### Heterogeneous catalysis (C9981)

- 1. Basic principles, thermodynamics, and kinetics
- 2. Active sites and catalyst evaluation

## Definition

- Catalyst is...
  - A substance that speeds up a chemical reaction
  - Without being consumed or changed



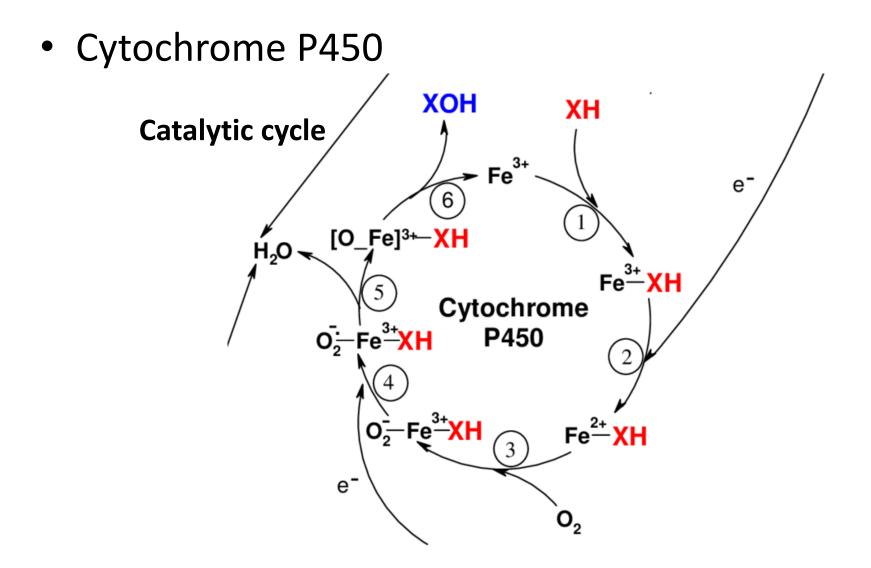
- We get our products
  - In shorter time; at lower rxn temperature; at lower pressure
  - cheaper; economical; ecological

## Types of catalyst (based on phase)

- Homogeneous
- Heterogeneous
- Enzymatic

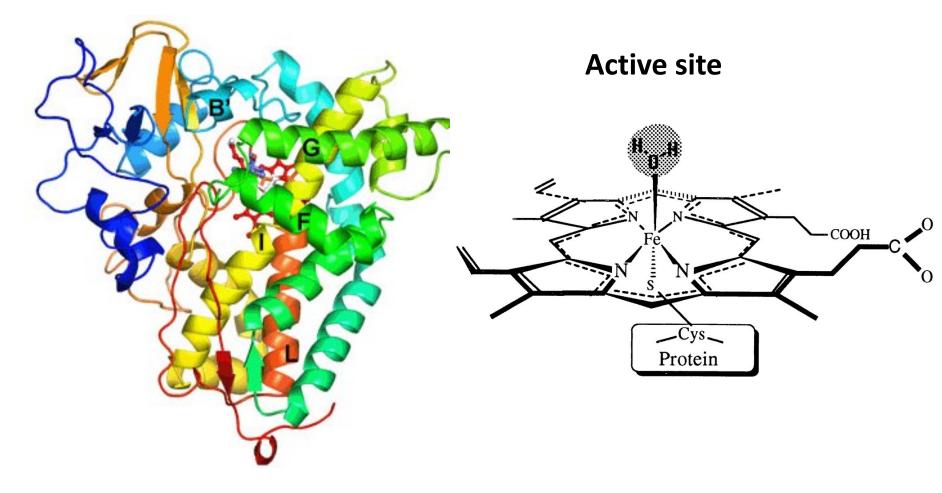


#### **Enzymatic catalysis**



#### Enzymatic catalysis

• Cytochrome P450



### Homogeneous catalysis

• A catalyst and rxn mixture in one unique phase

 $P(Cy)_3$ 

P(Cy)<sub>3</sub>

C

Gas phase

#### 1/

$$CI + O_3 \rightarrow CIO_3$$
  

$$CIO_3 \rightarrow CIO + O_2$$
  

$$CIO + O \rightarrow CI + O_2$$

Total:

 $O_3 + O \rightarrow 2 O_2$ 

#### 2/

Isomerization of hydrocarbons with **HF** (both in gaseous phase)

#### 1/

.Ph

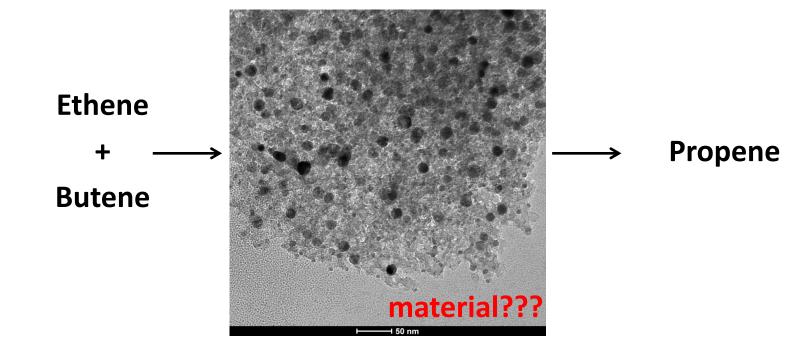
2/

Esterification of acids with alcohols catalyzed by H<sup>+</sup> (a,g. H<sub>2</sub>SO<sub>4</sub>, H<sub>3</sub>PW<sub>12</sub>O<sub>40</sub>)

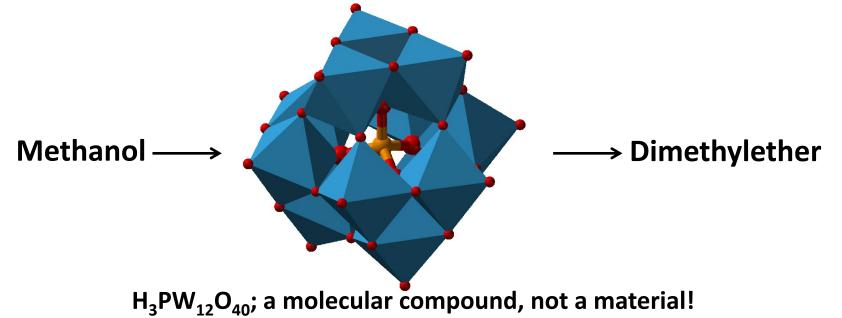
Liquid phase

Olefin metathesis over Grubbs catalyst (organometallics dissolved in liquid solvent along with precursors

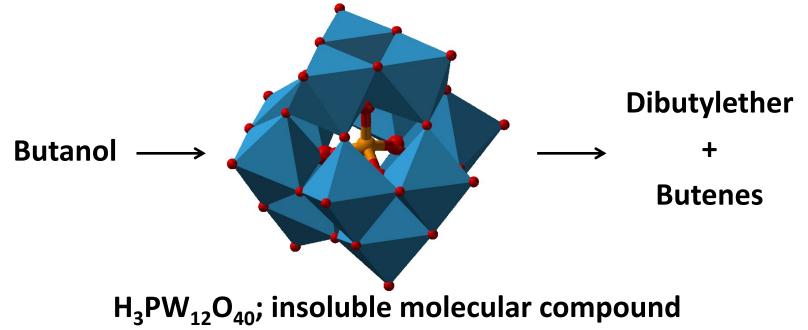
- A catalyst is present in a **different**, **distinct phase** in contrary to the rxn mixture
- Gas phase rxn mixture over solid catalyst
  - Olefin metathesis



- A catalyst is present in a **different**, **distinct phase** in contrary to the rxn mixture
- Gas phase rxn mixture over solid catalyst
  - Alcohol dehydration

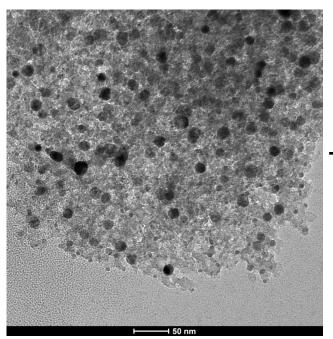


- A catalyst is present in a **different**, **distinct phase** in contrary to the rxn mixture
- Liquid phase rxn mixture over solid catalyst
  - Alcohol dehydration

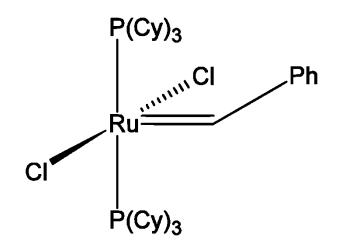


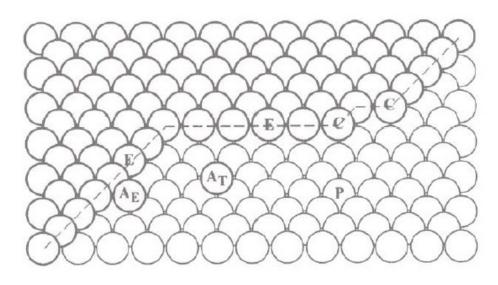
- A catalyst is present in a **different**, **distinct phase** in contrary to the rxn mixture
- Liquid phase rxn mixture over solid catalyst
  - Olefin metathesis





Jonger olefins

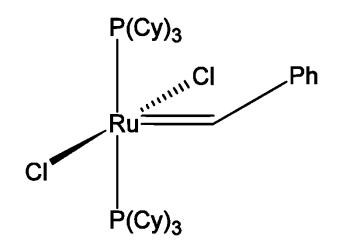




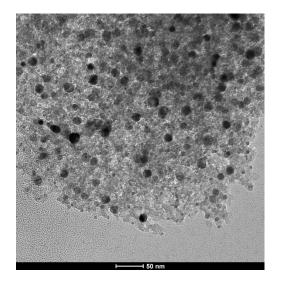
Well defined

= easier to characterize the active site, describe reactivity, and evaluate catalytic performance

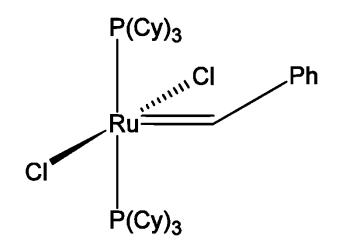
- Ill defined
  - = active site???
  - = more than one type
  - of active sites???
  - = number of active
  - sites???



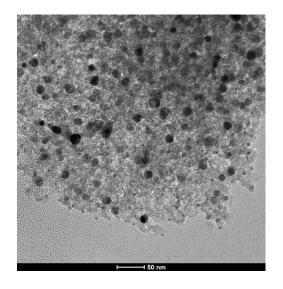
 One phase with reactants
 = higher probability that all necessary species meet and react<sup>©</sup>



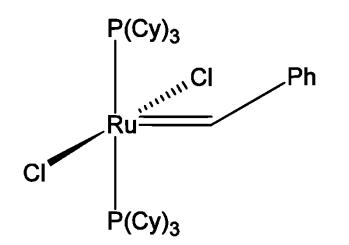
- Distinct phase
   = diffusion???
  - = adsorption???
  - = desorption???

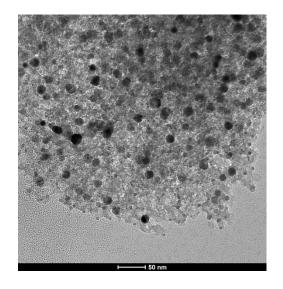


- Separation???
- Reusability/Price???
- Toxicity???
- Batch rxns only???



- Distinct phase
  - = easy to separate
  - = reusable/recyclable
  - = clean products
  - = continuous processes



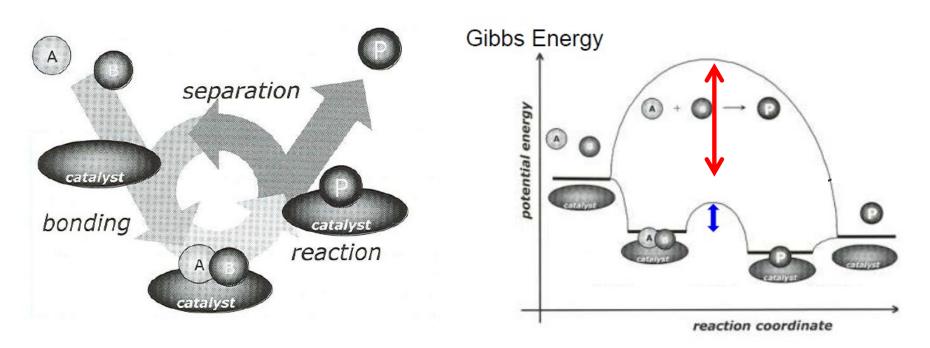


#### Homogeneous and Heterogeneous catalysis are complementary to each other

We choose either hetero or homo based on the rxn we want to catalyze (pros and cons)

#### Catalytic cycle

 $A + B \rightarrow P$ 



 $E_a >> E_a(cata); k = A \cdot e^{-Ea/RT}$ ΔG = ΔG(cata); ΔG = -RT·InK

- Addition of catalyst into the rxn mixture
  - does change "k"
  - does not change "K"

A → P, speeded up by addition of a catalyst K = 1;  $\Delta$ G = 0 kJ mol<sup>-1</sup>; final rxn mixture: 1A + 1P

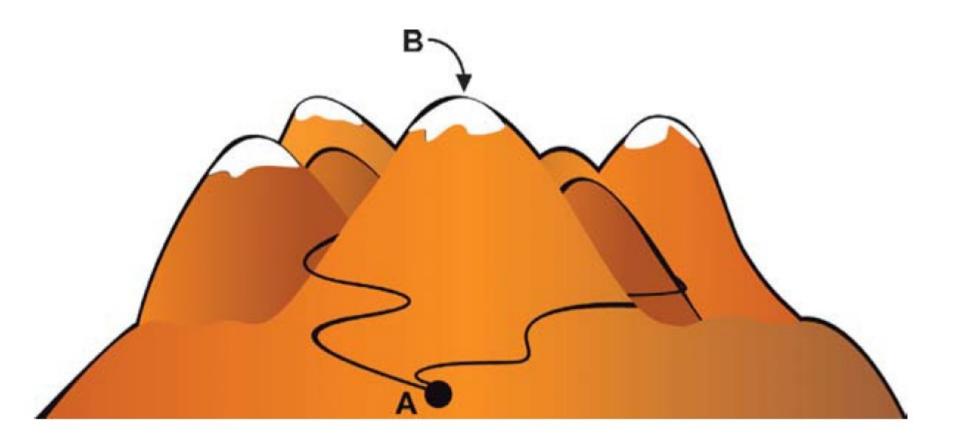
The catalyst is then equally efficient in catalysing the opposite process  $P \rightarrow A$ ; final rxn mixture: 1A + 1P

- If a catalyst is efficient in **dehydration** then it can be possibly used in **hydration**
- If a catalyst is efficient in hydrogenation
   then it can be possibly used in dehydrogenation

## I.e.: It depends on ΔG of studied reaction, whether the catalyst hydrogenates or dehydrogenates.

We know how to shift equilibrium of chemical reaction (#GenChem). This is not a job of the catalyst.

• Reaction coordinate: A multidimensional problem



- Reaction coordinate: A multidimensional problem
  - e.g. selective oxidation reactions (Table 1)

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• We are not shooting for the most stable product (thermodynamically); **Difficult!** 

Sratting material	Target product	Mol water per Mol starting material	ΔH <sub>298</sub> target proc uct	ΔH <sub>298</sub> I- Total oxida tion
СН₃ОН	CH₂O	1	-311	-675
$C_2H_4$	C₂H₄O	0	-438	-1323
C <sub>3</sub> H <sub>6</sub>	C₃H₄O	1	-365	-1959
i-C <sub>4</sub> H <sub>8</sub>	$C_4H_6$	1	-242	-2522
				$\overline{\bigcirc}$
d. <b>2015</b> , 54, 34	165 - 3520		Mountair	Spa
ר ודנ וניייי			cottage	resort

Table 1: Thermodynamic data for select catalytic oxidation reactions.

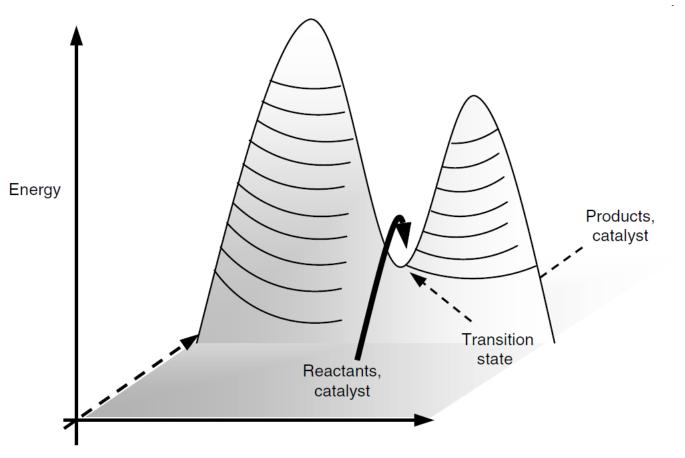
- Reaction coordinate: A multidimensional problem
  - How is it possible that we sometimes end up in a mountain cottage and not in the spa resort???
  - We need a catalyst!
  - The catalyst will lower the activation energy of our way to the mountain cottage (beautiful views, crazy friends,...)
  - The catalyst will increase the activation energy of our way to the spa resort
  - E.g. The catalyst has to increase the rate of hiking (selective oxidation) and decrease the rate of hiking (total oxidation). What a difficult job!

#### • Reaction coordinate: A multidimensional problem

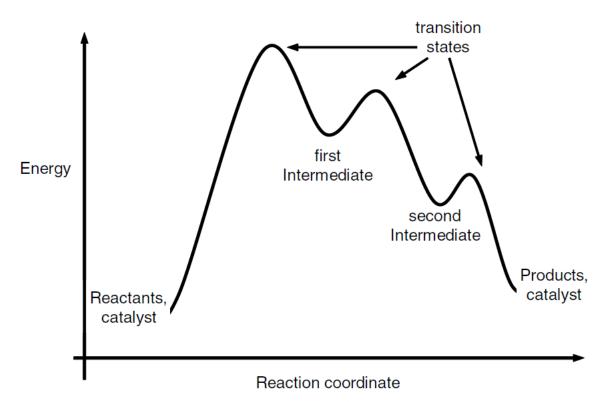
However, a product is usually sought which is not the most thermodynamically stable and in fact may be less stable than the starting material. The catalyst then has the task of quickly activating the starting materials while slowing the formation of the most thermodynamically favored products and thereby allowing the generation of less-stable products. The latter should not be further activated by the catalyst, although the catalyst must be potent enough to activate the more stable starting materials. Catalysts must also often prevent reactions to end up with the desired products, so the view that catalysts always accelerate reaction rates is, therefore, a misnomer.

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• **Reaction coordinate:** From multidimensional to twodimensional problem



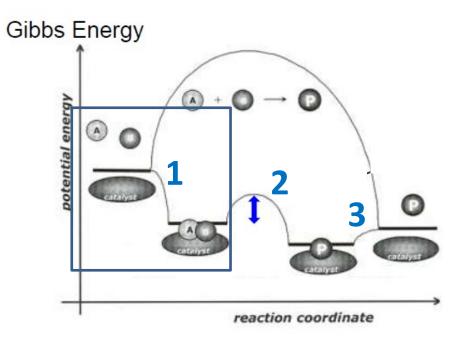
• Transitions state vs. Intermediate



**Figure 2.5** Energy/reaction coordinate diagram for a two-step reaction, with two catalytic intermediates and three transition states.

# Thermodynamics – heterogeneous catalysis

 $A + B \rightarrow P$ 



1: Adsorption of reactants on catalyst surface (hetero) / Formation of reaction intermediate ABC (enzymes and homo)

In heterogeneous catalysis always thermodynamically favorable

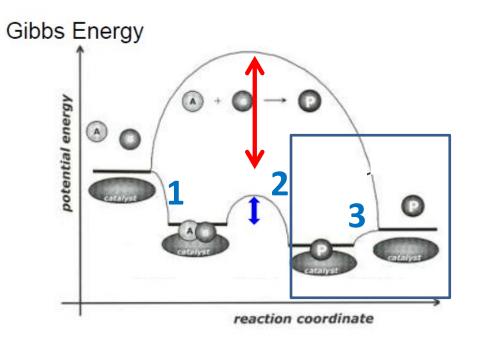
(coordinatively unsaturated surface + adsorbate)

Let's imagine weak interaction of A, B, and catalyst surface...???

Let's imagine very strong interaction of catalyst surface, A, and/or B...??

#### Thermodynamics

 $A + B \rightarrow P$ 

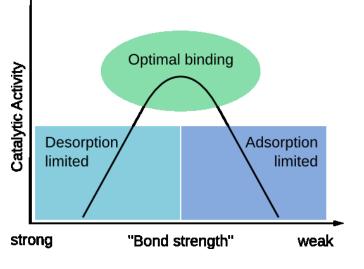


**3:** Desorption of products from catalyst surface (hetero) / Rupture of product intermediate PC (enzymes and homo)

Let's imagine very strong interaction of P with catalyst surface...???

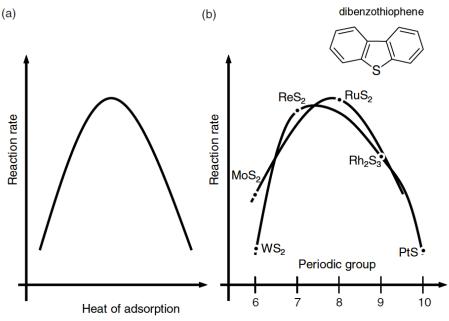
#### Thermodynamics

- Interactions of A,B, and P with catalyst not too weak, not too strong
   (- physi/chemicorption on catalyst surface)
  - (= physi/chemisorption on catalyst surface)



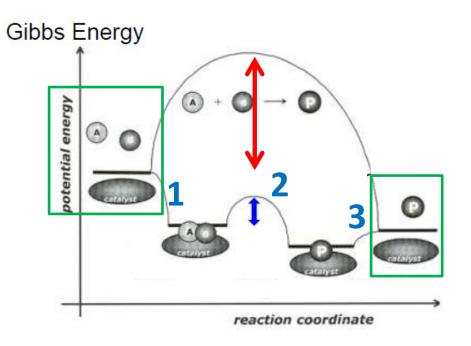
#### Sabatier's principle; Volcano plot

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**Figure 2.15** Examples of volcano plots, describing the reaction rate as a function of the heat of adsorption (*left*), and the activity of the second-row and third-row transition metal sulfides in the hydrodesulfurization of dibenzothiophene (*right*).

 $A + B \rightarrow P$ 



Before going any further...

Steps 1 and 3 are equally important to step 2 in catalysis .

Adsorption and desorption of A, B, and P might have a significant effect on E<sub>a</sub>.

In kinetic studies in heterogeneous catalysis we estimate only **apparent activation energy**  $(E_{app})$ , where all these contributions are included.

- Importance of reactant adsorption and product desorption
  - Example: Ethylbenzene dehydrogenation to styrene

*Table 3:* Some parameters<sup>[164a, 164f]</sup> for the sorption of ethylbenzene (EB) and styrene (St) on single-crystal model catalysts.<sup>[a]</sup>

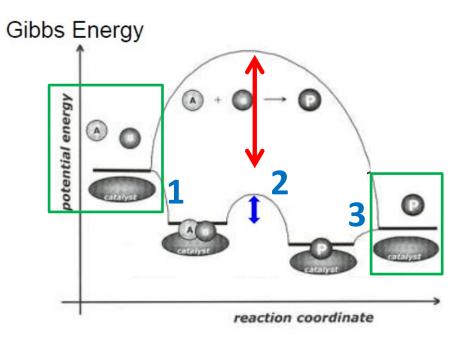
Surface	E <sub>des</sub> St	E <sub>des</sub> EB	θ EB [%]	θ St [%]	θ St/ θ EB
Fe₃O₄ (111)	118	86	92	100	250
Fe <sub>2</sub> O <sub>3</sub> (111)	73	64	37	29	0.8
KFeO <sub>2</sub> (111)	65	65	25	6	0.2

The best

catalvst

[a] The desorption energy is given in kJ mol<sup>-1</sup>. The degree of surface coverage was obtained with a reactant pressure of 100 mbar at a reaction temperature of 900 K.

 $A + B \rightarrow P$ 



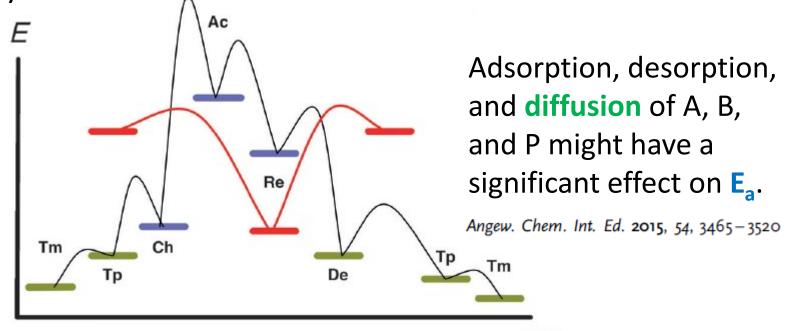
What is **preceding step** 1 and **following step 3**?

**Diffusion!** 

**Diffusion** of A, B, and P might have a significant effect on **E**<sub>a</sub> as well.

In kinetic studies in heterogeneous catalysis we estimate only **apparent activation energy**  $(E_{app})$ , where all these contributions are included.

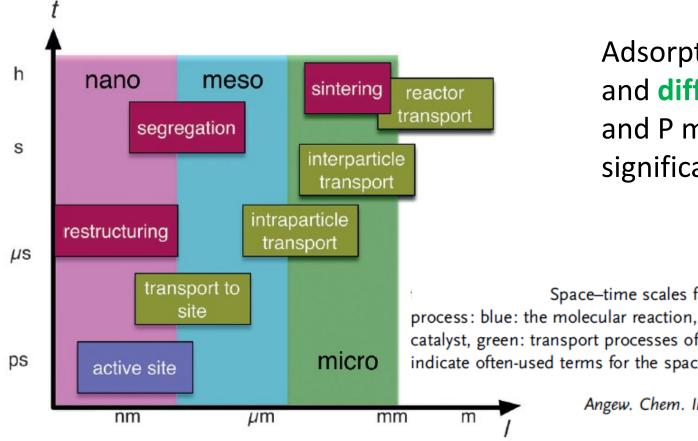
 Another representation of the complexity of heterogeneous catalytic reaction



RC

**Figure 1.** Dimensions in catalysis: A) Change in energy (*E*) of a catalytic system with respect to the reaction coordinate (RC) for the basic individual steps: Tm: transport macroscopic, Tp: transport in pores or solvation shells, Ch: chemisorption, AC: activation (dissociation), Re: reaction, De: desorption, dissociation. The energy changes in red denote the impact of the reaction on active centers

Another representation of the complexity of heterogeneous catalytic reaction



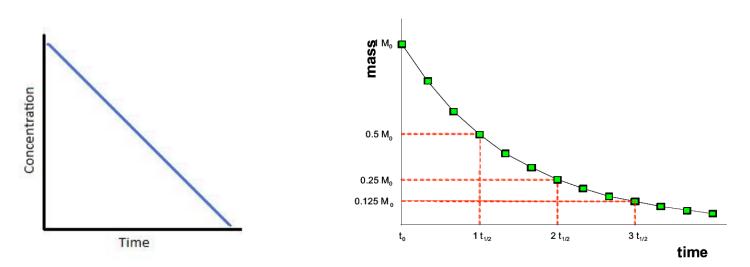
Adsorption, desorption, and **diffusion** of A, B, and P might have a significant effect on  $E_a$ .

Space-time scales for a heterogeneous catalytic process: blue: the molecular reaction, red: chemical dynamics on the catalyst, green: transport processes of the reactants. The vertical bars indicate often-used terms for the spacial dimensions.

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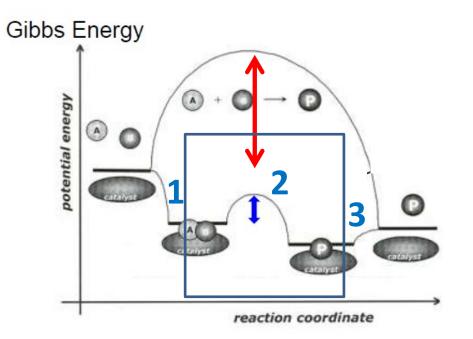
### Kinetics

- We know kinetics (#ChemKin)
- Rxns of zero order, first order, and second order



 But in catalysis also 0.39 order, –0.5 order... (many elementary rxns, fight for active site between reactants and products,...!)

 $A + B \rightarrow P$ 

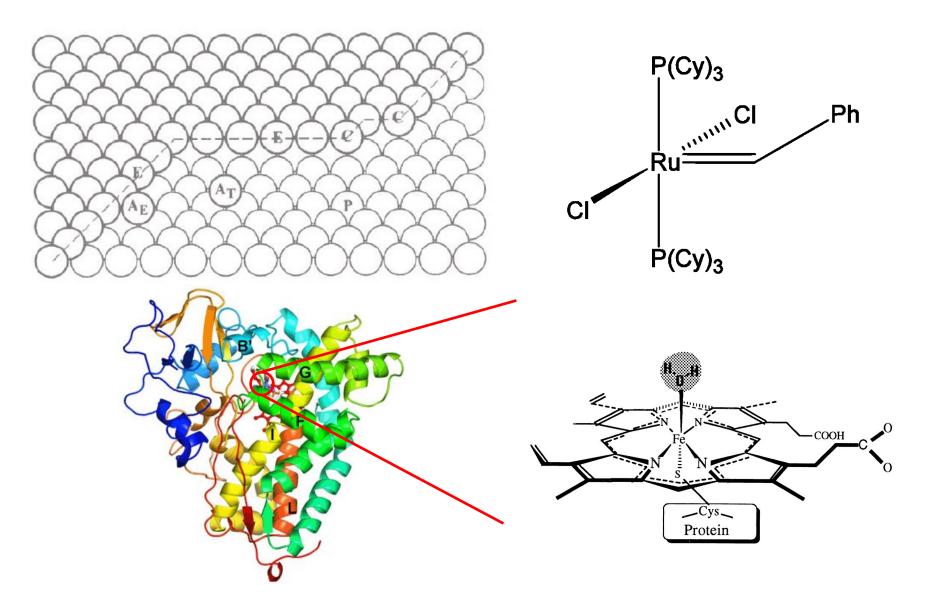


In order to decrease E<sub>a</sub>
 for step 2 we need to
 design an active site of the
 catalyst as good as possible

What is the active site???

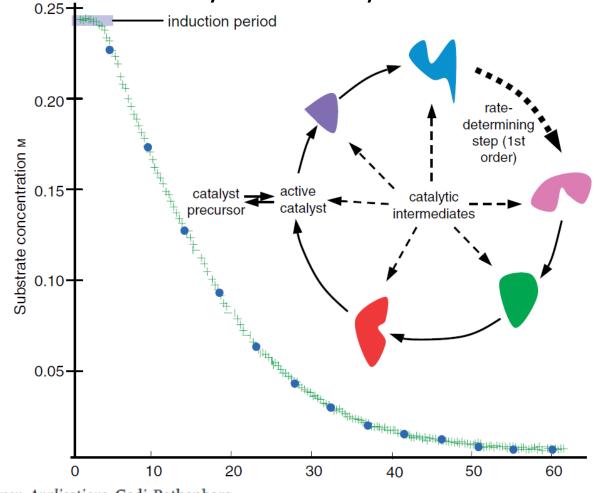
How do we measure the **"goodness"** of the active site???

#### Active sites



#### Active sites

• Active sites are often dynamic: They has to be created first!



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- Turn-over frequency (TOF; [s<sup>-1</sup>])
   = number of catalytic cycles performed by 1 active site per time unit
- Precise numbers for homogeneous and enzymatic catalysis
- Numbers for heterogeneous catalysis???

	TOF [s <sup>-1</sup> ]	
Hetero:	~1–100 s <sup>-1</sup>	
Homo:	~10–1000 s <sup>-1</sup>	
Enzymes:	~10000–1000000 s <sup>-1</sup>	

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- Turn-over number (TON; [-])
   = number of catalytic cycles performed by 1 active site before deactivation (~lifetime)
- Precise numbers for homogeneous and enzymatic catalysis
- Numbers for heterogeneous catalysis???

• **Selectivity** is ability of catalyst to form one product from a pool of products (possibly many)

reactant R 
$$\begin{cases} \times C \\ \rightarrow D \\ \times E \\ \times F \end{cases}$$

• **Selectivity** (S; [%])

= number of D molecules produced / R molecules converted

- Enantiomeric enrichment is ability of catalyst to form selectively one enantiomer
- Enantiomeric enrichment (ee; [%])
   = S(P<sub>R</sub>) S(P<sub>S</sub>)
   (e.g. Final mixture consists of 90 % P<sub>R</sub> and 10 % P<sub>S</sub>
   ee = 80 %)

	S [%]	ee [%]
Hetero:	1–100	1–100
Homo:	> 90	> 70
Enzymes:	> 99.99	> 99.99

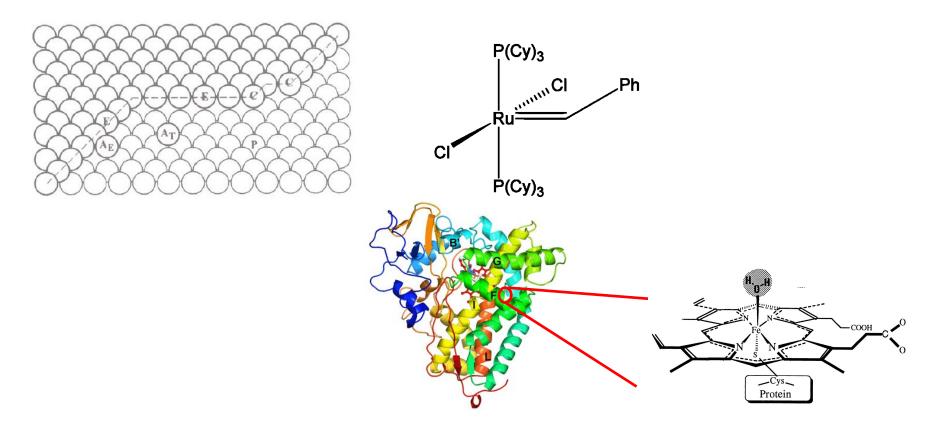
 Selectivity is ability of catalyst to form one product from a pool of products (possibly many)

 Specificity is ability of catalyst to react with one reactant among many (similar) reactants

$$A + B \begin{cases} \times C \\ \rightarrow D \\ \times E \\ \times F \end{cases}$$

$$A + \begin{cases} C & \star & AC \\ D & \rightarrow & AD \\ E & \star & AE \\ F & \star & AF \end{cases}$$

#### Active sites



**Electronic** and **steric** properties do play an important role! (TOF, TON, Selectivity, ee, specificity).

#### $R \rightarrow P + P'$

- Conversion (C; [%])
   = number of R molecules converted / number of R molecules introduced
- Yield (Y; [%])
   = number of P molecules produced / number of R molecules introduced
- Selectivity (S; [%])
   = number of P molecules converted / number of R molecules converted

$$S = \frac{Y}{C}$$

#### $R \rightarrow P + P'$

- Productivity (STandard Yield, STY; [g g<sup>-1</sup> s<sup>-1</sup>])
   = amount of product P produced per unit of time and unit of catalyst mass
  - high conversion, high selectivity, low catalyst mass,
     high flow
  - = industrial viewpoint

• Homework

- Ecological point of view
- Atom efficiency [%]
   = mass of desired product / total mass of all products
- E factor [-]
   = mass of all wastes (solvents, gases, unreacted precursors, byproducts) / mass of desired products
- EQ factor [-]

= E factor, mass of each waste multiplied by Q
(environmental unfriendliness), e.g. Q = ~0 for water,
~ 1 for NaCl, and ~1000 for toluene...

- Ecological point of view
- Atom efficiency [%], E factor [-], EQ factor [-]

