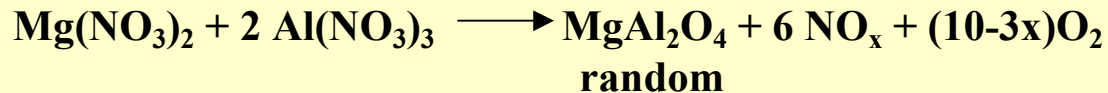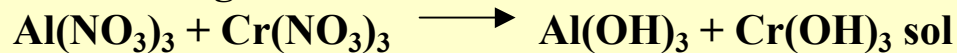
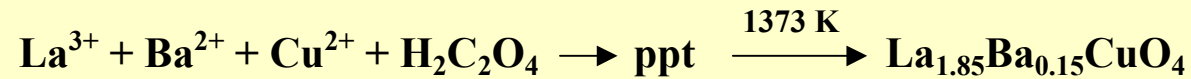**freeze drying gives solid $(Al/Cr)(OH)_3$ @ LN_2 temperature, 5 Pa anealing @ 950 °C for 2.5 h gives solid solution $Al_{2\text{-}x}Cr_xO_3$**

Zirconia

$$ZrSiO_4(zircon) + NaOH \longrightarrow Na_2ZrO_3 + Na_2SiO_3 \xrightarrow{\ HCl\ }$$

$$ZrOCl_2 \xrightarrow{OH^-,\ YCl_3} Zr(OH)_4\ /\ Y(OH)_3 \xrightarrow[\text{calcination}]{\text{azeot. dist.}} \text{nano-}Y/ZrO_2$$
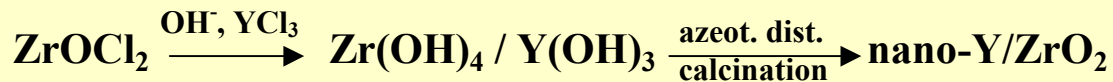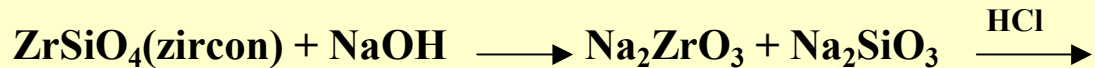
Coprecipitation Method

High-T_c Superconductors

$$La^{3+} + Ba^{2+} + Cu^{2+} + H_2C_2O_4 \longrightarrow ppt \xrightarrow{1373 \text{ K}} La_{1.85}Ba_{0.15}CuO_4$$

Magnetic garnets, tunable magnetic materials

$$Y(NO_3)_3 + Gd(NO_3)_3 + FeCl_3 + NaOH \rightarrow Y_xGd_{3-x}Fe_5O_{12}$$
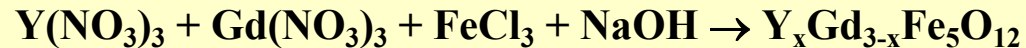
Firing @ 900 ^{o}C, 18-24 hrs, pellets, regrinding, repelletizing,
repeated firings, removes $REFeO_3$ perovskite impurity
Isomorphous replacement of Y^{3+} for Gd^{3+} on dodecahedral sites,
solid solution, similar rare earth ionic radii
complete family accessible, $0 < x < 3$, $2Fe^{3+}$ O_h sites, $3Fe^{3+}$ T_d sites,
$3RE^{3+}$ dodecahedral sites

Oxalate Coprecipitation

$LiMPO_4$ (M = Mn, Fe, Co, or Ni)
- olivine structure
- new cathode materials for lithium rechargeable batteries
- multicomponent olivine cathode materials $LiMn_{1/3}Fe_{1/3}Co_{1/3}PO_4$

$Mn_{1/3}Fe_{1/3}Co_{1/3}(C_2O_4)_3 \, 2H_2O$
stoichiometric, homogeneously mixed transition metal oxalate precursor
the differences in chemical behavior of Fe, Co, and Mn ions
- control of pH - different solubilities of $MC_2O_4 \, 2H_2O$
- control of atmosphere - Fe^{2+} get easily oxidized to Fe^{3+}
- control of temperature and aging time - $FeC_2O_4·2H_2O$ and $CoC_2O_4·2H_2O$ have temperature-dependent polymorphisms: monoclinic α (90 °C) and orthorhombic β (25 °C), $MnC_2O_4·2H_2O$ forms only monoclinic

Solid state reaction of $Mn_{1/3}Fe_{1/3}Co_{1/3}(C_2O_4)_3 \, 2H_2O$ and LiH_2PO_4

Pechini and Citrate Gel Method

Aqueous solution of metal ions

$$
HO-\begin{array}{l} -COOH \\ -COOH \\ -COOH \end{array}
$$

Chelate formation with citric acid
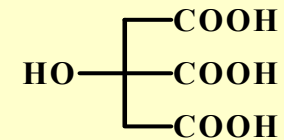
Polyesterification with polyfunctional alcohol on heating

Further heating leads to resin, transparent glassy gel
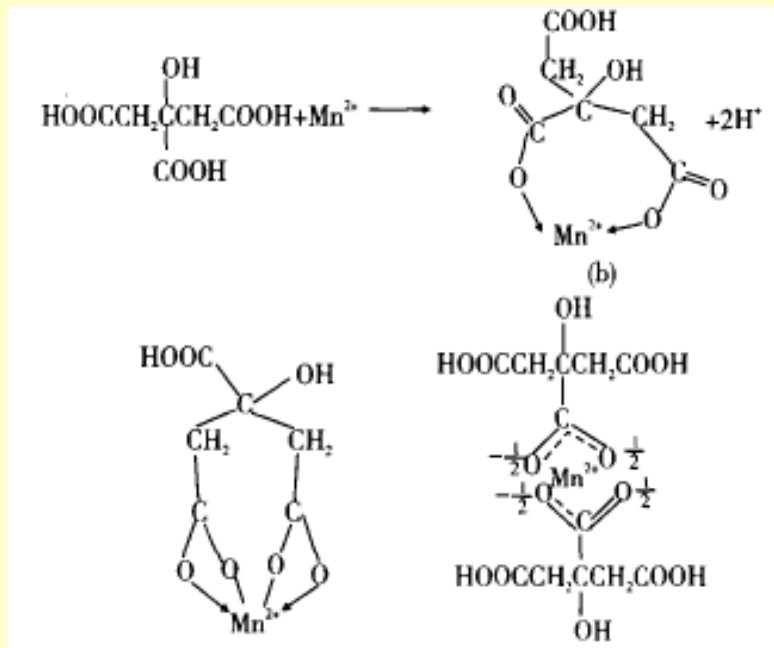calcination provides oxide powder

Control of stoichiometry by initial reagent ratio

Complex compositions, mixture of metal ions
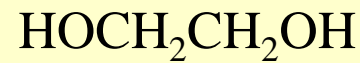
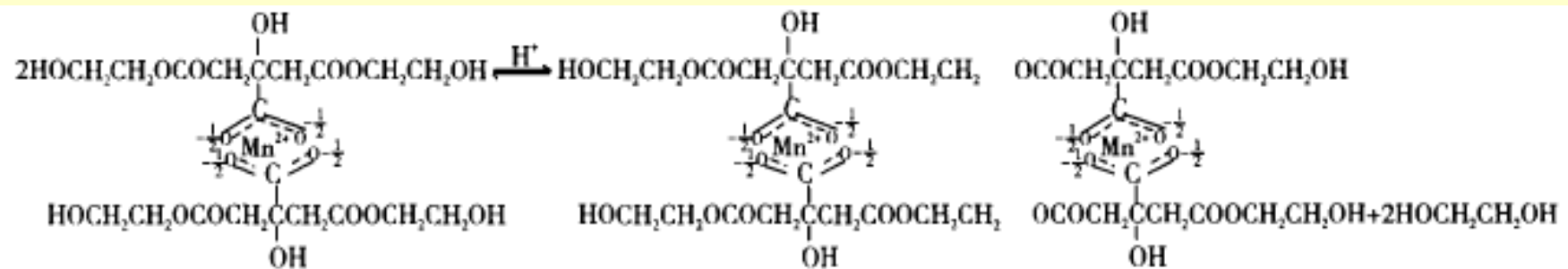Good homogeneity, mixing at the molecular level

Low firing temperatures

Pechini and Citrate Gel Method

Chelation

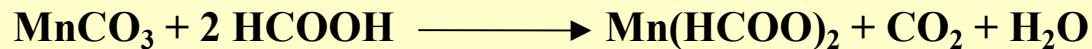Complexation-coordination polymers

$HOCH_2CH_2OH$

Polyesterification

polycondensation

Pechini and Citrate Gel Method

$BaTiO_3$
by conventional powder method at 1200 °C
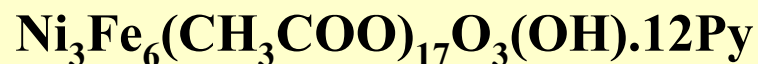
Ba^{2+} + $Ti(O^iPr)_4$ + citric acid at 650 °C

Sc_2O_3 + 6 HCOOH $\longrightarrow$ $2Sc(HCOO)_3$ + 3 H_2O
$MnCO_3$ + 2 HCOOH $\longrightarrow$ $Mn(HCOO)_2$ + CO_2 + H_2O
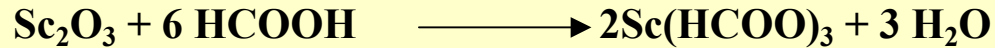
added to citric acid, water removal, calcination @ 690 °C gives
$ScMnO_3$
without citric acid only mixture of Sc_2O_3 and Mn_2O_3 is formed

Double Salt Precursors

Double salts of known and controlled stoichiometry such as:
$Ni_3Fe_6(CH_3COO)_{17}O_3(OH).12Py$

**Burn off organics 200-300 °C, then 1000 °C in air for 2-3 days**
Product highly crystalline phase pure $NiFe_2O_4$ spinel
Good way to make chromite spinels, important tunable magnetic materials
Juggling the electronic-magnetic properties of the O_h and T_d ions in the spinel lattice

| Chromite spinel	Precursor	Ignition T, °C
$MgCr_2O_4$	$(NH_4)_2Mg(CrO_4)_2.6H_2O$	1100-1200
$NiCr_2O_4$	$(NH_4)_2Ni(CrO_4)_2.6H_2O$	1100
$MnCr_2O_4$	$MnCr_2O_7.4C_5H_5N$	1100
$CoCr_2O_4$	$CoCr_2O_7.4C_5H_5N$	1200
$CuCr_2O_4$	$(NH_4)_2Cu(CrO_4)_2.2NH_3$	700-800
$ZnCr_2O_4$	$(NH_4)_2Zn(CrO_4)_2. 2NH_3$	1400
$FeCr_2O_4$	$(NH_4)_2Fe(CrO_4)_2$	1150

Double Salt Precursors
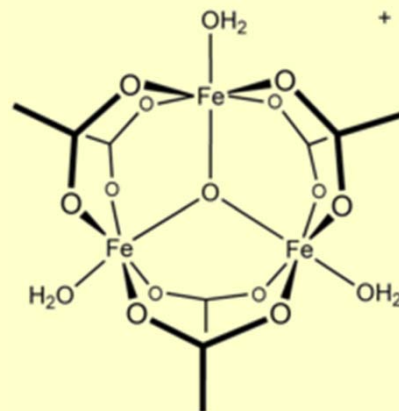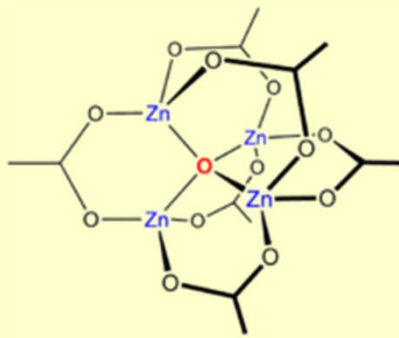
Single Source Precursors

- **Compounds containing desired elements in a proper stoichiometric ratio**
- **Easy chemical pathway for ligand removal**

$$H_2O \quad + \quad (M\text{-}O\text{-}SiO_3)_x$$
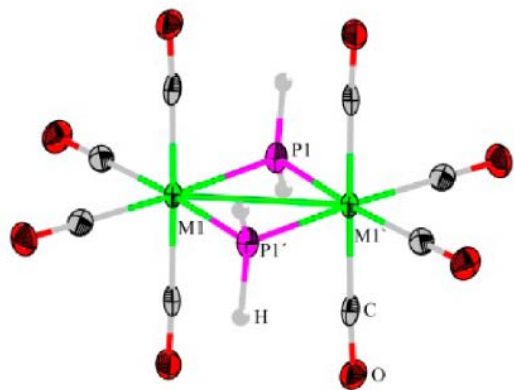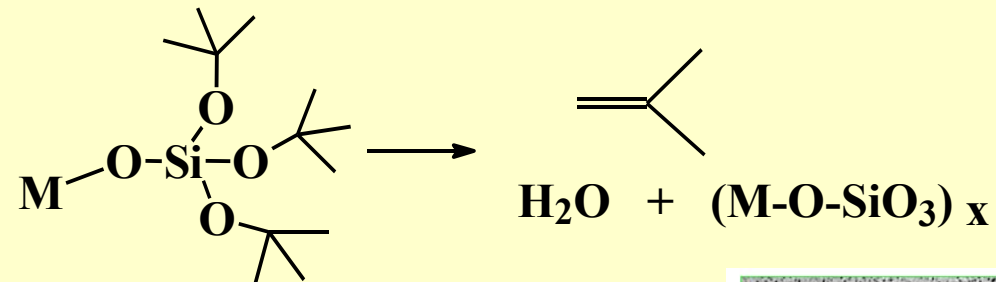
Thermolysis
180 °C for 1 h

Hexadecylamine (HDA)
Oleic acid (OlA)
Mesitylene

CrP
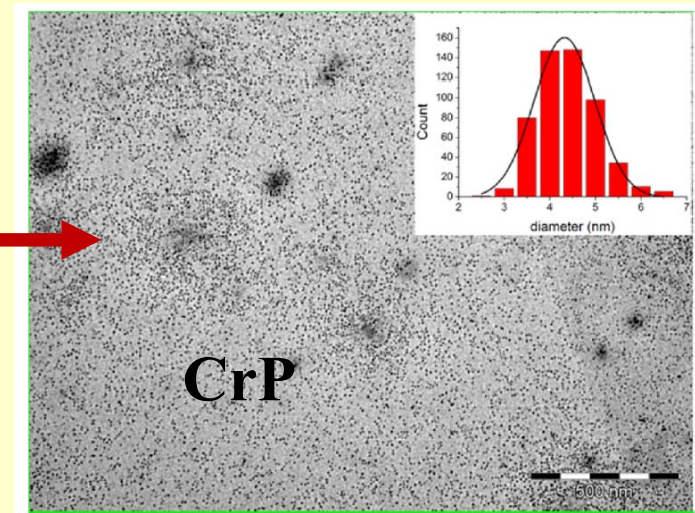
Known phases in Cr-P system: Cr_3P, Cr_2P, Cr_2P_7, CrP, CrP_2, CrP_4

12

Vegard's Law

Vegard law behavior:

A linear relationship exists between the concentration of the substitute element and a property of a solid-solution, e.g. the size of the lattice parameters.

Any property P of a solid-solution member is the atom fraction weighted average of the end-members
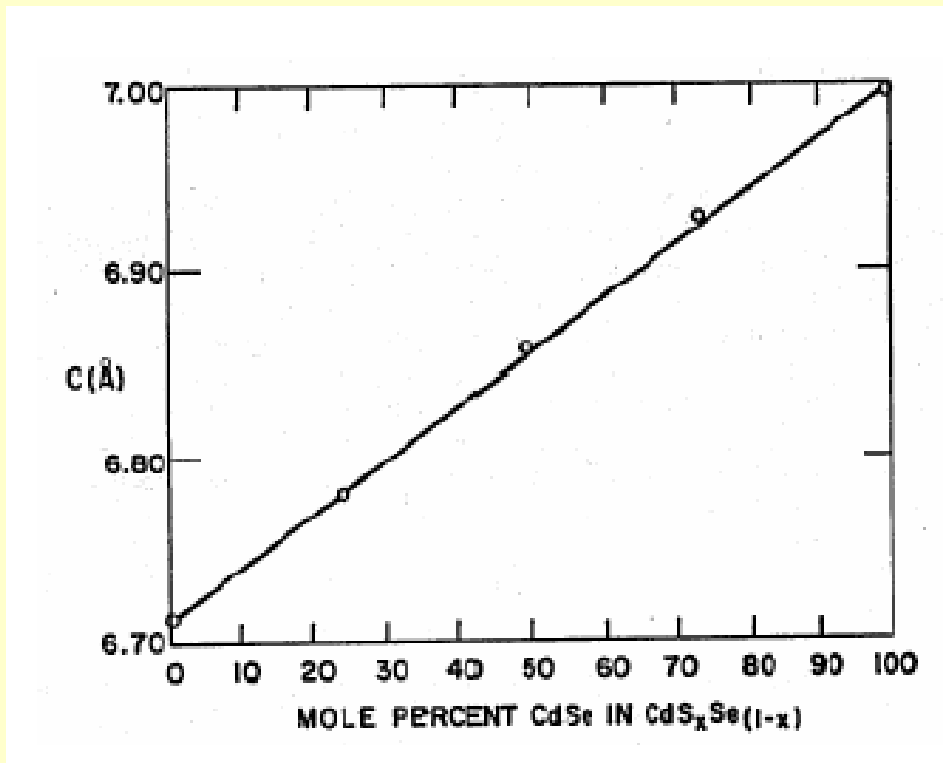
The composition of the $A_{1-x}B_x$ alloy can be calculated from Vegard's law

The lattice parameter of a solid solution alloy *a* will be given by a linear dependence of lattice parameter on composition:

$a(A_{1-x}B_x) = x\,a(B) + (1-x)\,a(A)$

Vegard's Law

$$c(CdSe_{1-x}S_x) = x\ c(CdS) + (1-x)\ c(CdSe)$$

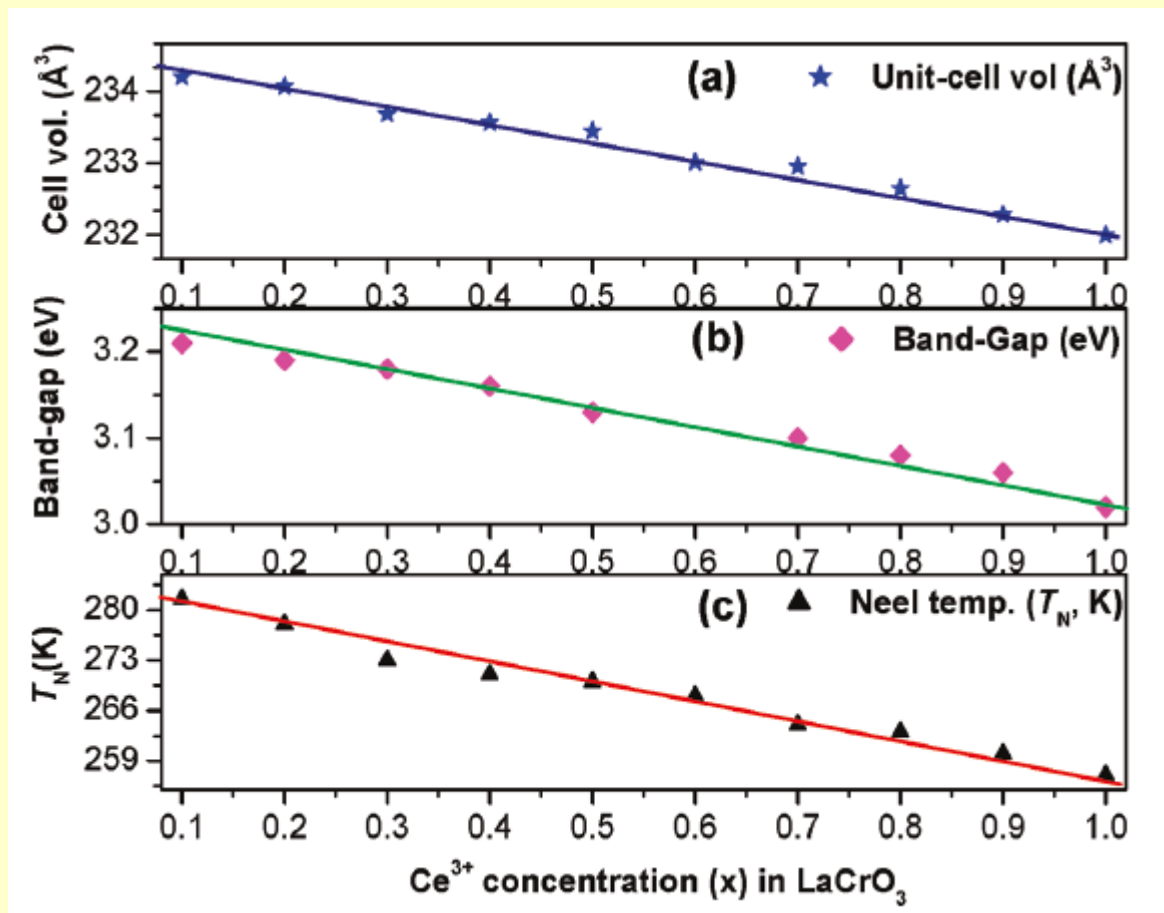MOLE PERCENT CdSe IN CdS$_x$Se$_{(1-x)}$

Anion radius

S^{2-} 1.84 Å

Se^{2-} 1.98 Å

a hexagonal wurzite structure
a cubic zinc blende
a high pressure form with the NaCl structure

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La$_{1-x}$Ce$_x$CrO$_3$

Flux Method

Molten salts (inert or reactive), oxides, metals

MNO_3, MOH, (M = alkali metal)

FLINAK: LiF-NaF-KF

M_2Q_x (M = alkali metal, Q = S, Se, Te)

molten salts ionic, low mp, eutectics, completely ionized
act as solvents or reactants, T = 250-550 °C
enhanced diffusion, reduced reaction temperatures in comparison with
powder method
products finely divided solids, high surface area (SA)
slow cooling to grow crystals
separation of water insoluble product from a water soluble flux
incorporation of the molten salt ions in product prevented by using salts
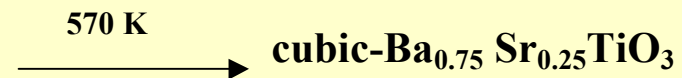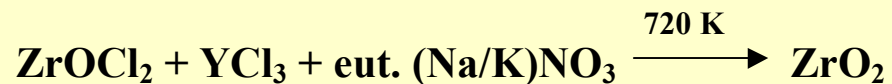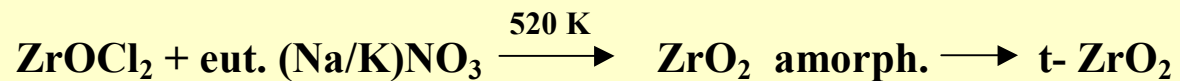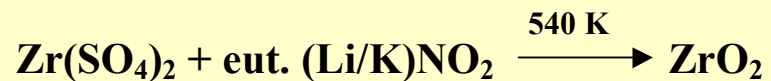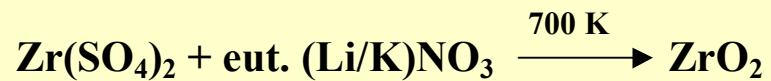**with ions of much different sizes than the ones in the product**
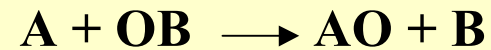**($PbZrO_3$ in a B_2O_3 flux)**

Flux Method

Lux-Flood formalism
oxide = strong base
acid = oxide acceptor $\qquad$ $A + OB \longrightarrow AO + B$
base = oxide donor

$$Zr(SO_4)_2 + \text{eut. } (Li/K)NO_3 \xrightarrow{700 \text{ K}} ZrO_2$$

$$Zr(SO_4)_2 + \text{eut. } (Li/K)NO_2 \xrightarrow{540 \text{ K}} ZrO_2$$

$$ZrOCl_2 + \text{eut. } (Na/K)NO_3 \xrightarrow{520 \text{ K}} ZrO_2 \text{ amorph.} \longrightarrow t\text{-} ZrO_2$$

$$ZrOCl_2 + YCl_3 + \text{eut. } (Na/K)NO_3 \xrightarrow{720 \text{ K}} ZrO_2$$

$$BaCO_3 + SrCO_3 + TiO_2 + \text{eut. } (Na/K)OH$$

$$\xrightarrow{570 \text{ K}} \text{cubic-}Ba_{0.75} Sr_{0.25} TiO_3$$

Flux Method

fly ash (aluminosilicates)

NaOH, NH$_4$F, NaNO$_3$ $\longrightarrow$ zeolites (sodalite, cancrinite)

NH$_4$H$_2$PO$_4$ + (Na/K)NO$_3$ + M(NO$_3$)$_2$ $\longrightarrow$ (Na/K)MPO$_4$

4 SrCO$_3$ + Al$_2$O$_3$ + Ta$_2$O$_5$ $\longrightarrow$ Sr$_2$AlTaO$_6$
900 °C in SrCl$_2$ flux
1400 °C required for a direct reaction

K$_2$Te$_x$ + Cu $\longrightarrow$ K$_2$Cu$_5$Te$_5$ K$_2$Te$_x$ reactive flux, 350 °C

Flux Method

Electrolysis in molten salts

Reduction of TiO_2 pellets to Ti sponge in a $CaCl_2$ melt at 950 °C

O^{2-} dissolves in $CaCl_2$, diffuses to the graphite anode

insulating TiO_2 $\rightarrow$ TiO_{2-x} conductive

graphite anode
anodic oxidation   **$2\ O^{2-} \rightarrow O_2 + 4\ e^-$**
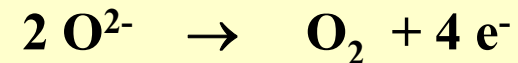
cathode TiO_2 pellet
cathodic reduction   **$Ti^{4+} + 4\ e^- \rightarrow Ti$**
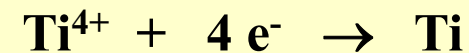
Ionic Liquids

Organic cations (containing N, P)

Inorganic anions: Cl^-, $AlCl_4^-$, $Al_2Cl_7^-$, $Al_3Cl_{10}^-$, PF_6^-, $SnCl_3^-$, BCl_3^-, BF_4^-, NO_3^-, $OSO_2CF_3^-$ (triflate), $CH_3C_6H_4SO_3^-$, $N(SO_2CF_3)_2^-$, PO_4^{3-}
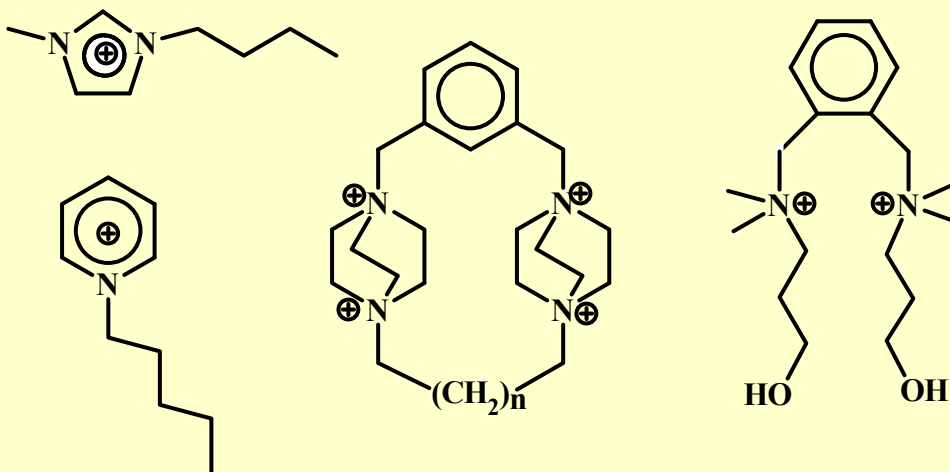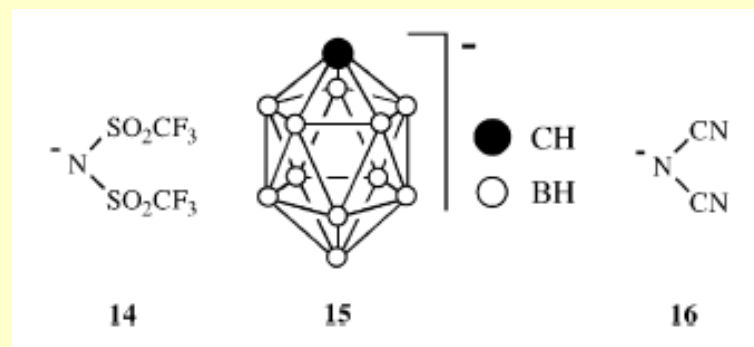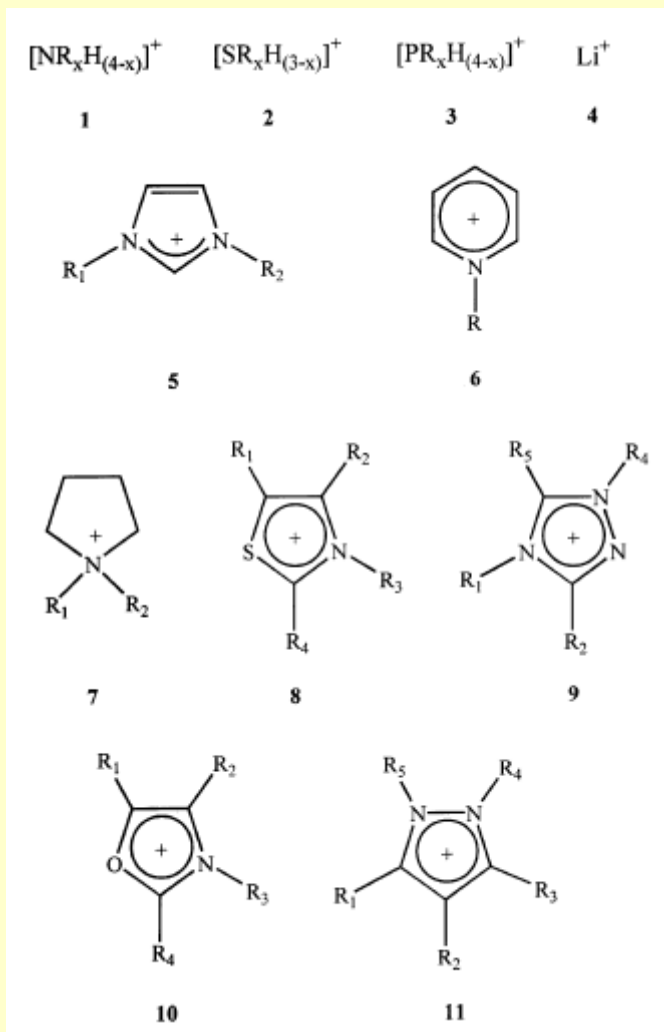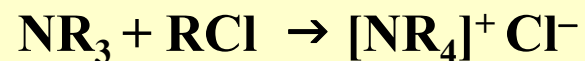
Ionic Liquids

Oldest known (1914) : $EtNH_3^+NO_3^-$ mp 12 °C

➔Liquids at room temperature or low mp

➔Thermal operating range from –40 °C to 400 °C

➔Higly polar, noncoordinating, completely ionized

➔Nonvolatile – no detectable vapor pressure

➔Nonflamable, nonexplosive, nonoxidizing, high thermal stability

➔Electrochemical window > 4V (not oxidized or reduced)

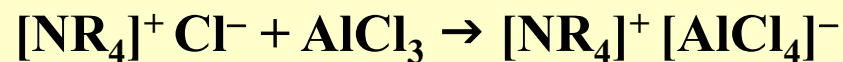➔Immiscible with organic solvents
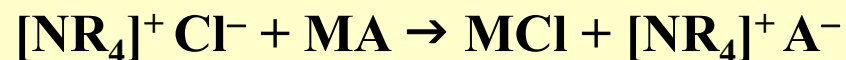
➔Hydrophobic IL immiscible with water
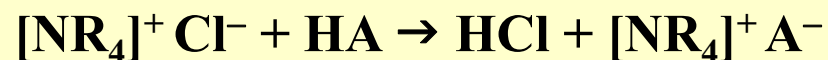
Ionic Liquids

Synthesis of Ionic Liquids

$NR_3 + RCl \rightarrow [NR_4]^+ Cl^-$

Aluminates
$[NR_4]^+ Cl^- + AlCl_3 \rightarrow [NR_4]^+ [AlCl_4]^-$

Metal halide elimination
$[NR_4]^+ Cl^- + MA \rightarrow MCl + [NR_4]^+ A^-$

Reaction with an acid
$[NR_4]^+ Cl^- + HA \rightarrow HCl + [NR_4]^+ A^-$

Ion exchange
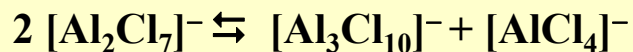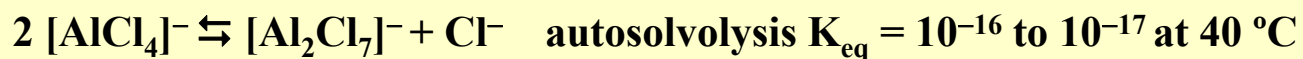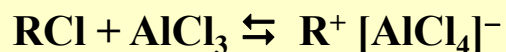$[NR_4]^+ Cl^- + \text{Ion exchanger A} \rightarrow [NR_4]^+ A^-$
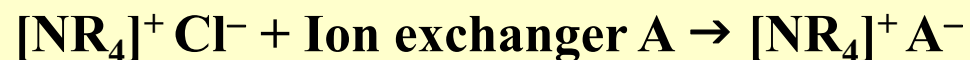
Halogenoaluminate(III) Ionic Liquids

The most widely studied class of IL

High sensitivity to moisture – handling under vacuum
or inert atmosphere in glass/teflon

$RCl + AlCl_3 \rightleftharpoons R^+ [AlCl_4]^-$

$2 [AlCl_4]^- \rightleftharpoons [Al_2Cl_7]^- + Cl^-$ autosolvolysis $K_{eq} = 10^{-16}$ to 10^{-17} at 40 ºC

$2 [Al_2Cl_7]^- \rightleftharpoons [Al_3Cl_{10}]^- + [AlCl_4]^-$
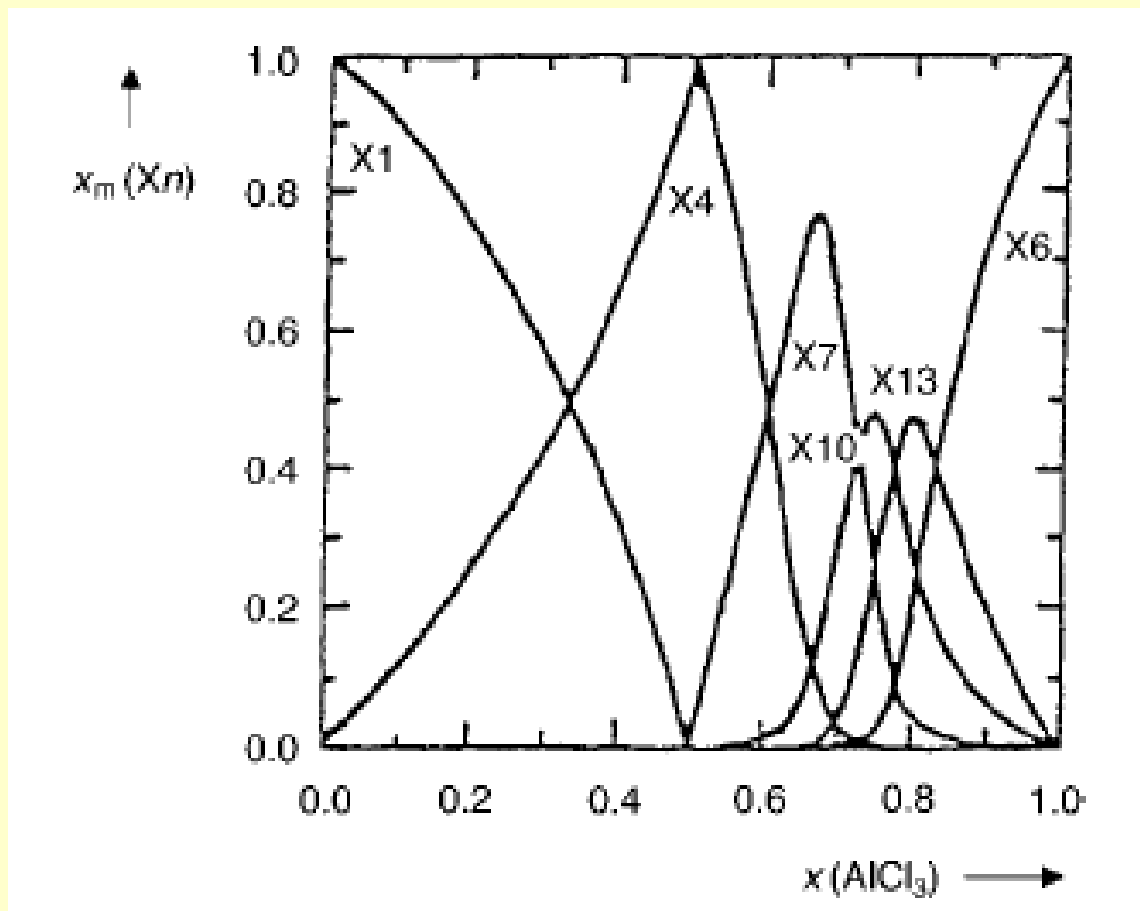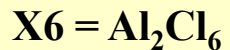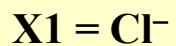
Acidic: excess of $AlCl_3$ as $[Al_2Cl_7]^-$ $x(AlCl_3) > 0.5$

Basic: excess of Cl^- $x(AlCl_3) < 0.5$

Neutral: $[AlCl_4]^-$ $x(AlCl_3) = 0.5$
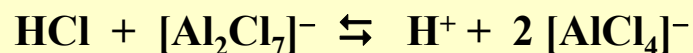
Equilibria in Halogenoaluminate(III) IL

Equilibria in IL

X1 = Cl^-

X4 = $[AlCl_4]^-$

X7 = $[Al_2Cl_7]^-$

X10 = $[Al_3Cl_{10}]^-$

X13 = $[Al_4Cl_{13}]^-$

X6 = Al_2Cl_6

Halogenoaluminate(III) Ionic Liquids

$2 \, [AlCl_4]^- \rightleftharpoons [Al_2Cl_7]^- + Cl^-$ autosolvolysis $K_{eq} = 10^{-16}$ to 10^{-17} at 40 ºC
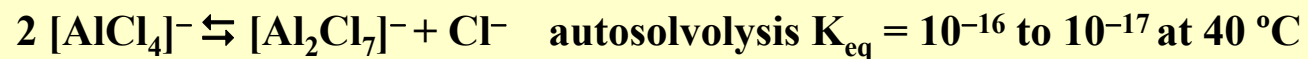
Acidic IL with an excess of $AlCl_3$

$HCl + [Al_2Cl_7]^- \rightleftharpoons H^+ + 2 \, [AlCl_4]^-$

Proton extremely poorly solvated = high reactivity

Superacid   [EMIM]Cl/$AlCl_3$/HCl H_0 = -19   **(HSO_3F: H_0 = -15)**

Latent acidity

$MCl + [Al_2Cl_7]^- \rightleftharpoons M^+ + 2 \, [AlCl_4]^-$ **buffered IL**

$B + M^+ + [AlCl_4]^- \rightleftharpoons MCl + B\text{-}AlCl_3$
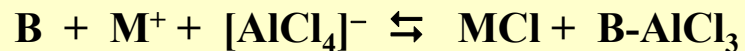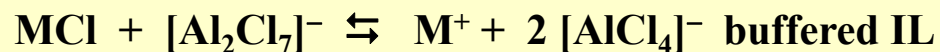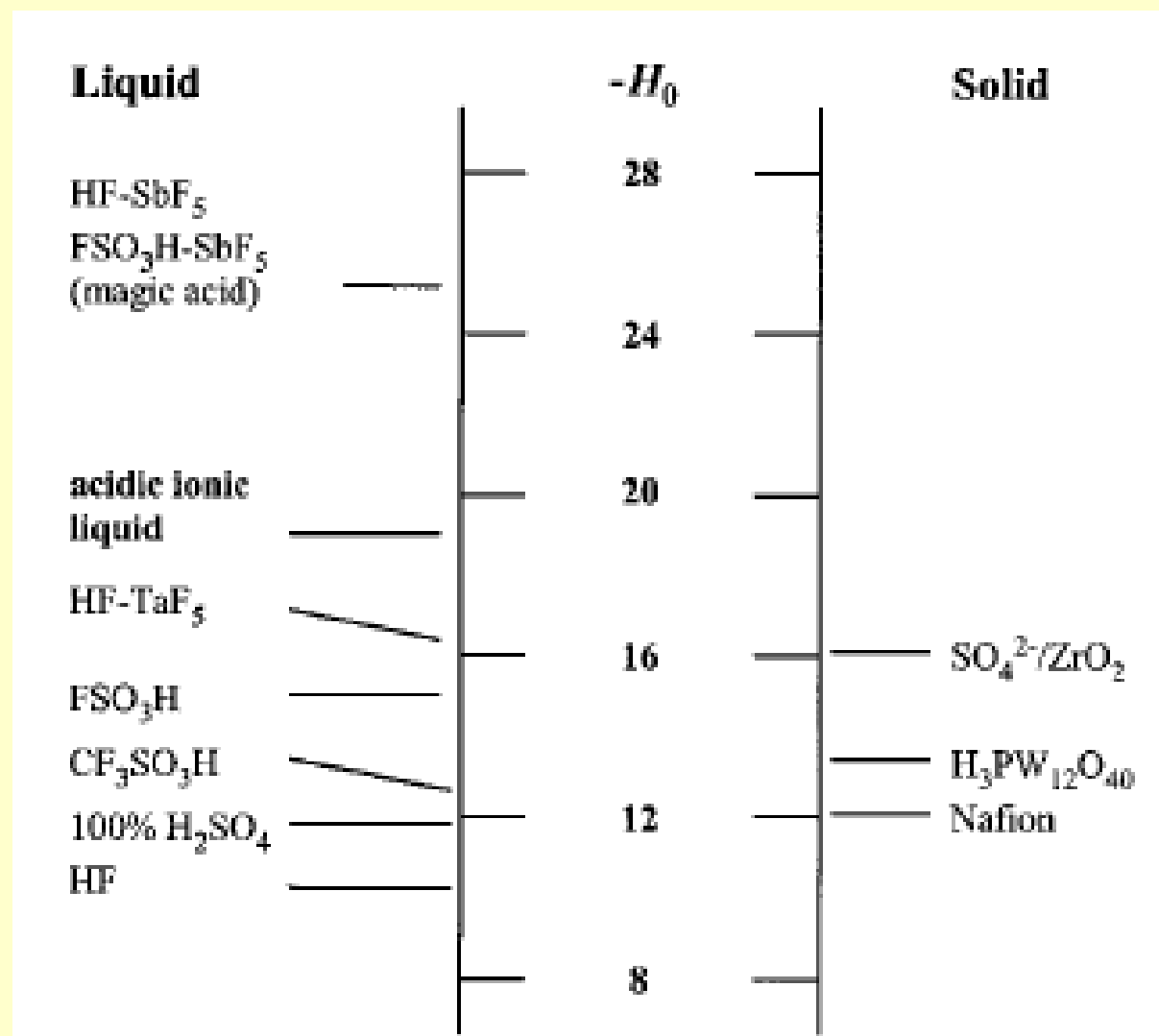
Superacidity

Superacidic [EMIM]Cl/AlCl$_3$/HCl

I = not protonated
II = slightly protonated
III and IV = 10-20 %
V = 75-90%
VI-VIII = nearly completely
IX and X = completely
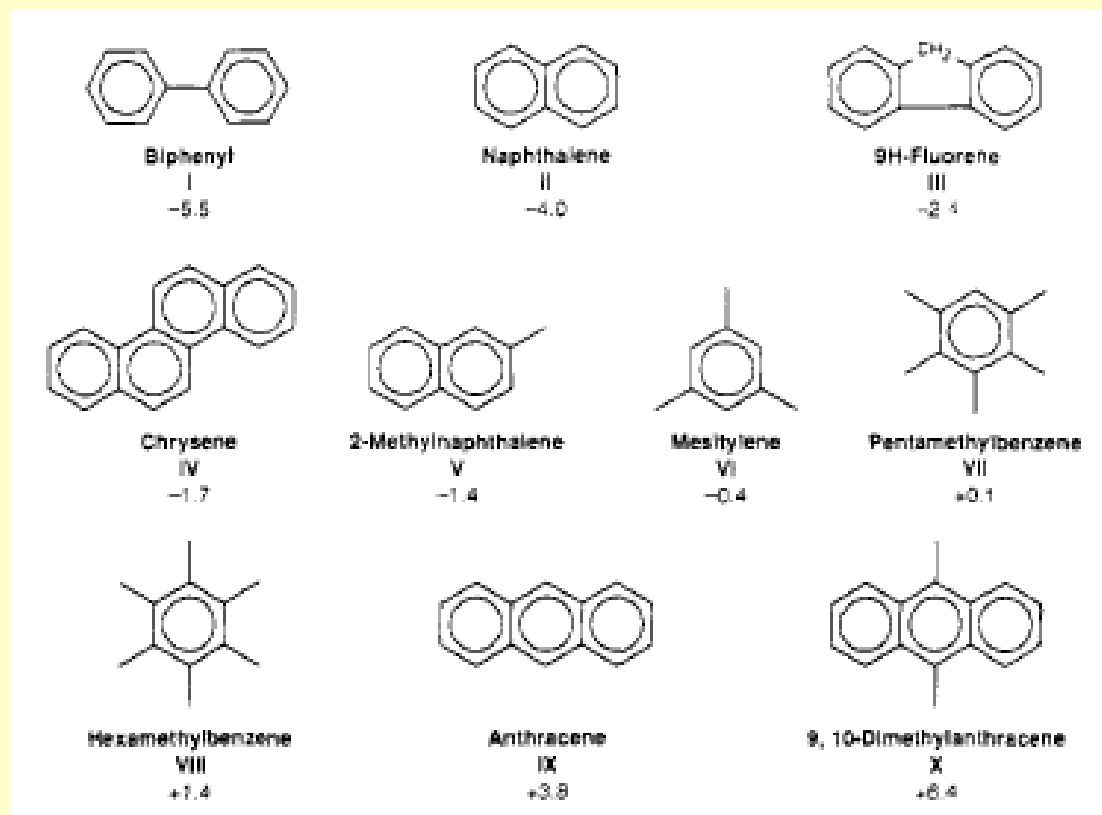
log K$_b$ in HF

Ionic Liquids

Completely inorganic ionic liquids

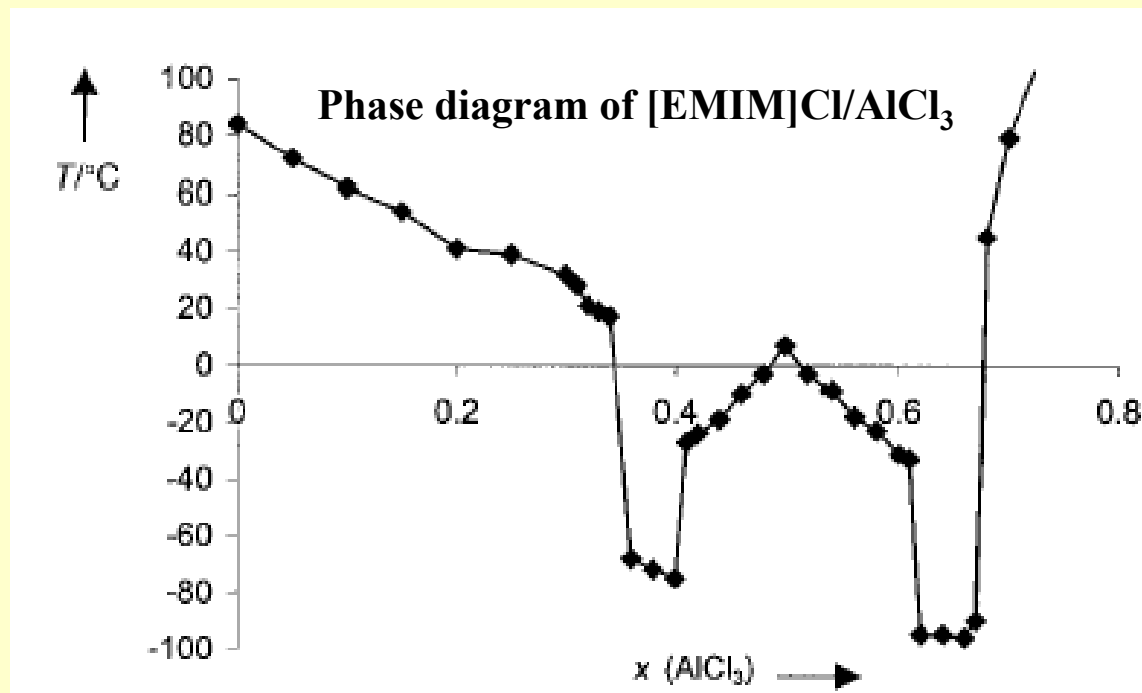| Compound	mp (K)	Compound	mp (K)
$Na_{13}[La(TiW_{11}O_{39})_2]$	253.0	$Na_{13}[Tm(TiW_{11}O_{39})_2]$	260.2
$Na_{13}[Ce(TiW_{11}O_{39})_2]$	263.0	$Na_{13}[Yb(TiW_{11}O_{39})_2]$	267.2
$Na_{13}[Pr(TiW_{11}O_{39})_2]$	253.0	$Na_5[CrTiW_{11}O_{39}]$	261.5
$Na_{13}[Sm(TiW_{11}O_{39})_2]$	256.0	$Na_5[MnTiW_{11}O_{39}]$	253.0
$Na_{13}[Gd(TiW_{11}O_{39})_2]$	265.1	$Na_5[FeTiW_{11}O_{39}]$	257.6
$Na_{13}[Dy(TiW_{11}O_{39})_2]$	265.2	$Na_6[ZnTiW_{11}O_{39}]$	257.4
$Na_{13}[Er(TiW_{11}O_{39})_2]$	261.0		

Melting Point of Ionic Liquids

Melting point is influenced by:

Cation – low symmetry, weak imtermolecular interactions, good distribution of charge
Anion – increasing size leads to lower mp
Composition – Phase diagram

Phase diagram of [EMIM]Cl/AlCl$_3$

Melting Point of Ionic Liquids

R	X	mp/°C
Me	Cl	125
Et	Cl	87
n-Bu	Cl	65
Et	NO_3	38
Et	$AlCl_4$	7
Et	BF_4	6
Et	CF_3SO_3	-9
Et	$(CF_3SO_3)_2N$	-3
Et	CF_3CO_2	-14
n-Bu	CF_3SO_3	16

Density of Ionic Liquids

The density of IL decreases as the bulkiness of the organic cation increases:
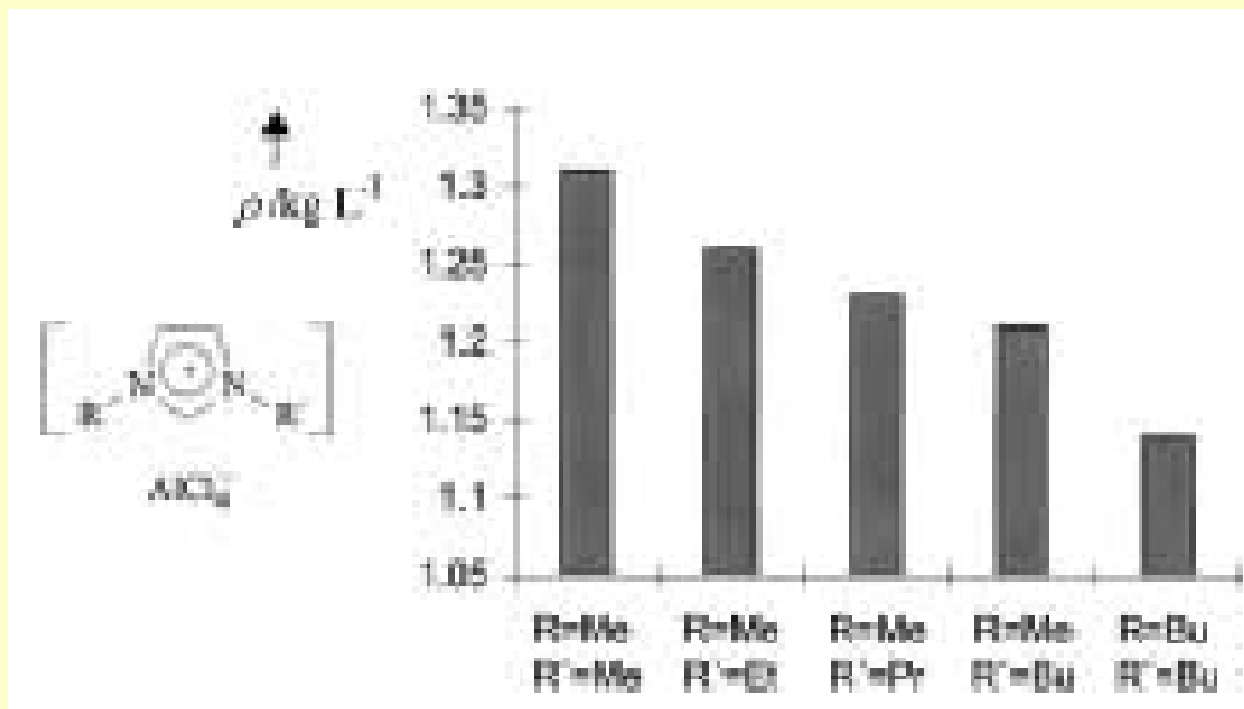
Viscosity of Ionic Liquids

The viscosity of IL depends on:

van der Waals interactions

H-bonding

Anion $[A]^-$	η [cP]
$CF_3SO_3^-$	90
n-$C_4F_9SO_3^-$	373
CF_3COO^-	73
n-$C_3F_7COO^-$	182
$(CF_3SO_2)_2N^-$	52

Solubility in/of Ionic Liquids

Variation of the alkyl group
Increasing nonpolar character of the cation increases solubility of nonpolar solutes.

Water solubility depends on the anion
water-soluble [BMIM] Br, CF_3COO, CF_3SO_3
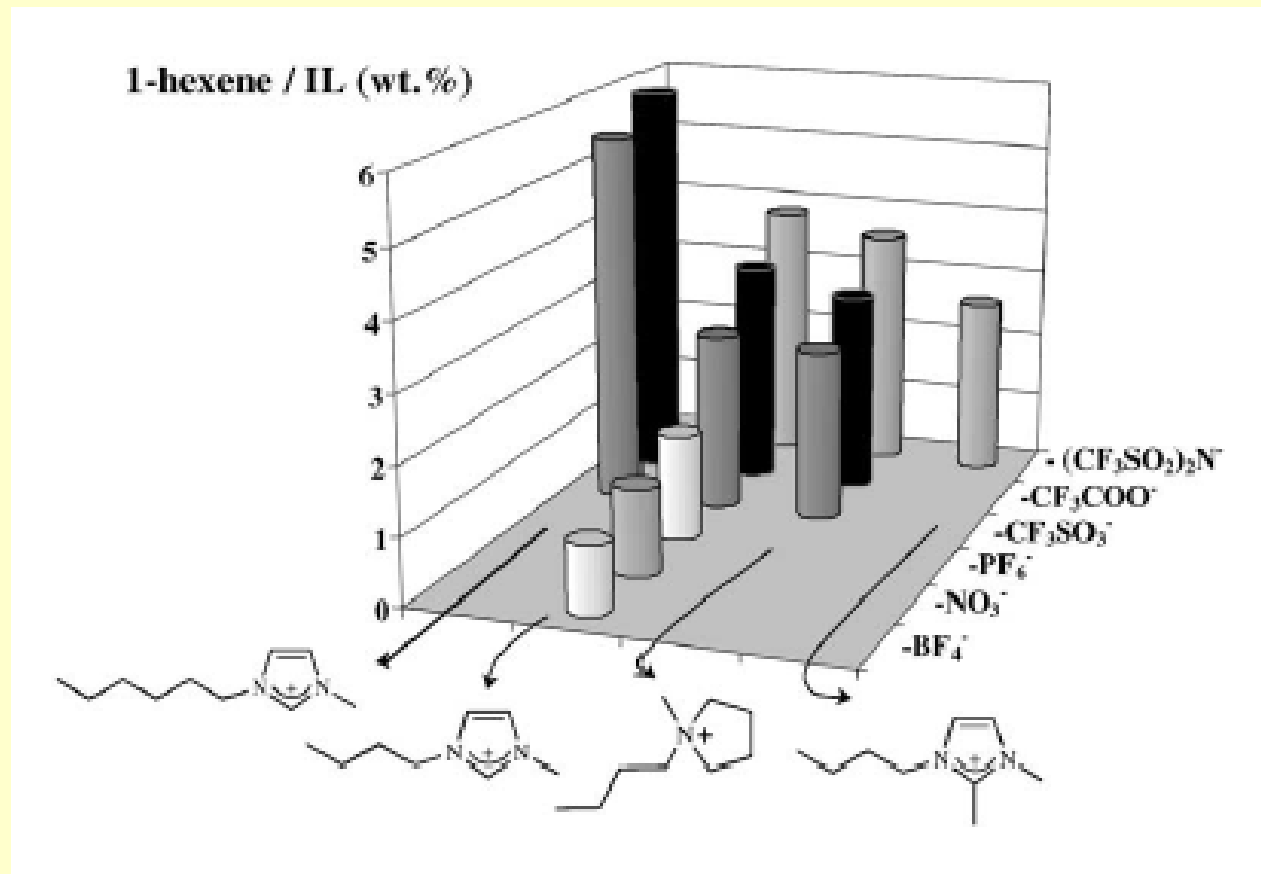**Water-immiscilble [BMIM] PF_6 $(CF_3SO_2)_2N$**

IL miscible with organic solvent IF their dielectric constant is above a certain limit given by the cation/anion combination

Polarity by $E_{(T)}(30)$ scale

[EtNH$_3$][NO$_3$]   0.95   between CF_3CH_2OH and water

[BMIM] PF$_6$ as methanol

Solubility in/of Ionic Liquids

Applications of Ionic Liquids

Electrodeposition of metals and alloys (also nanoscopic)

Al, $CoAl_x$, $CuAl_x$, $FeAl_x$, $AlTi_x$

Semiconductors Si, Ge, GaAs, InSb, CdTe

Electrodeposition of a Bi-Sr-Ca-Cu alloy (precursor to SC oxides)

Melt of MeEtImCl at 120 ºC

$BiCl_3$, $SrCl_2$, $CaCl_2$, $CuCl_2$ dissolve well

Constituent	$BiCl_3$	$SrCl_2$	$CaCl_2$	$CuCl_2$
Concentration $(mol\ kg^{-1}\ MeEtImCl)$	0.068	0.50	0.18	0.050

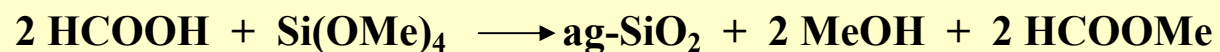**Substrate Al**
-1.72 V vs the Ag/Ag^+ reference electrode

Applications of Ionic Liquids

Biphasic solvent systems

Preparation of aerogels

$$2 \text{ HCOOH} + \text{Si(OMe)}_4 \longrightarrow \text{ag-SiO}_2 + 2 \text{ MeOH} + 2 \text{ HCOOMe}$$

Natural gas sweetening (H_2S, CO_2 removal)

Electrolytes in batteries or solar cells

Dissolving spent nuclear fuel (U^{4+} oxidized to U^{6+})

Extraction

Enyzme activity

Applications of Ionic Liquids

Olefin polymerization
Ethene + $TiCl_4$ + $AlEtCl_2$ in acidic IL
Ethene + Cp_2TiCl_2 + $Al_2Me_3Cl_3$ in acidic IL

Cp_2TiCl_2 + $[cation]^+[Al_2Cl_7]^-$ $\rightleftarrows$ $[Cp_2TiCl]^+$ + $[cation]^+$ + 2 $[AlCl_4]^-$

Olefin hydrogenation
Cyclohexene + H_2 + $[RhCl(PPh_3)_3]$ (Wilkinson's catalyst)