

# Heterogeneous catalysis

Lecture 9

Zeolites in oil refinement

# Zeolites - synthesis

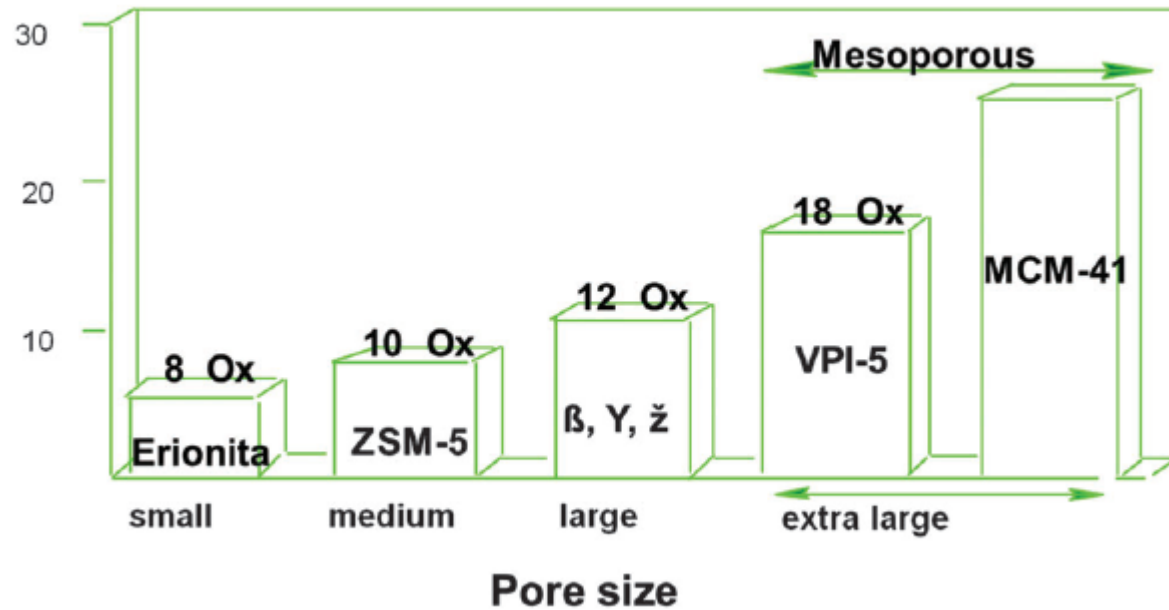
- **Reaction mixture:** ..., ..., ..., ...
  - pH adjustment, (gelation)
  - Hydrothermal treatment in an autoclave
  - ...
  - ...
- **Result:** H-zeolite (Brønsted acidic with H<sup>+</sup> ions)

# Zeolites - synthesis

- **Reaction mixture:**  $\text{Na}_2\text{SiO}_3$ ,  $\text{Al}_2\text{O}_3$ , quarternary ammonium salt (=structure directing agent), water
  - pH adjustment, (gelation)
  - Hydrothermal treatment in an autoclave
  - Ion exchange ( $\text{Na}^+$  for  $\text{NH}_4^+$ )
  - Calcination (=  $\text{NH}_3$  removal)
- **Result:** Crystalline H-zeolite (Brønsted acidic with  $\text{H}^+$  ions)

# Zeolites - synthesis

- Pore size



- Si/Al ratio  $\geq 1$

# Zeolites - acidity

- **Brønsted:** ...

- Structure:

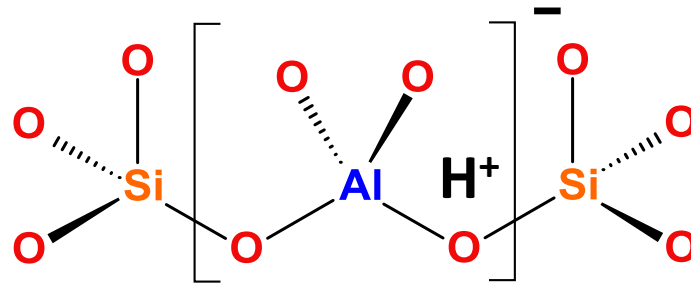
- **Lewis:** ...

- Structure:

# Zeolites - acidity

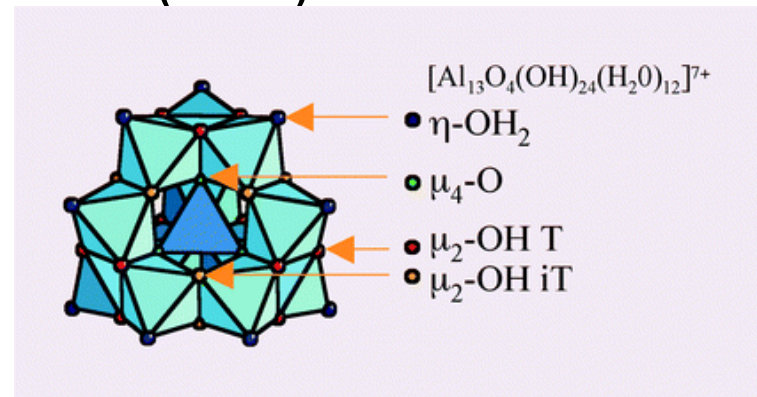
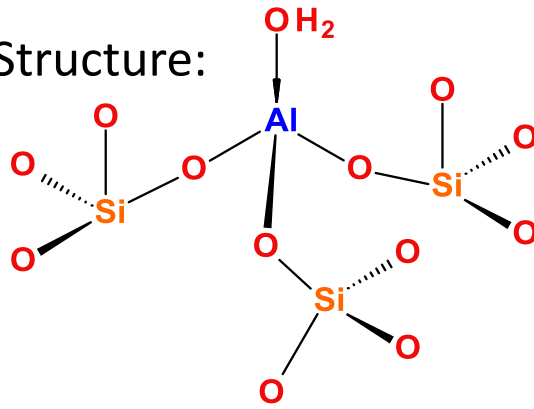
- **Brønsted:** negative charge of the aluminosilicate net balanced by strongly acidic protons

– Structure:



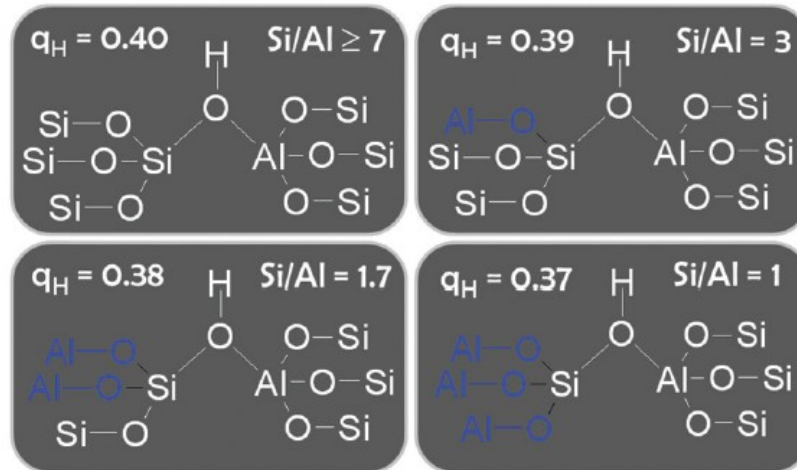
- **Lewis:** Al atoms that are not embedded in the aluminosilicate net (e.g. surface species, amorphous stuff, alumina particles) = extraframework aluminum species (EFAL)

– Structure:



# Zeolites - acidity

- **Brønsted:** depends on the second coordination sphere (i.e. Si/Al ratio)



- **Lewis:** Extraframework aluminum species (EFAL) depends on
  - Si/Al ratio
  - Aging (time on stream, steaming)
  - Can be washed out (depending on pH – acid washing)

# Zeolites - acidity

- **High Si/Al ratio**
  - Strong Brønsted acid sites
  - Weak Brønsted acid sites
  - Strong Lewis acid sites
  - Weak Lewis acid sites
  
- **Low Si/Al ratio**
  - Strong Brønsted acid sites
  - Weak Brønsted acid sites
  - Strong Lewis acid sites
  - Weak Lewis acid sites

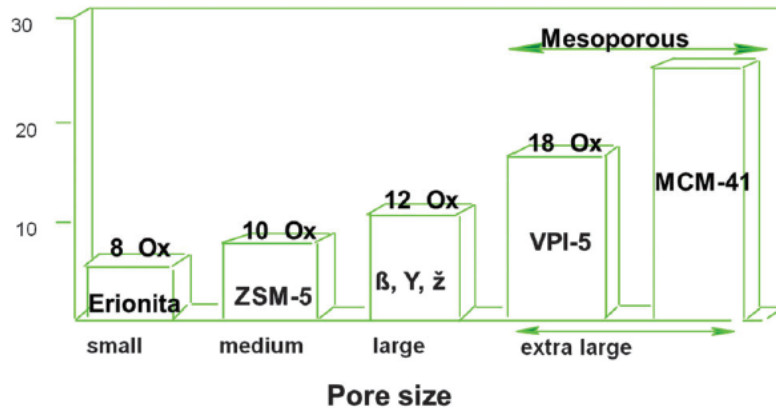


# Zeolites - acidity

- **High Si/Al ratio**
  - Strong Brønsted acid sites
  - ~~– Weak Brønsted acid sites~~
  - ~~– Strong Lewis acid sites~~
  - ~~– Weak Lewis acid sites~~
  
- **Low Si/Al ratio**
  - ~~– Strong Brønsted acid sites~~
  - Weak Brønsted acid sites
  - Strong Lewis acid sites
  - Weak Lewis acid sites

# Zeolites - acidity

- **Confinement effect**



- **Superacidity**

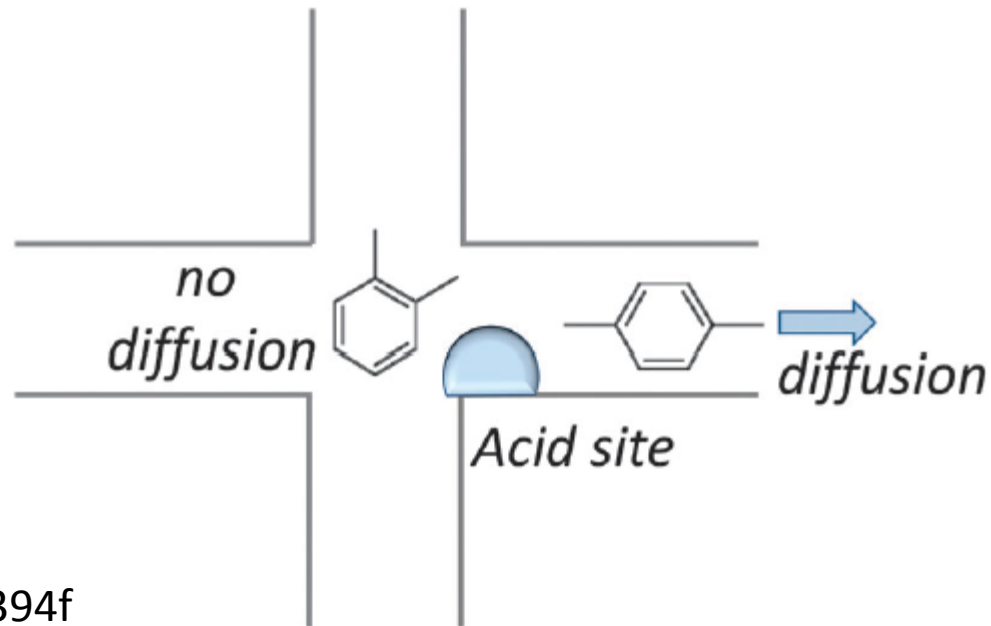
- Various probes at RT – acid site strength similar to 70 % H<sub>2</sub>SO<sub>4</sub> (=NO!)
- Ability to protonate hydrocarbons at working conditions (=YES!)
- ?

# Zeolites – diffusion/shape selectivity

- **Diffusion**

- Big difference between zeolites with 8 membered vs. 12 membered ring pore openings
- Big difference between zeolites with 1D, 2D, and 3D-connected pore structure

- **Shape selectivity**

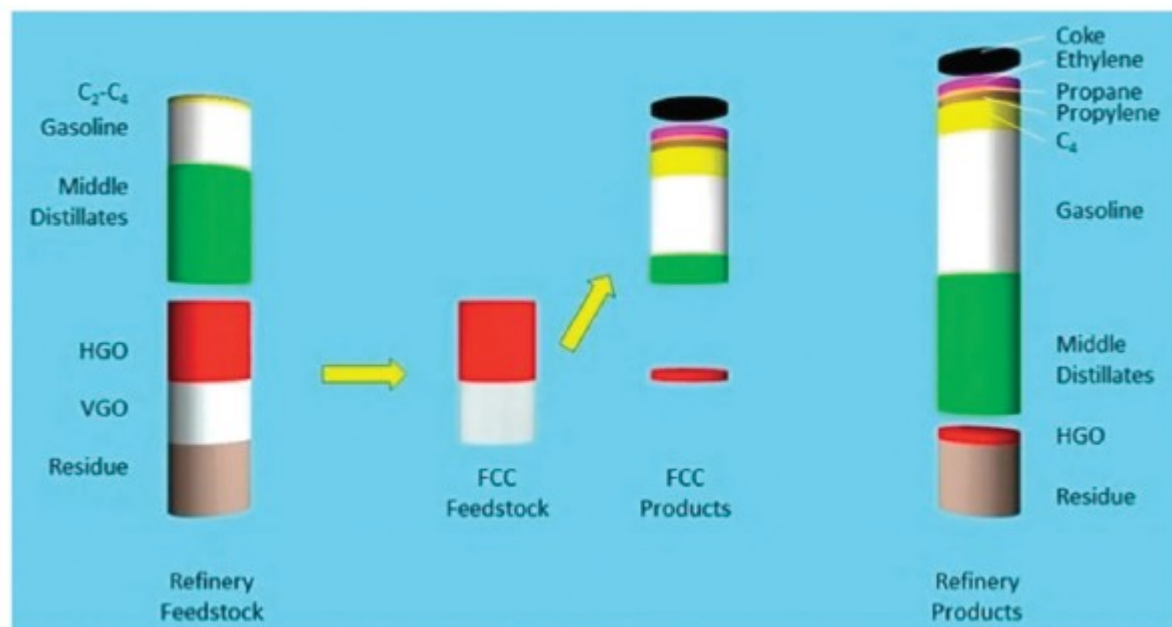


# Zeolites in oil refinement

- **Fluid catalytic cracking**
- **Isobutane-butene alkylation**
- **Reforming (+ steam reforming)**
- **Hydrocracking**
- **Linear paraffin isomerization**

# Zeolites in oil refinement

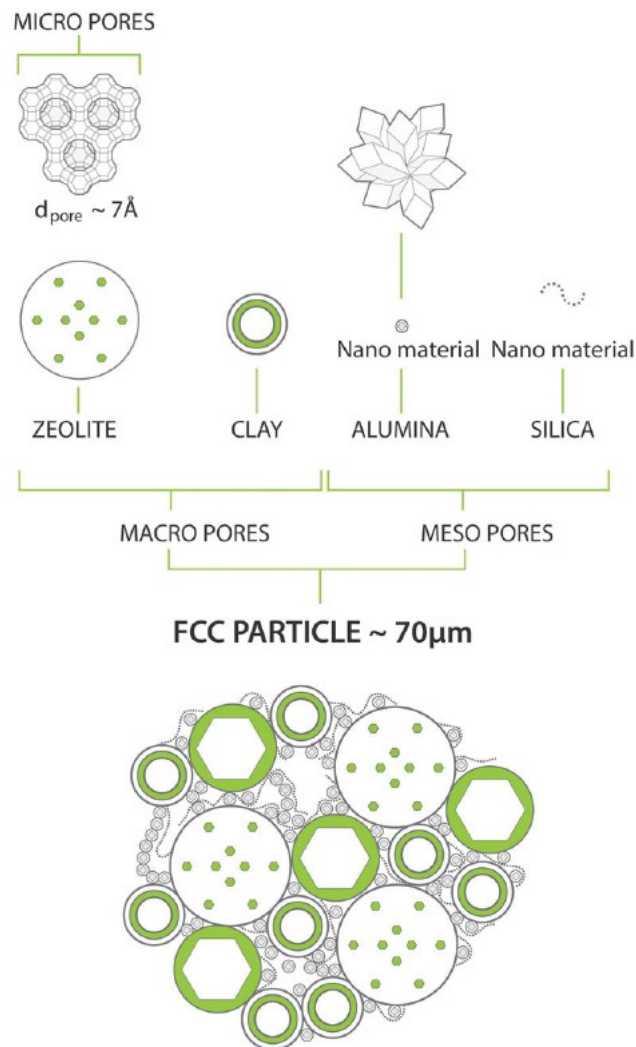
- Fluid catalytic cracking



# Zeolites in oil refinement

- **Fluid catalytic cracking**

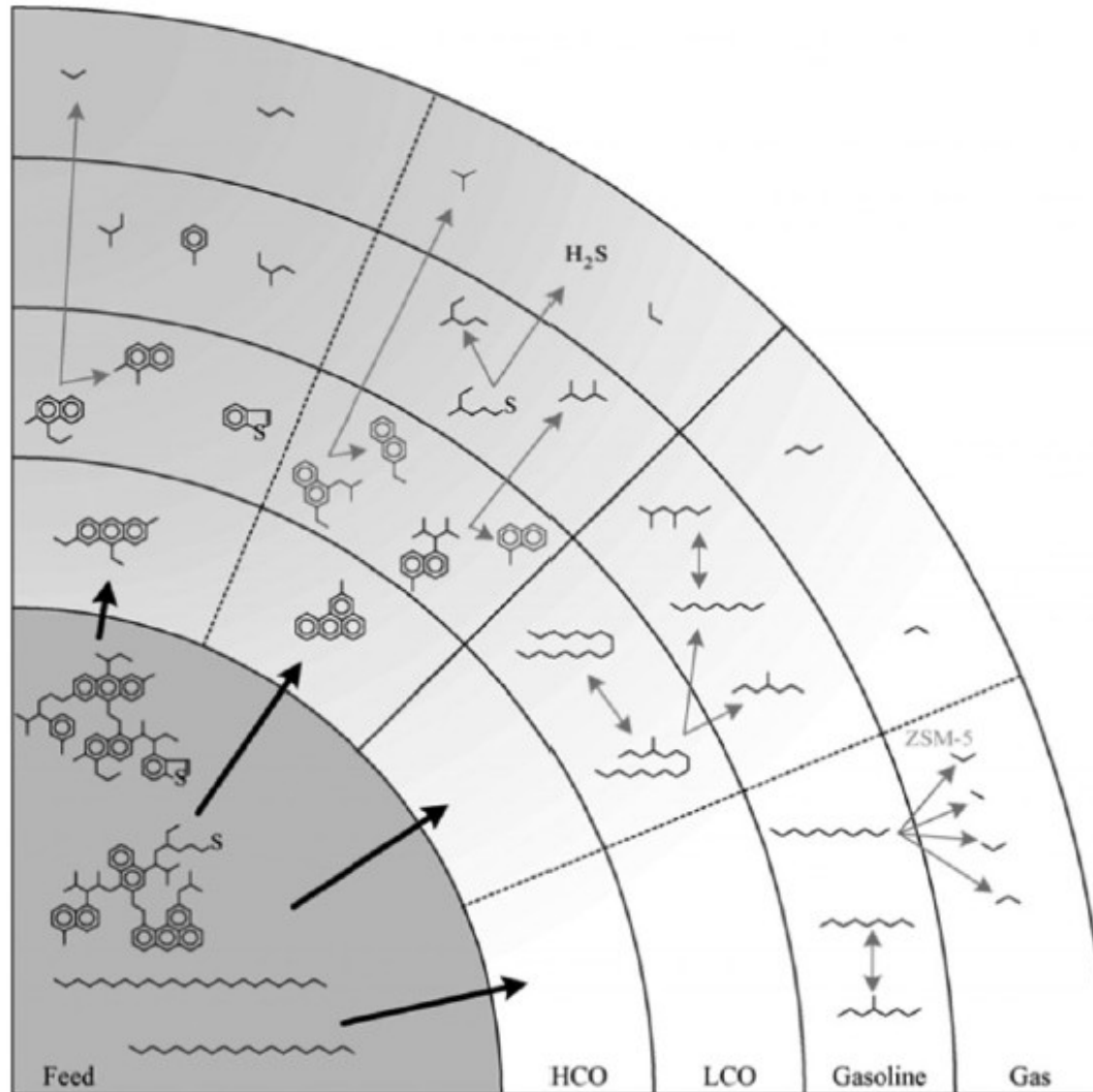
- Zeolite Y 10-50 wt%
- Binders 50-90 wt%
- At the beginning –  $\text{AlCl}_3$
- Addition of HZSM-5



# Zeolites in oil refinement

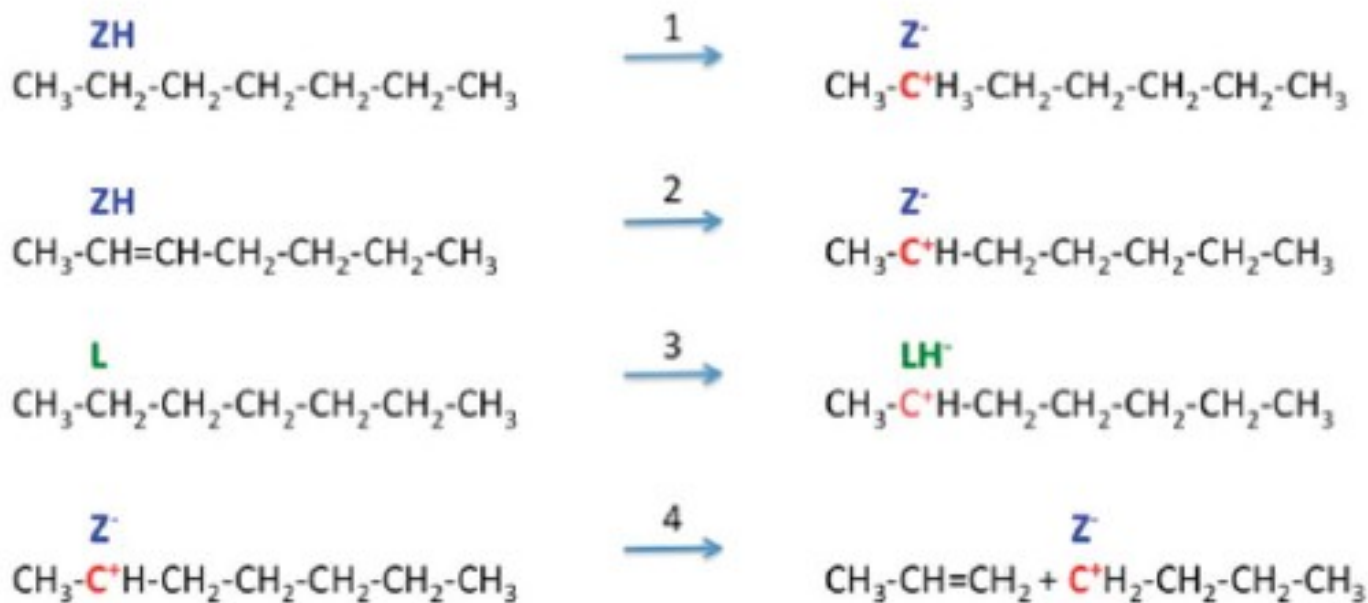
- **Fluid c**

- Sho
- Ison
- „Arc
- HZS



# Zeolites in oil refinement

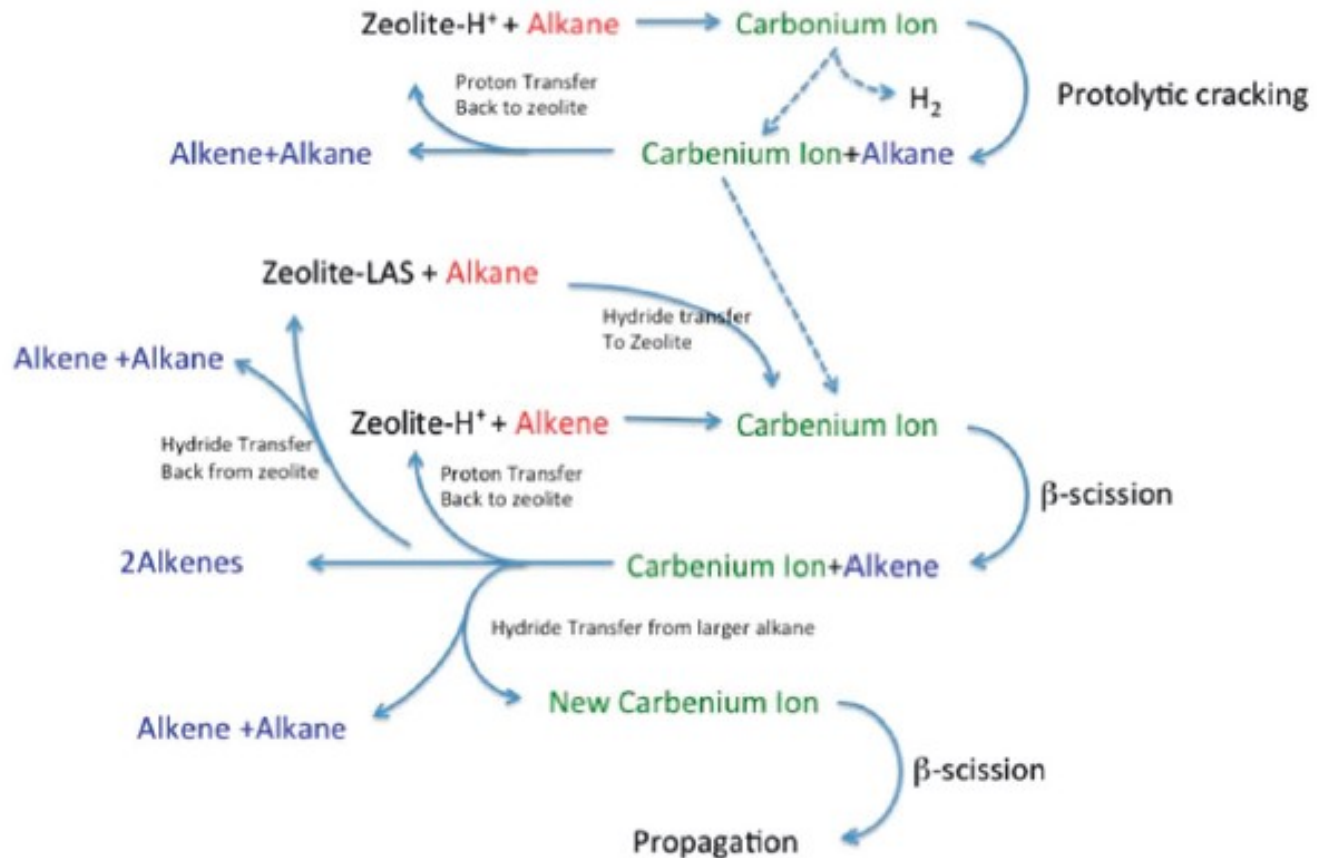
- **Fluid catalytic cracking**
  - Protonation + protolytic cracking
  - H<sup>+</sup> abstraction + β scission





# Zeolites in oil refinement

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# Zeolites in oil refinement

- **Fluid catalytic cracking**

- Protonation + protolytic cracking

- We need strong Brønsted acid sites (zeolite Y)

- H<sup>-</sup> abstraction +  $\beta$  scission

- We need strong Lewis acid sites (steamed/(acid washed) zeolite Y)

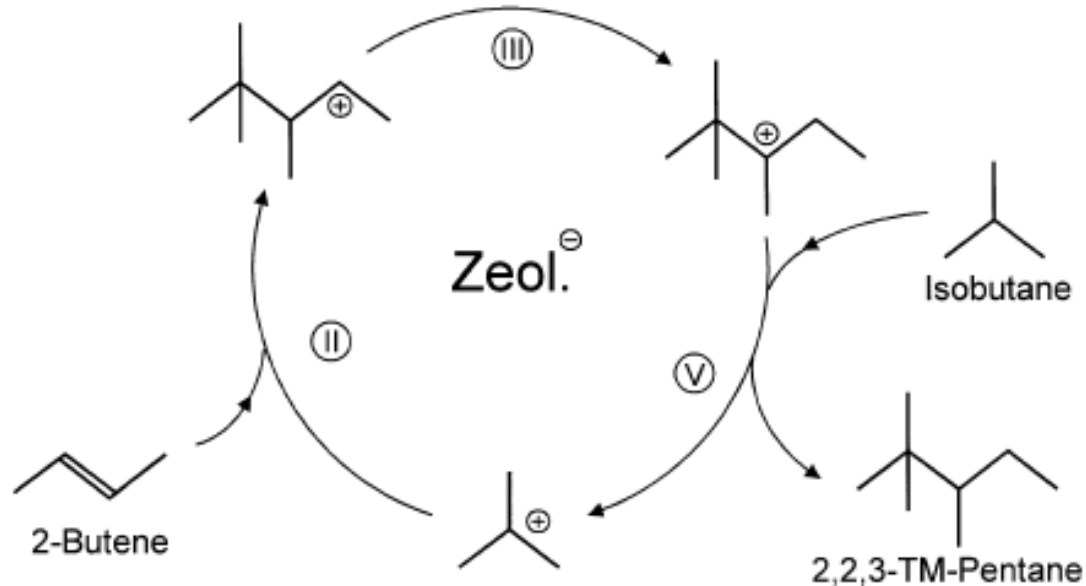
- Long linear hydrocarbons diffusion

- Precracking on alumina and silica-alumina (non-innocent binders)
- Hierarchical porosity in zeolites (steamed/(acid washed) zeolite Y)

# Zeolites in oil refinement

- **Isobutane-butene alkylation**

- We want highly branched C8 hydrocarbons (high octane number)
- HF and H<sub>2</sub>SO<sub>4</sub> catalyzed alkylation still running in industry
- Large pore zeolites as a substitution



# Zeolites in oil refinement

- **Isobutane-butene alkylation**

- Large pore zeolites as a substitution
- BUT! 2-butene dimerization...oligomerization...coking...deactivation

Table 1 Activity and selectivity of some acid zeolites as alkylation catalysts

Zeolite	USY	Beta	Mordenite	ZSM-5	MCM-22
2-Butene conv. (%)	100	97	94	100	95
C <sub>8</sub> (wt%)	40.9	50.6	70.2	83.5	33.0
Trimethylpentanes	74.1	76.9	76.9	20.9	36.9
2,2,4-Trimethylpentane	37.7	52.4	57.2	27.3	4.1

# Zeolites in oil refinement

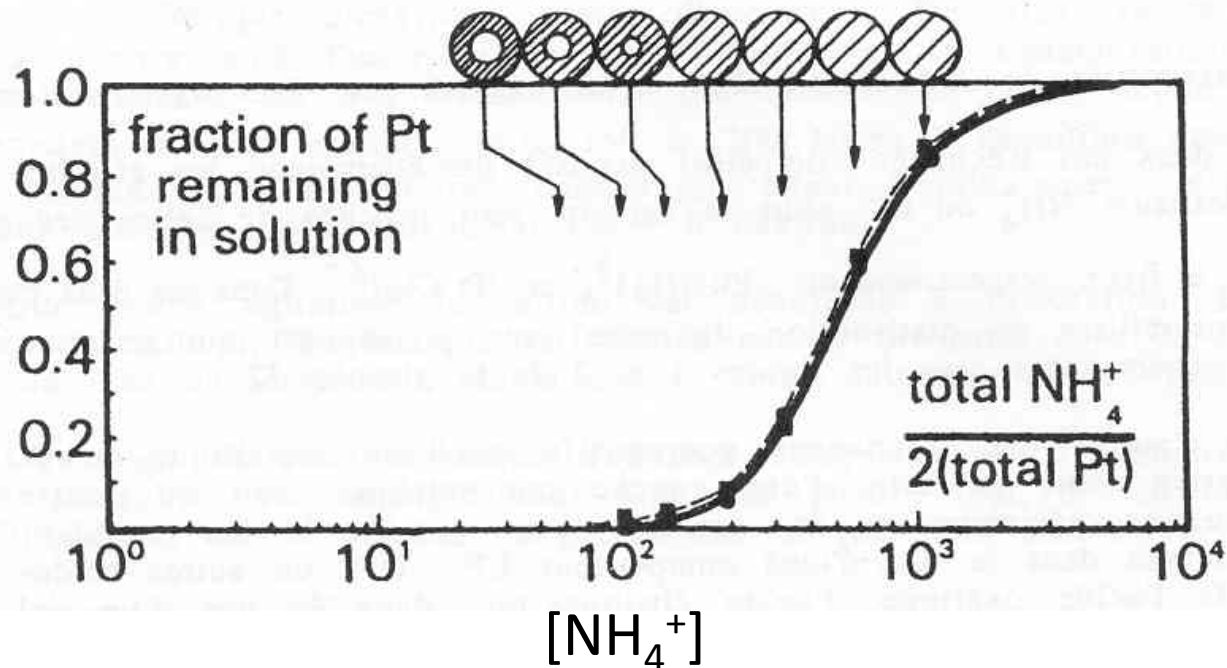
- **Linear paraffin isomerization**
  - Linear C8 (C7) → branched C8 (C7)
  - Requires strong Brønsted acidity and hydrogenation/dehydrogenation activity (Pt(Ni) on mordenite)
  - Mordenite – large pore, monodirectional pores
  - Mordenite – dealuminated (strong H<sup>+</sup>), acid washed (low EFAL)
  - Protonation = carbocations
  - Stability of carbocations? Branched hydrocarbons?

# Zeolites in oil refinement

- **Linear paraffin isomerization**
  - Pt(Ni) on mordenite
  - How do we deposit Pt on a zeolite? (Lecture 3)

# Zeolites in oil refinement


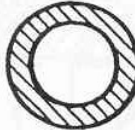
- **Linear paraffin isomerization**
  - Pt, Pd, Ni on mordenite
  - Electrostatic interaction = **ion exchange**
    - Competitive ion exchange



# Zeolites in oil refinement

- **Linear paraffin isomerization**
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## ISOMERIZATION OF N-HEXANE ON Pt/HUSY

T (°C)	$10^4 v_i$ (mole h <sup>-1</sup> g <sup>-1</sup> of Pt/HUSY)		$\frac{v_{IGD}}{v_{IPD}}$
	G.D. 	P.D. 	
230	39	70	2.6 2.3 2.2
250	180	140	
260	317	280	
270	613	540	
280			

G.D. : good distribution

P.D. : poor distribution



# Zeolites in oil refinement

- **Hydrocracking (i.e. cracking in the presence of H<sub>2</sub>)**
  - Shortening of long hydrocarbons
  - From linear to branched (alkylation, carbocations,...)
  - Hydrogenation/dehydrogenation
  - Pt, Pd on mordenite (also zeolite Y and β)

# Zeolites in oil refinement

- **Reforming and steam reforming**

- Cyclization, isomerization of cyclic compounds to cyclohexene, cyclohexene and its derivatives dehydrogenation to benzene, toluene, xylene (BTX), and other aromatics
- H<sub>2</sub> as a useful „by-product“
- Pt on high surface area support, non-acidic
- Reforming in the presence of H<sub>2</sub>O = H<sub>2</sub> production